# Take Off of Small Leidenfrost Droplets 

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#### Abstract

We put in evidence the unexpected behavior of Leidenfrost droplets at the later stage of their evaporation. We predict and observe that, below a critical size $R_{l}$, the droplets spontaneously take off due to the breakdown of the lubrication regime. We establish the theoretical relation between the droplet radius and its elevation. We predict that the vapor layer thickness increases when the droplets become smaller. A satisfactory agreement is found between the model and the experimental results performed on droplets of water and of ethanol.


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The name of J. G. Leidenfrost (1715-1794) is still remembered because he was the first to publish the observation that a puddle of water dropped on a very hot surface divides into droplets, which stand each above the surface and slowly evaporate. At the end of the process, he noticed [1]: ". . .before the whole drop disappears. Which at last exceedingly diminished so that it can hardly any more be seen, with an audible crack, which with the ears one easily hears, it finishes its existence, and in the spoon [making the hot surface] it leaves a small particle of earth. .."

Over the years, the Leidenfrost phenomenon has attracted the attention of many investigators, see for instance [2-8], but seemingly little interest has been paid to the observation by Leidenfrost of the final stage of the droplet evaporation, in particular, what happens when the droplets become very small before finally disappearing. We investigate in this Letter theoretically and experimentally the final regime of the Leidenfrost droplets. We show that when the droplets become smaller than a well defined radius, they suddenly take off due to the breakdown of the classical Leidenfrost lubrication regime. They thus reach an elevation which is much higher than their radius.

Let us consider first an almost spherical drop of volatile liquid with radius $R$ and mass $M$ standing slightly above a hot flat surface with a vapor film of thickness $h$ in between. Let $l$ be the horizontal width of this film, this length will be related to the other physical parameters of the problem.

Our estimate will rely on the fact that, in a range of parameters, the horizontal length scale $l$ is much larger than $h$. Both $l$ and $h$ are less than $R$, the radius of the droplet. Furthermore, we shall consider a range of parameters where the vapor pressure in the film is negligible compared to Laplace's capillary pressure. Therefore the droplet remains almost exactly spherical in this regime. This will yield the condition (3) derived below, valid under the constraint $h \ll R$. This condition happens to be
impossible to satisfy if the droplet becomes too small, that is if its weight is too small to balance the upward pressure in the gap between the hot plate and the droplet. Therefore, it is natural to guess that, when this happens, the droplet lifts off the plate. This defines a second regime where $h \gg R$. The scaling laws for this second regime are given in this Letter and we show that the droplet reaches a higher elevation as it gets smaller and smaller by evaporating.

Energy conservation during the evaporation process of the droplet (namely Stefan's boundary condition on the liquid-vapor interface), which we assume to be just below the boiling temperature, and Fourier law for the heat transfer in the film yield the order of magnitude for the vertical velocity of vapor $w$ near the surface of the droplet:

$$
\begin{equation*}
w=\frac{\lambda \delta T}{h L \rho_{v}} \tag{1}
\end{equation*}
$$

Here $\delta T=T_{1}-T_{0}$ is the temperature difference between the droplet and the hot plate, $\rho_{v}$ is the mass density of the vapor, $\lambda$ the heat conductivity in the vapor, and $L$ the latent heat of evaporation per unit mass. Lubrication theory, valid if $l \gg h$, yields the magnitude of the horizontal velocity $u$ in terms of the vertical velocity: $u=\frac{l w}{h}$, where $l$ is the horizontal extent of the vapor film. From the Poiseuille relation, such a flow is driven by a horizontal pressure gradient scaling as $\delta P / l \sim \eta u / h^{2}$. Therefore, the typical gradient is of order $\delta P / l \sim w l \eta / h^{3}$. Using now Eq. (1) we find (replacing sign $\sim$ by $=$ for readability):

$$
\begin{equation*}
\delta P=\eta l^{2} \frac{\lambda \delta T}{h^{4} L \rho_{v}} \tag{2}
\end{equation*}
$$

The liquid drop is at mechanical equilibrium when $M g=\delta P l^{2}$ namely when its weight is equal to the vertical component of the force due to viscous pressure in the gap between the droplet and the hot plate. Note that the contribution of the viscous stress to this vertical force is of the
same order of magnitude as the one of hydrostatic pressure. Therefore we find using the mechanical equilibrium relation given above that:

$$
\begin{equation*}
\frac{l^{4}}{h^{4}}=\frac{L \rho_{v} M g}{\eta \delta T \lambda} \tag{3}
\end{equation*}
$$

As stressed above, the lubrication approximation becomes invalid when $h \sim l$. From the $M$ dependence of the righthand side of Eq. (3), we find that the lubrication approximation becomes invalid if the radius of the droplet is less than a critical drop radius $R_{l}$ defined by the condition $l=h$. The breakdown of the lubrication approximation will then occur for:

$$
\begin{equation*}
R_{l}=\left(\frac{\eta \delta T \lambda}{g L \rho_{v} \rho_{l}}\right)^{1 / 3} \tag{4}
\end{equation*}
$$

Therefore one expects that, as $R$ gets smaller than $R_{l}$, the droplet takes off from the hot plate. The range of values of $h \sim R \sim R_{l}$ is beyond reach of simple order of magnitude estimates and its analysis requires a solution of the full set of equations for the multiphase Stokes flow and the heat transfer model. Let us consider the asymptotic regime where $R$ is much less than $R_{l}$, where one expects the droplet to lift well above the hot plate $(h \gg R)$. In this regime, the equilibrium elevation of the droplet is reached when the gravity force is balanced by the dipolar component of the velocity field generated by the evaporation from the droplet surface and by its image with respect to the horizontal plane. This dipolar approximation is correct for $h \gg R$. Let $T_{1}$ the temperature at infinity and $T_{0}$ the temperature of the droplet. The temperature field satisfying Laplace's equation around an isolated droplet reads: $T(r)=T_{1}+\left(T_{0}-T_{1}\right) R / r$. The origin of the spherical coordinates $(r=0)$ is taken at the center of the droplet. Let us consider now the temperature due to the image with the temperature field of order $T_{i m} \sim\left(T_{1}-T_{0}\right) R / 2 h$ near the physical droplet, with a nearly uniform vertical gradient. As justified below, in the limit of large $h$ the net vertical heat flux is of order of the derivative of $T_{i m}$ with respect to $h$, namely $\left(T_{1}-T_{0}\right) R / h^{2}$. Using Stefan's law we find the order of magnitude of the net vertical velocity in the vapor near the droplet reads:

$$
\begin{equation*}
\frac{\lambda}{L \rho_{v}} \frac{\left(T_{1}-T_{0}\right) R}{h^{2}} \tag{5}
\end{equation*}
$$

This relation is similar to Eq. (1), but with $\delta T / h$ replaced by $\left(T_{1}-T_{0}\right) R / h^{2}$. Multiplying this velocity by $\eta R$, as in the Stokes drag law, we obtain the vertical force on the droplet. Balancing this force with gravity we find that, in the limit $h \gg R$ (namely for $R \ll R_{l}$ ), the dimensionless elevation of the droplet at equilibrium $h^{*}=h / R$ should scale as:

$$
\begin{equation*}
h^{*}=\left(R_{l} / R\right)^{3 / 2} \tag{6}
\end{equation*}
$$

Before going further, we have to analyze the constraint on the pressure in the gap: it must be negligible compared to the Laplace pressure in the droplet to ensure that it remains close to its spherical shape everywhere. It can be shown [9] that $l \sim \sqrt{R h}$ is a fair estimate of the horizontal extent of the layer for which the viscous pressure contributes significantly to the vertical force. Using Eq. (2) and this relation between $l, R$, and $h$, the pressure induced by the Poiseuille flow in the gap is found to be of order $\delta p=$ $g \rho_{l} \frac{R R_{l}^{3}}{h^{3}}$. It crosses the order of magnitude of Laplace's pressure inside the droplet when $\delta P=\frac{\sigma}{R}$. This happens when the radius becomes of order $R_{i}=\left(\frac{\sigma}{g \rho_{l}}\right)^{2 / 7} R_{l}^{3 / 7}$. This relation is obtained using the above geometrical relation for $l$ and Eq. (3) reformulated as $h / l=\left(R_{l} / R\right)^{3 / 4}$. This assumes that the capillary length $\left(\frac{\sigma}{g \rho_{l}}\right)^{1 / 2}$ is much larger than $R_{l}$, since otherwise the cross over would happen in a range of values of $R$ smaller than $R_{l}$ : this is impossible because $R_{i}$ was derived under the assumption that the lubrication approximation holds in the gap between the sphere and the hot plate. The condition $R_{i} \gg R_{l}$ is fulfilled in the experiments described below, but there could be other situations at stake for which this condition may not be fulfilled. This also gives us the opportunity to address another feature of our experiments, namely, the difference of behavior between droplets of water and of ethanol. Since the quantity $R_{i} / R_{l}$ is independent of the radius of the droplet, but depends on the properties of the liquid and its vapor, the behavior of Leidenfrost droplets is not unique to rescalings, because it depends on a dimensionless ratio with a different value depending on the liquid used. Let us also notice that for radii larger than $R_{i}$, the shape of the droplet becomes rather complex, because it depends on the (large) deformation of the droplet surface due to the Poiseuille pressure inside the vapor gap [10,11]. This happens in a range of parameters outside of this study. Therefore, we focus on the range of parameters such that $R_{l} \ll R \ll R_{i}$. In this range, using Eq. (3) and the geometrical relation for $l$, the dimensionless height satisfies:

$$
\begin{equation*}
h^{*}=\left(R_{l} / R\right)^{3 / 2} \tag{7}
\end{equation*}
$$

For usual liquids the value of $R_{i}$ is a few hundred microns. It is therefore worth mentioning that this prediction is qualitatively different and even opposed to the one commonly used for which the vapor thickness is expected to decrease when the radius of the droplet decreases.

The previous relations rely on the assumption that the temperature field between the drop and the substrate (the plane located at $z=0$ ) is a solution of Laplace's equation. This approximation is valid in the limit in which the convective heat flux is negligible compared to the diffusive flux (small Peclet number limit) and it holds in our experiments. From the image solution of potential problems, the temperature field between the drop and the hot plate is the same as the one between two spheres at temperatures


FIG. 1 (color online). Experimental set-up. A cloud of submillimetric droplets is rained toward a silicon wafer inserted in a copper bloc kept at a controlled temperature $T_{1}$. The droplet of radius $R$ is at temperature $T_{0}$ and at a distance $h$ from the substrate.
$T_{0}$ and $2 T_{1}-T_{0}$ and separated by a distance $2 h$. Laplace's equation for two spheres was solved 100 years ago by Jeffery [12] thanks to bispherical coordinates. We have numerically recovered the expected dependence of the temperature gradient in the limits of large $h / R$ and small $h / R$. As given above by scaling arguments, they, respectively, $\operatorname{read} \nabla T \sim \Delta T R / h^{2}$ and $\nabla T \sim \Delta T / h$.

Considering a water drop on a hot plate at $400^{\circ} \mathrm{C}$ the numerical estimate of the critical radius is $R_{l} \simeq 19 \mu \mathrm{~m}$. To our knowledge, no quantitative experiment has been done at such small sizes. We therefore decided to perform experiments on ultradistilled water and ethanol drops to verify the scaling laws derived just above. The experimental setup is depicted in Fig. 1. A cloud of submillimetric droplets is rained on a silicon substrate kept at a controlled temperature $T_{1}$. The two upper blocks are necessary to reduce the number of drops falling in the field of the camera. They are also useful for the thermal stability of the system. Experiments are performed under a laminar air flow protection in order to prevent dust contamination. A high-speed camera, at a frame rate of 2000 frames per second, was used to record several evaporation take off processes. An image analysis allowed us to measure the radius and elevation of droplets as a function of time. The typical error made on these measurements is $2 \mu \mathrm{~m}$. On the top of Fig. 2, we show six pictures taken during the take off of a water droplet. On the bottom of Fig. 2 we plot the height of the water droplet deposited on a silicon substrate at $T=375^{\circ} \mathrm{C}$ and room pressure. It first bounces and lands on the silicon substrate. It then enters in the lubrication regimes in which both radius and vapor thickness decrease with time. At a certain time, the droplet takes off from the substrate (see the movie M1 in the Supplemental Materials [13]).

We recorded several evaporation processes and we represent in Fig. 3 the dimensionless elevation of the droplet $h^{*}$ as a function of its radius $R$. The measurements are in qualitative agreement with the pictures of Fig. 2 (top):


FIG. 2. Top: Pictures of a Leidenfrost droplet and its reflected image on the silicon wafer. Bottom: Height of the droplet as a function of time. After being dropped, it first bounces and lands on the substrate. The droplet then stands on the substrate in the lubrication regime. It finally takes off from the substrate.
almost all droplets take off from the substrate when their radii become of order $R_{l}$. The theoretical prediction given above is tested against experiments. The full line is a best fit with a single parameter $a$ multiplying the predicted critical radius $R_{l}$. We can see that the theoretical prediction fits rather well the experimental data with a value $a=2.2$ close to unity. One can see that there is an important dispersion in sizes at which the droplets take off. It seems that, for the system of water droplets under study, the lift-off is analogous to a subcritical transition (in other words, for the same radius and temperature difference, there are two equilibrium elevations in a certain range of values of $R / R_{l}$ ). The same behavior has been observed for water droplets on substrates at different temperatures. Decreasing the temperature tends to decrease the dispersion of radii at take off. Nevertheless the discontinuous character of the escape from the lubrication regime remains.

We also investigated the behavior of an ethanol Leidenfrost droplet. The same experimental procedure is used and the silicon substrate is kept at similar temperatures as for the study of water Leidenfrost droplets. Unlike water droplets, almost all ethanol droplets do not rebound and land on the substrate (see the movie $M 2$ in the Supplemental Materials [13]). This is due to the lower


FIG. 3 (color online). Dimensionless height of the droplets as a function of their radii. The full line is a best fit to Eq. (6). Note that a minority of droplets fall back on the substrate. This is certainly due to dust contamination. The same data are represented in the inset but in log-log. The dotted line indicates the value of $R_{l}$ for water Leidenfrost droplets on a substrate kept at $T=400^{\circ} \mathrm{C}$.
latent heat of ethanol and therefore to its larger evaporation rate. As a consequence the ethanol droplets enter directly in the regime described above for which $h \gg l$ and we do not observe a transition from the lubrication regime. The experimental results are presented in Fig. 4 in which we plot, as for water droplets, the dimensionless elevation of the droplet $h^{*}$ as a function of its radius $R$. The data are presented for 10 different ethanol droplets on a substrate kept at $T=400^{\circ} \mathrm{C}$. As stressed just above the escape from the lubrication regime is no longer present and the height $h$ of the droplets increases in a continuous manner. In the inset of Fig. 4, we represent the same experimental data but plotted in a log-log representation. The black line corresponds to the scaling law predicted in Eq. (6). A rather


FIG. 4 (color online). Dimensionless height of ethanol droplets as a function of $R$. The substrate is kept at $T=400^{\circ} \mathrm{C}$. The same data are represented in the inset but in log-log. The full line corresponds to the scaling law predicted in Eq. (6).
good agreement is found between the theoretical prediction and the experiments.

In this Letter, we have put in evidence the unexpected behavior of a Leidenfrost droplet in the latter stage of its evaporation. Below a critical size $R_{l}$ the droplets escape from the lubrication regime and take off from the substrate. In an intermediary regime $\left(R_{l} \ll R \ll R_{i}\right)$, the thickness of the vapor film increases as the radius of the droplet decreases. This latter prediction, based upon a detailed analysis of the various physical phenomena involved, is qualitatively different, and even opposed to the one commonly used: as a result of the standard approach to the Leidenfrost phenomenon the vapor thickness is predicted to decrease as the radius of the droplet decreases. The different scaling laws presented in this paper are in semiquantitative agreement with the experimental data obtained on water and ethanol Leidenfrost droplets. In particular, as observed and predicted, the thickness of the vapor film increases as the droplets become smaller. Besides its fundamental interest, this study should find implications in many domains such as, for example, in diesel combustion engines or in heat transfer using cooling spray [14]. We hope that this study will motivate numerical approaches complementary to the present study.
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[9] We consider a film below a spherical drop of thickness $h(r)=h_{0}+r^{2} / 2 R$. Here $r$ is the distance to the center of the drop in cylindrical coordinates and $h_{0}$ the film thickness at $r=0$. Applying the standard lubrication approximation to describe the flow under the drop in evaporation leads to the following relation between $p(r)$ and $h(r)$ :

$$
\begin{equation*}
\frac{d}{d r}\left(\frac{r h^{3}}{12} \frac{d p}{d r}\right)+\frac{r \eta \lambda \delta T}{L \rho_{v} h}=0 \tag{8}
\end{equation*}
$$

After a double integration the pressure field reads:

$$
\begin{equation*}
p(r)=p_{0}-\frac{12 \eta \lambda \delta T}{L \rho_{v}} \int_{0}^{r} \frac{d r_{1}}{r_{1} h^{3}\left(r_{1}\right)} \int_{0}^{r_{1}} \frac{r_{2} d r_{2}}{h\left(r_{2}\right)} \tag{9}
\end{equation*}
$$

where $p_{0}$ is a constant so that the pressure decreases to zero at infinity. Using the expression given just above for $h(r)$ it can be shown that the pressure decreases rapidly to 0 as $r^{-6}$ on a scale length $\sqrt{R h_{0}}$. Therefore $\sqrt{R h_{0}}$ is a fair estimate of the horizontal extent of the layer where the viscous pressure due to the evaporation contributes significantly to the lifting force.
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