

Sedimentation of granular columns in the viscous and weakly inertial regimes

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We investigate the dynamics of granular columns of point particles that interact via long-range hydrodynamic interactions and fall under the action of gravity. We investigate the influence of inertia using the Green's function for the Oseen equation. The initial conditions (density and aspect ratio) are systematically varied. Our results suggest that universal self-similar laws may be sufficient to characterize the temporal and structural evolution of the granular columns. A characteristic time above which an instability is triggered (which may enable the formation of clusters) is also retrieved and discussed.

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Granular materials that are assemblies of discrete macroscopic solid particles with sizes large enough that Brownian motion is irrelevant have been a subject of intensive research during the past few years [1]. They are ubiquitous in our everyday lives and remain at the heart of several geophysical (sand dunes, coastal geomorphology, avalanches, etc.) and industrial processes (chemical, pharmaceutical, food, agricultural, etc.) [1]. The variety of these fields makes these granular materials subject to very different flow and stress conditions. In particular, when the particles are suspended in a fluid, one may expect that subtle hydrodynamic effects should play a leading role [2]. This must be contrasted with the case of dry granular materials for which the influence of the carrying fluid is negligible. In that case both the inelasticity of the collisions and/or the friction between the grains are crucial [1]. While the falling of a single or a couple of particles in purely viscous and weakly inertial regimes was well described by Stokes and Oseen [3], understanding the interactions of a cloud of particles remains a challenge, as complex collective dynamics emerge due to the multiple long-range interactions (e.g., fluidized beds [4,5]). Similar difficulties exist also for n -body gravitational problems. Therefore, many investigations were done in order to better understand the behavior of these particle-laden flows, presenting a large panel of geometries such as jets, streams, drops, and spherical clouds. The sedimentation of spherical clouds of particles, in an external fluid of variable viscosity, has been recently investigated experimentally and numerically [6]. With the exception of the experimental work of Nicolas [7], investigations related to jets or column of particles focused mainly on highly viscous fluids (i.e., zero Reynolds numbers limit) [8,9], air, and moderate vacuum (large Reynolds numbers limit) [10–12] or other kinds of interactions: capillary bridges, van der Waals forces [13–16], etc.

In this paper we present an investigation that fully characterizes, using point-particle simulations, the dynamics of freely falling granular columns in different flow regimes, clarifying the dependence on the Reynolds number, the aspect ratio, and the particle density. The main characteristics of the present system are (i) solid particles suspended in a viscous fluid and

interacting by virtue of the fluid; (ii) particles heavier than the fluid, thus sedimenting on account of gravity; and (iii) no continuous supply of particles in the granular cylinder.

We will first describe the model used for the numerical simulations, defining the characteristic quantities of the problem and its relevant parameters before presenting and discussing our results. At the beginning of the simulation, we randomly initialize the positions of N_0 particles in a cylindrical column of radius R_0 and length H_0 ; the dimensionless particle density $n_0 = N_0/\pi h^*$ is homogeneous ($h^* = H_0/R_0$). In addition to their settling velocity $U_\eta = F/6\pi\eta a$ in the fluid of viscosity η under the action of the gravitational force F , the point particles of radius a are subject to the hydrodynamic pairwise interactions modeled by the dimensionless Green's function of the Oseen equation [2,3,6], which represents the additional velocity induced on a point particle by another point-particle distant by $\mathbf{d} = (d_x, d_y, d_z)$:

$$u_k^* = \frac{3}{4}a^* \left(\frac{d_k}{d^2} \left[\frac{2l^*}{d}(1-E) - E \right] + \frac{E}{d} \delta_{kz} \right), \quad k = x, y, z, \quad (1)$$

$$E = \exp \left(- \left(1 + \frac{d_z}{d} \right) \frac{d}{2l^*} \right), \quad a^* = a/R_0, \quad l^* = \eta/U_\eta \rho_f R_0. \quad (2)$$

In Eq. (1), all lengths and velocities were made dimensionless using U_η as a reference velocity and R_0 as a reference length. A reference time $\tau_\eta = R_0/U_\eta$ was also defined. Here ρ_f is the mass density of the external fluid and l^* represents the importance of the viscous effects. Note that the velocity given by Eq. (1) is the solution to the corrected Navier-Stokes equation, which models the weakly inertial regime:

$$\rho_f(\mathbf{U}_\eta \cdot \mathbf{grad})\mathbf{u} = -\mathbf{grad} p + \eta \Delta \mathbf{u}, \quad (3)$$

where p is the fluid pressure. By choosing the frame of reference moving with the terminal settling velocity of an isolated particle, we compute all the $N_0 - 1$ interactions on each particle and obtain a set of equations describing the motion of the particles, of the form

$$\frac{dM_{ki}}{dt} = \sum_{j \neq i} u_k^*, \quad k = x, y, z; \quad i = 1, N_0; \quad j = 1, N_0. \quad (4)$$

This equation is integrated using an Adams-Bashford time-marching algorithm and at each iteration we obtain the

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Cartesian position $M = (x, y, z)$ of each particle. The detection of the interface of a granular column is performed by dividing axially the domain into h^* overlapping volumes. For each volume, the radial position of the interface is calculated by calculating the mean radial position of the farthest particles. The parameters for the simulations are the aspect ratio h^* , the particle density n_0 , l^* , and a^* . However, we note that Eq. (1) is linear with respect to a^* and therefore the dynamics of the problem will vary linearly with it. As a consequence, we set $a^* = 0.05$ for all simulations. As our simulations neglect particle-particle collisions, they are only applicable to dilute regimes.

It is interesting to write the particle Reynolds number as $Re_p = a^*/l^* = aU_\eta\rho_f/\eta$. Variation in this problem is performed by varying η ; however, as we are investigating the behavior of a macroscopic object, we have to define a macroscopic Reynolds number $Re = R_0U_{col}\rho_f/\eta$, where U_{col} is the characteristic velocity of a cylindrical column, which can be defined using the settling velocity of a vertical cylinder of aspect ratio h^* in a viscous fluid, hence $U_{col} = P \ln(h^*/2)/2\pi\eta H_0$, P being the macroscopic gravitational force. Calculating the equivalent mass of the column from its volume fraction, one can find that $U_{col} = 3\pi n_0 a^* \ln(h^*/2)U_\eta$ and therefore $Re = 3\pi n_0 \ln(h^*/2)Re_p$.

An example of simulations performed by varying Re are shown in Fig. 1. We observe that all the columns stretch and thin while they fall. We also observe that a leading mushroom-shaped plume forms at the front [8], while a particle leakage can be observed at the rear. For the last instant, we see that the columns lose their cohesion and eventually detach into shorter columns and droplets, which means that a varicose instability grows in time. Considering now the effect of the Reynolds number in relative frames, we see that increasing Re relatively slows down the falling of the columns and increases their effective cohesion. We also observe that the size of the leading mushroom is larger for the same instant. It is important to understand that, in order to compare them,

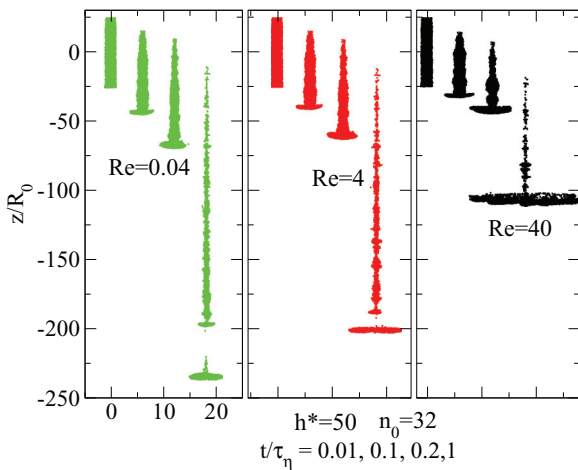


FIG. 1. (Color online) Falling of cylindrical granular columns for $Re = 0.04, 4, \text{ and } 40$ with an aspect ratio $h^* = 50$ and particle density $n_0 = 32$. Four different instants are shown, i.e., $t/\tau_\eta = 0.01, 0.1, 0.2,$ and 1 , and time increases from left to right. The columns are shown in the reference frame of an isolated particle falling at its settling velocity.

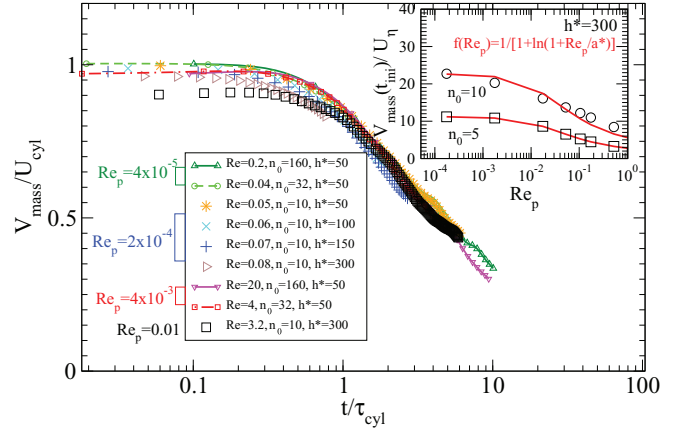


FIG. 2. (Color online) Variation of the reduced velocity of the center of mass $V_{\text{mass}}/U_{\text{cyl}}$ versus reduced time t/τ_{cyl} for $Re_p = 4 \times 10^{-5}, 2 \times 10^{-4}, 4 \times 10^{-3}, \text{ and } 10^{-2}$; $h^* = 50, 100, 150,$ and 300 ; and $n_0 = 10, 32,$ and 160 , with $U_{\text{cyl}} = U_{\text{col}}/[1 + \ln(1 + Re_p/a^*)]$ and $\tau_{\text{cyl}} = H_0/U_{\text{cyl}}$. The inset shows variation of the dimensionless initial velocity of the center of mass V_{mass}/U_η versus Re_p for $n_0 = 5$ and 10 and $h^* = 300$ (symbols denote simulations and the lines the analytical functions).

columns for different Re were represented in different frames. As the viscosity of the fluid for $Re = 0.05$ is much larger than the viscosity for $Re = 50$, columns at large Re in the absolute frame will experience a faster dynamics. These results are qualitatively comparable to those of Pignatel *et al.* [6], which showed that increasing Re enhances effective cohesion and slows the falling of spherical clouds of particles.

Figure 2 shows the time variation of the center of mass V_{mass} reduced by a corrected characteristic velocity of the column U_{cyl} . Indeed, when varying Re_p at fixed h^* and n_0 , we observed a correction in V_{mass} that was not taken into account in U_{col} . This correction is shown in the inset of Fig. 2, where V_{mass}/U_η decreases with Re_p following a logarithmic behavior. We successfully retrieved this behavior by the function $f(Re_p) = 1/[1 + \ln(1 + Re_p/a^*)]$ and in order to take into account the Re_p dependence of the dynamics, we defined a new characteristic velocity $U_{\text{cyl}} = 3\pi U_\eta n_0 a^* \ln(h^*/2) f(Re_p)$ along with a macroscopic characteristic time $\tau_{\text{cyl}} = H_0/U_{\text{cyl}}$. Finally, we observe in Fig. 2 that for a large set of different parameters, the whole temporal evolution of $V_{\text{mass}}/U_{\text{cyl}}$ collapses into a single universal curve. It shows that for $t \ll \tau_{\text{cyl}}$, the columns fall with a constant velocity U_{cyl} before decreasing with time following a logarithmic behavior when $t \gg \tau_{\text{cyl}}$. This confirms that U_{cyl} and τ_{cyl} are the adequate velocity and characteristic time that describe the falling of the columns.

The variation of the particle mean density $\langle n(t) \rangle/n_0$ versus dimensionless time t/τ_η is presented in Fig. 3. For different Reynolds number and initial particle densities, we observe a first incompressible regime where $\langle n(t) \rangle$ is almost constant followed by a weakly compressible regime where the mean particle density experiences a slow time decay. While in the main figure there seems to be different dynamics, the inset of Fig. 3 shows that using the characteristic time τ_{cyl} provides a better collapse of the data. In addition, we see that

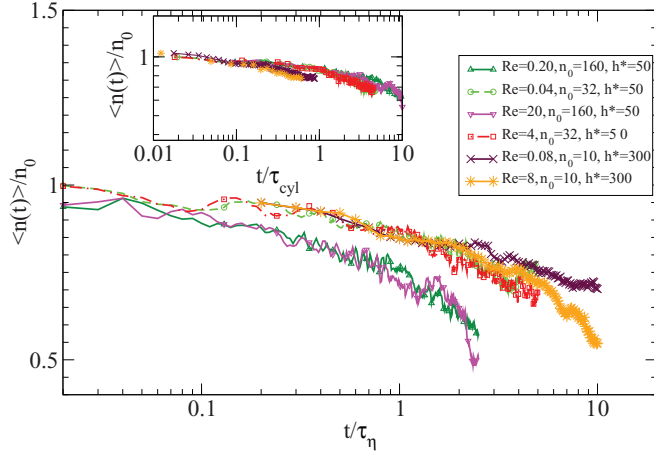


FIG. 3. (Color online) Variation of the reduced particle mean density $\langle n(t) \rangle / n_0$ versus dimensionless time t / τ_η for $Re_p = 4 \times 10^{-5}$ and 4×10^{-3} and $n_0 = 32$ and 160 . The inset shows the variation of the reduced particle mean density $\langle n(t) \rangle / n_0$ versus the reduced time t / τ_{cyl} for the same parameters.

$t \ll \tau_{cyl}$ corresponds to an incompressible regime, while $t \gg \tau_{cyl}$ corresponds to a weakly compressible flow.

The deformations of the columns are displayed in Fig. 4. It provides an adequate description of the dynamics of both the reduced length $H(t) / H_0$ and of the reduced mean radius $R(t) / R_0$ (calculated excluding the extremities of the column). Once again, the dynamics of the column deformation for a large set of different parameters h^* , n_0 , and Re_p is represented by universal curves. When $t \ll \tau_{cyl}$ the columns remain undeformed, while for $\tau_{cyl} < t < 10\tau_{cyl}$ the length increases following a universal scaling as $H(t) \sim H_0(t / \tau_{cyl})^{2/3}$ and the mean radius decreases as $R(t) \sim R_0(t / \tau_{cyl})^{-1/3}$. Assuming a weakly compressible flow for $t > \tau_{cyl}$ (in agreement with Fig. 3), the volume of the column has to remain constant,

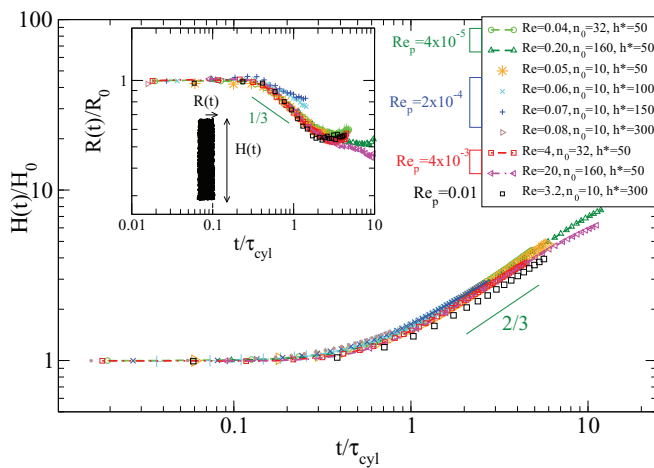


FIG. 4. (Color online) Variation of the reduced length of the column $H(t) / H_0$ versus reduced time t / τ_{cyl} for $Re_p = 4 \times 10^{-5}$, 2×10^{-4} , 4×10^{-3} , and 10^{-2} ; $h^* = 50, 100, 150, \text{ and } 300$; and $n_0 = 10, 32, \text{ and } 160$. The inset shows the variation of the mean reduced radius of the column $R(t) / R_0$ versus reduced time t / τ_{cyl} for the same set of parameters.

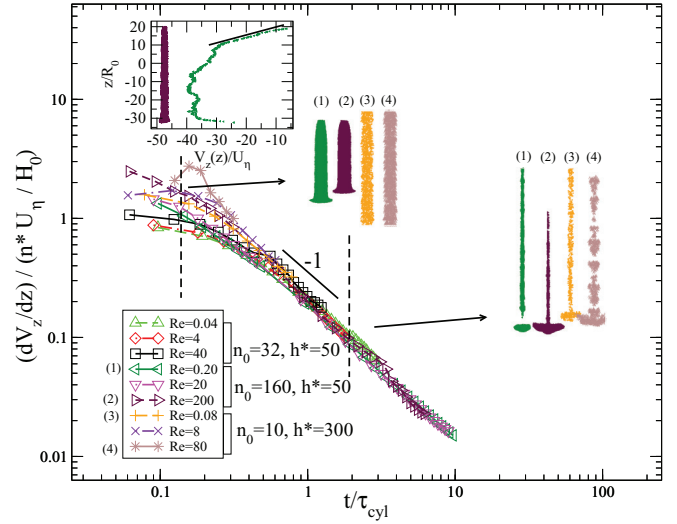


FIG. 5. (Color online) Variation of the reduced axial velocity gradient $(dV_z/dz) / (n^* U_\eta / H_0)$ versus reduced time t / τ_{cyl} for $Re = 0.04, \dots, 200$; $h^* = 50, 300$; and $n_0 = 10, 32, 160$ with $n^* = 2\pi n_0$. The inset shows the shape of a column (left) axial position z / R_0 versus particle axial velocity V_z / U_η (right). The black line shows the linear behavior of V_z with z .

i.e., $\pi R(t)^2 H(t) \sim \pi R_0^2 H_0$, which is well recovered by the previous scaling laws.

Now let us focus on the strain rate dV_z/dz selected at a local scale. It is an important parameter to describe the elongational stretching applied to the columns. It is known that stretching stabilizes liquid columns and prevent instabilities from growing and forming satellite drops [17]. Figure 5 provides a universal curve representing the variation of the reduced axial velocity gradient $(dV_z/dz) / (n^* U_\eta / H_0)$ versus reduced time t / τ_{cyl} , where a different set of parameters presents a good collapse. The elongation rate, or axial velocity gradient (whose extent grows with time along the column), is deduced from the axial velocities of the particles at the rear of the columns, as shown in the inset. We see clearly that in the incompressible regime ($t < \tau_{cyl}$), the elongational rate remains constant and scales like $n^* U_\eta / H_0$. This scaling comes from the fact that a single particle is on average surrounded by $2N_0 / h^* = n^*$ particles (i.e., the particles contained in a sphere of diameter $2R_0$), therefore its characteristic velocity is $n^* U_\eta$ while its characteristic axial length is H_0 . In the weakly compressible regime ($t > \tau_{cyl}$), dV_z/dz decays like t^{-1} . This is consistent with an incompressible self-similar decay of the column radius $R(t) \sim R_0 t^\alpha$ that gives $(dV_z/dz) = -\frac{2}{R} \frac{dR}{dt} \sim t^{-1}$ independently of the thinning exponent α . Although not strictly comparable as they perform event-driven simulations of streams of particles interacting via collisions and cohesive forces and not via hydrodynamic interactions, Ulrich and Zippelius [16] showed a similar result in the case of particles that fall in vacuum under the action of gravity. In that case the elongational rate is simply retrieved from the incompressibility condition and the velocity field imposed by the free fall. Finally, Fig. 5 also displays snapshots of columns at different Reynolds numbers. We observe that for $t \ll \tau_{cyl}$, the columns are cohesive and destabilization has not yet occurred, while

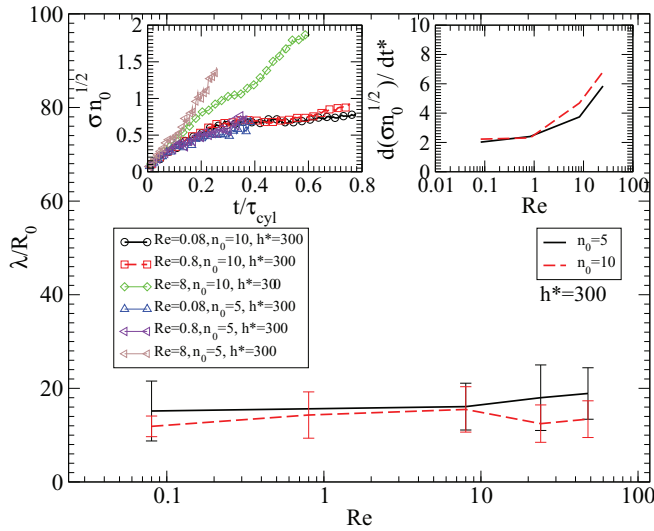


FIG. 6. (Color online) Variation of the reduced most unstable wavelength λ/R_0 versus Re for $n_0 = 5$ and 10 and $h^* = 300$. The left inset shows the variation of the standard deviation of the radial variation σ versus reduced time t/τ_{cyl} for $n_0 = 5, 10$; $Re = 0.08, 0.8, 8$; and $h^* = 300$. The right inset shows the variation of $d(\sigma n_0^{1/2})/dt^*$ (calculated at short times) versus Re for $n_0 = 5, 10$ and $h^* = 300$ with $t^* = t/\tau_{cyl}$.

the columns for $t > \tau_{cyl}$ show a clear destabilization due to the development of a varicose instability.

Finally, let us focus on the description of the instability that leads to the destabilization of the columns. The main features of the instability are shown in Fig. 6. In the main panel of Fig. 6, we note that the value of the most unstable wavelength λ is almost constant and shows no clear dependence on the Reynolds number (λ was deduced from the interface profile). In the regime $Re \ll 1$, we found $\lambda \sim 15R_0$ for $n_0 = 5$ and $\lambda \sim 12R_0$ for $n_0 = 10$, which are both consistent with the values found in earlier investigations [8,9] dedicated to the effect of n_0 . The inset of Fig. 6 shows the temporal evolution of the standard deviation of the reduced radial variation (excluding the front drop) $\sigma n_0^{1/2}$ for $n_0 = 5$ and 10 and for

$Re = 0.08, 0.8, 8$. We see that the data collapse for $Re \ll 1$, in good agreement with the results of Crosby and Lister, who suggested that the growth of the standard deviation of the reduced radial variation is mainly due to fluctuations in the average number density of particles along the axial distance about its mean value [9]. However, σ seems to present larger values for $Re \gg 1$. This means that increasing the Reynolds number may have a noticeable effect on the varicose instability. This induces a stronger effective cohesion and leads to a more efficient destabilization. These observations provide another route to the instability of granular jets along with the recently observed clustering due to cohesion and liquid bridges between grains [14,15]. Furthermore, our results suggest that the sedimentation of particle-laden jets may eventually furnish an interesting system to study the compressible Rayleigh-Plateau instability as suggested recently [18].

To conclude, we have shown that universal scaling laws fully characterize the dynamics of free-falling granular columns in viscous fluids. The characteristic velocity U_{cyl} scales linearly with the particle density, while it shows a logarithmic increase with the aspect ratio and a decreasing logarithmic correction with the particle Reynolds number. A universal characteristic time τ_{cyl} based on U_{cyl} and the column length H_0 has also been retrieved. When $t < \tau_{cyl}$, the flow could be considered as incompressible and the columns deform only slightly and are subjected to a constant strain rate n^*U_η/H_0 while falling at a constant velocity U_{cyl} . For $t > \tau_{cyl}$, we showed that the flow was weakly compressible and that the columns were subjected to an elongational rate decaying like t^{-1} , while they stretched like $t^{2/3}$ and thinned like $t^{-1/3}$ before the development of a varicose instability leading to a long wavelength destabilization. Finally, we found that the most unstable wavelength of the instability of the order of $\sim 10R_0$ is almost independent of inertia corrections, while the growth rate of the most unstable mode shows a clear increase with the Reynolds number.

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