

Multibaker map for shear flow and viscous heating

László Mátyás,¹ Tamás Tél,¹ and Jürgen Vollmer^{2,3}

¹*Institute for Theoretical Physics, Eötvös University, P. O. Box 32, H-1518 Budapest, Hungary*

²*Fachbereich Physik, Universität Essen, 45117 Essen, Germany*

³*Max Planck Institute for Polymer Research, Ackermannweg 10, 55128 Mainz, Germany*

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A consistent description of shear flow and the accompanying viscous heating as well as the associated entropy balance is given in the framework of a deterministic dynamical system. The laminar shear flow is modeled by a Hamiltonian multibaker map which drives velocity and temperature fields. In the appropriate macroscopic limit one recovers the Navier-Stokes and heat conduction equations along with the associated entropy balance. This indicates that results of nonequilibrium thermodynamics can be described by means of an abstract, sufficiently chaotic, and mixing dynamics. A thermostating algorithm can also be incorporated into this framework.

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I. INTRODUCTION

Shear flows provide one of the paradigms of transport processes [1–5]. The importance of chaos in the equations underlying macroscopic shearing has recently been addressed by various numerical studies [6–9], which to some extent were supported by kinetic theory [3,9] and rigorous mathematical work [7,10]. In contrast, however, a simple, exactly solvable model based on a low-dimensional chaotic dynamics—whose mixing property would be the cause of irreversibility—has not yet been established. For material and heat transport such types of model have helped to understand the physical content of thermostating schemes used in numerical simulations [11–14] (see, however, [15] for open questions). In the present article we introduce a similar model for shear flows in the hope that it can also serve such a purpose. The approach will be based on multibaker maps. Previous work in this spirit described the phenomena of diffusion [16–18], conduction in an external field [19–22], chemical reactions [23], thermal conduction [24], and cross effects due to the simultaneous presence of an external field and heat conduction [25,26]. These models are based on an abstract dynamics, rather than on microscopic particle trajectories. The appropriate definition of heat is therefore still not settled. In the present model for shear flow, however, the temperature has a source, which follows from the conservation laws of the dynamics, and can naturally be called viscous heating.

Our aim is to model a sheared fluid confined between two parallel walls at the coordinates $x=0$ and $x=L$ (Fig. 1). The flow is assumed to be two dimensional in the (x,y) plane. Shear is induced by prescribing different y components of the average velocities \mathbf{v} of particles close to the respective walls. In order to make the calculations more transparent, we confine the discussion to cases where the driving is sufficiently weak to induce only a laminar flow, i.e., to cases where the velocity of particles is always directed in the vertical direction such that $\mathbf{v}=(0,v(x))$. For this system we establish a local entropy balance that covers time dependent effects and does not rely on the implementation of boundary conditions.

Three different boundary conditions for dealing with the dissipated heat are considered. (i) In the simplest case the system is isolated. A stationary linear velocity profile emerges in that case, and the temperature becomes uniform. No steady state is reached, however, due to a constant increase of temperature in response to the viscous heating. In addition, we consider systems where (ii) there is a bulk thermostat uniformly taking out the viscous heat, and (iii) the temperature is fixed to the same value at both boundaries so that the asymptotic temperature profile is stationary, but no longer uniform.

The paper is organized as follows. In Sec. II we recall basic notions of irreversible thermodynamics that are to be recovered in a suitable continuum limit of the multibaker dynamics. In Sec. III we introduce the model, and establish the evolution equations for the velocity and the temperature field. This allows us to address the entropy dynamics and its balance equation (Sec. IV). Subsequently, in Sec. V the macroscopic limit of the resulting equations is worked out. The global behavior at different boundary conditions is compared

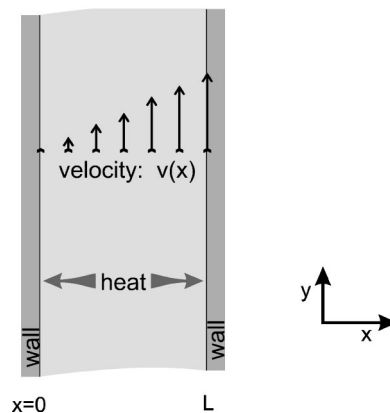


FIG. 1. Graphical illustration of the shear flow. The system is confined between two walls at positions $x=0$ and L . The walls move relative to each other in the y direction, thus inducing a velocity profile $v(x)$ indicated by vertical arrows. For a fixed temperature at the walls this leads to an accompanying heat flow in the x direction (gray arrows).

to irreversible thermodynamics in Sec. VII, and conclusions are drawn in Sec. VIII.

II. IRREVERSIBLE THERMODYNAMICS

In this section we recall the thermodynamic description of shear flows accompanied by viscous heating. The picture is simplified by considering an incompressible fluid at constant pressure.

A. Transport equations

For a system with constant density and pressure the temperature T is the only relevant state variable, and for a complete description one also has to specify the velocity field \mathbf{v} of the fluid [1,2]. The thermodynamic state variables are the velocity field \mathbf{v} and the temperature T [2]. Mass conservation is expressed by a continuity equation. For incompressible fluids the uniform mass density ρ implies that the flow is divergence-free, i.e.,

$$\partial_i v_i = 0. \quad (1)$$

Here $i = x, y$ labels the components of the local flow velocity $\mathbf{v} \equiv (v_x, v_y)$, and we adopted the Einstein convention, i.e., summation over repeated indices. The equation of motion for the velocity components is given by the Navier-Stokes equation. For the case of a negligible pressure gradient it reads

$$\frac{d}{dt} v_i = \nu \partial_j \partial_j v_i, \quad (2)$$

where ν is the kinematic viscosity, and d/dt is the total time derivative.

The system of equations is closed [2] by the equation

$$\frac{d}{dt} T = \frac{\lambda}{\rho c_V} \partial_i \partial_i T + \frac{1}{2} \frac{\nu}{c_V} (\partial_k v_l + \partial_l v_k) (\partial_k v_l + \partial_l v_k) \quad (3)$$

for the temperature evolution. Here, c_V is the specific heat at constant volume, and λ is the thermal conductivity.

B. Entropy balance

The balance equation of the entropy density s is

$$\partial_t s = \sigma^{(irr)} + \Phi, \quad (4)$$

$$\Phi = -\partial_{ij} j_i^{(s)} + \Phi^{(th)}, \quad (5)$$

where $\sigma^{(irr)}$ is the irreversible entropy production reflecting the viscous heating of the flow, Φ the entropy flux, and $\mathbf{j}^{(s)}$ the entropy-current density. The term $\Phi^{(th)}$ models an entropy flux let into a heat bath. It takes nonvanishing values wherever there is a flux into the environment (i.e., for instance, at the boundaries when there is a heat flux through the walls). We call a system a *thermodynamic bulk system* when the term $\Phi^{(th)}$ vanishes. On the other hand, it is convenient to consider also cases with a nonvanishing $\Phi^{(th)}$ in the bulk. We say that a system is subjected to an *ideal thermostat* when the dissipated heat is directly let into the heat

bath. In that case the entropy current vanishes in the steady state, $j_i^{(s)} = 0$, while $\Phi^{(th)}$ is nonzero in the bulk, and counterbalances the steady-state entropy production.

For an incompressible fluid in local equilibrium the Gibbs relation $ds = du/T$ applies locally. The evolution equations can be used to evaluate the terms in Eq. (4). A straightforward calculation yields for the rate of irreversible entropy production (cf. for instance [1, Chap. XII. Eq. (23)])

$$\sigma^{(irr)} = \lambda \frac{(\partial_i T)(\partial_i T)}{T^2} + \frac{\nu \rho}{2T} (\partial_j v_k + \partial_k v_j) (\partial_j v_k + \partial_k v_j). \quad (6)$$

The associated entropy current takes the form [1, Chap. XII. Eqs. (22) and (24)]

$$j_i^{(s)} = -\lambda \frac{\partial_i T}{T}. \quad (7)$$

It depends only on the local temperature and its gradient. The flow velocity \mathbf{v} does not enter.

C. Laminar flow

For a laminar flow driven by prescribed nontrivial y components of the velocity at the two walls, the velocity field at any position (x, y) takes the form $\mathbf{v} \equiv (0, v(x))$ (see Fig. 1). The x component of the velocity vanishes, and the profile is translationally invariant in the y direction (parallel to the walls). We restrict our investigation to cases where the same holds for the temperature such that $T = T(x)$. Consequently, for laminar flow the transport equations take the form

$$\partial_t v = \nu \partial_x^2 v, \quad (8a)$$

$$\partial_t T = \frac{\lambda}{\rho c_V} \partial_x^2 T + \frac{\nu}{c_V} (\partial_x v)^2, \quad (8b)$$

while the rate of irreversible entropy production $\sigma^{(irr)}$ and the entropy current $j^{(s)}$ can be written as

$$\sigma^{(irr)} = \lambda \left(\frac{\partial_x T}{T} \right)^2 + \frac{\nu \rho}{T} (\partial_x v)^2, \quad (9a)$$

$$j^{(s)} = -\lambda \frac{\partial_x T}{T}. \quad (9b)$$

The scalar current $j^{(s)}$ denotes the x component of the entropy current, and an analogous convention is adopted for all currents. The y components of the currents vanish in the setting considered.

III. THE MULTIBAKER MAP

In order to model the laminar flow we divide the plane into square cells of size $a \times a$ that are large enough, on the one hand, to admit thermodynamically meaningful averages, but, on the other hand, sufficiently small to neglect gradients across cells. The cells are considered as the regions used in irreversible thermodynamics to define local equilibrium vari-

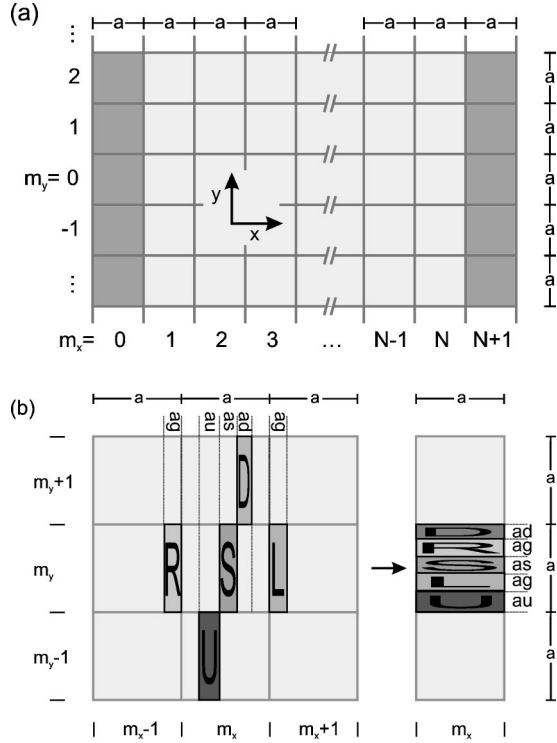


FIG. 2. Graphical illustration of the action of the multibaker map on its phase space (x,y) . The indices labeling the columns and rows are given on the lower and left margins, respectively, while their width is indicated at the upper and right margins. (a) The mapping is defined on a domain of $N+2$ identical columns of square cells of size $a \times a$ that are labeled by the indices $m_x = 0, \dots, N+1$ and $m_y = -\infty, \dots, \infty$. Boundary conditions on the flow are implemented in the shaded cells $m_x = 0$ and $N+1$. (b) The action of the map on regions that are mapped into cell (m_x, m_y) . The contraction and expansion for these regions is indicated by the deformation of the tags (R, U, S, D, L) in the different branches of the map.

ables. The system shown in Fig. 1 is represented by a rectangular array of $N \equiv L/a$ cells in the horizontal direction, and an infinite number of cells vertically [Fig. 2(a)]. Cells are labeled by the indices $m_x = 0, \dots, N+1$, and $m_y = -\infty, \dots, \infty$. All cells have the same dynamics except the outermost ones where it is modified to implement boundary conditions.

A. Action of the mapping in the (x,y) plane

After each time unit τ every cell is divided into five columns [Fig. 2(b)]. The rightmost (R) and leftmost (L) columns have width ag . They are mapped onto a strip of height ag in cell (m_x+1, m_y) and cell (m_x-1, m_y) , respectively. The left column (U) of widths au is mapped upward onto a strip of height au in cell (m_x, m_y+1) , and the right one labeled by (D) downward into (m_x, m_y-1) , respectively. Region S stays within the cell. In all cases the area of the strips is preserved.

This dynamics is driving two fields. Denoting the composite index (m_x, m_y) as \mathbf{m} , these fields are (i) the velocity field $v_{\mathbf{m}}$ describing the mean flow velocity $v(x,y)$ in cell \mathbf{m} ;

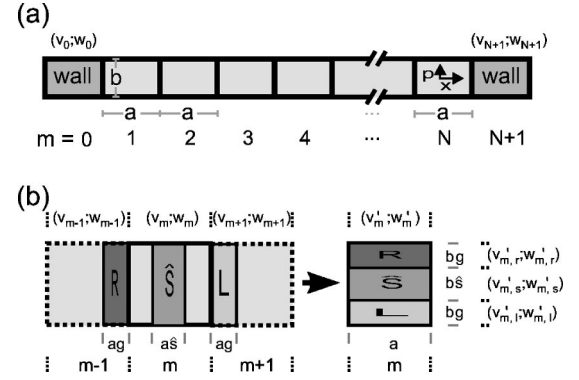


FIG. 3. Graphical illustration of the (x,p) multibaker representation of the laminar flow. (a) Domain of the map. The outermost cells (indicated as dark gray boxes) are again used to implement boundary conditions. (b) Action in the bulk. The average values of the fields $v(x,y)$ and $w(x,y)$ in the cells [cf. Eqs. (12) and (18)] and strips [cf. Eqs. (11) and (19)] are given on the margins.

(ii) an energy field $w_{\mathbf{m}}$ that represents the kinetic energy of peculiar kinetic energy).

The dynamics on this two-dimensional lattice can be considered as a model of the velocity and energy transport in the configuration space. In order to obtain a faithful representation of the entropy balance, however, one has to consider the phase-space dynamics. To define the dynamics in the analog of a μ space, we take into account the translation invariance of the problem. The velocity and energy fields can take on different values in the columns $m_x = 0, \dots, N+1$ of Fig. 2(a), but the fields have to be uniform within every column. In this respect it is not necessary to follow the dynamics in the y direction, and one achieves a quasi-one-dimensional dynamics in an (x,p) space, where p represents a momentumlike variable of the model.

B. Action of the mapping in the (x,p) space

The domain of the multibaker representation in the (x,p) space is shown in Fig. 3(a). It comprises a chain of $N+2$ cells of size $a \times b$ that for sake of more condensed notation are labeled by the index m (instead of m_x). The middle N cells represent the bulk, and two additional ones are used to implement boundary conditions (cf. Sec. VI). The parameter b sets the momentum scale. It will not play any role in thermodynamic considerations.

In order to maintain the same dynamics in the transport direction in the two representations of the flow, each cell is divided into three columns of size ag , $a\hat{s}$, and ag , where g is the same as above and $\hat{s} = 1 - 2g$. The left and right columns of cell m are mapped into a strip of height ag in cell $m+1$ and cell $m-1$, respectively, as shown in Fig. 3(b). The middle column of size $a\hat{s}$ is squeezed and stretched onto a strip of height $b\hat{s}$ and remains in the same cell.

This multibaker dynamics drives the velocity and energy fields. Their values might depend on the phase-space coordinate. Hence, we are dealing with a bivariate distribution of the velocity $v(x,p)$ and peculiar kinetic energy $w(x,p)$ within each cell m . Only the cell averages v_m and w_m appear

in the transport equations. The dependence of $v(x,p)$ and $w(x,p)$ on the phase-space coordinates contributes essentially to the entropy dynamics, however.

C. The dynamics of the velocity field

The mass density ρ_m is proportional to the average phase-space density ϱ_m in cell m , i.e.,

$$\rho_m = Mb\varrho_m, \quad (10)$$

where M is a constant of dimension mass. When interpreting the mass density or associated quantities from the point of view of the two-dimensional flow, ρ_m is to be understood as a mass density in the x coordinate per unit length in the y direction. Hence, $\rho_m v_m$ represents the preserved momentum density (per unit length) of the hydrodynamic flow. Its evolution expresses momentum conservation. As a consequence, the updated values for the velocity on the strips (L, \hat{S}, R) after one time unit are [see the right side of Fig. 3(b)]

$$\begin{aligned} \rho'_m v'_{m,l} &= \rho_{m+1} v_{m+1}, \\ \rho'_m v'_{m,s} &= \rho_m v_m, \\ \rho'_m v'_{m,r} &= \rho_{m-1} v_{m-1}, \end{aligned} \quad (11)$$

where $v'_{m,l}$, $v'_{m,s}$, and $v'_{m,r}$ stand for the velocities of the flow in the regions (L, \hat{S}, R) of cell m , respectively. The prime indicates that the updated values of the field are considered. The average momentum $\rho_m v_m$ of the full cell is the average of the contributions in the different strips, i.e.,

$$\rho_m v_m = (g\rho_{m,r}v_{m,r} + \hat{s}\rho_{m,s}v_{m,s} + g\rho_{m,l}v_{m,l}) \quad (12)$$

at any instant of time. If the velocity is initially uniform in the full cell (i.e., the values of v in all strips agree), then due to Eqs. (12) and (11) the average velocity of cell m becomes after one time step

$$\rho'_m v'_m = (1-2g)\rho_m v_m + g\rho_{m-1}v_{m-1} + g\rho_{m+1}v_{m+1}. \quad (13)$$

Observing that the mass density ρ is uniform and constant in time, the updated value of the cell velocity v_m is found to be

$$v'_m = v_m + g(v_{m-1} + v_{m+1} - 2v_m). \quad (14)$$

This evolution can be written in the form of a discrete balance equation

$$\frac{v'_m - v_m}{\tau} = -\frac{j_{m+1}^{(v)} - j_m^{(v)}}{a} \quad (15)$$

with the discrete current defined by

$$j_m^{(v)} = -\frac{a^2 g}{\tau} \frac{v_m - v_{m-1}}{a}. \quad (16)$$

In the boundary columns $m=0$ and $N+1$ the dynamics will be augmented by force terms (Sec. VI) in order to fix the

velocity to the constant values $v_0 \equiv v_L$ and $v_{N+1} \equiv v_R$, respectively, irrespective of the momentum flowing into these cells.

D. The dynamics of the energy field

The full kinetic energy e_m of cell m is obtained by integrating $e_m \varrho_m$ over the volume ab of the cell. At any instant of time it is the spatial average of the energies $e_{m,l}$, $e_{m,s}$, and $e_{m,r}$ of the different strips,

$$e_m = g e_{m,l} + \hat{s} e_{m,s} + g e_{m,r}. \quad (17)$$

The difference between the energy e and the translational specific kinetic energy $Mv^2/2$ of the flow defines the peculiar kinetic-energy density $w \equiv e - Mv^2/2$, whose macroscopic limit will be proportional to the local temperature. Therefore, on the strip $i=l,s,r$ in cell m one observes densities $w_{m,i}$ of the peculiar kinetic energy that satisfy

$$e_{m,i} = \frac{M}{2} v_{m,i}^2 + w_{m,i},$$

while at the same time the coarse-grained kinetic energy e_m obeys

$$e_m = \frac{M}{2} v_m^2 + w_m.$$

Using these definitions and the averaging rule (17) for the energy one finds

$$\begin{aligned} w_m &= g w_{m,l} + \hat{s} w_{m,s} + g w_{m,r} + \frac{M}{2} [g v_{m,l}^2 + \hat{s} v_{m,s}^2 + g v_{m,r}^2 \\ &\quad - (g v_{m,l} + \hat{s} v_{m,s} + g v_{m,r})^2]. \end{aligned} \quad (18)$$

This shows that the average kinetic energy w_m is not the straightforward spatial average of the values $w_{m,i}$ on the strips. Rather, intracell variations of the velocity field (i.e., a nontrivial distribution of the $v_{m,i}$) also contribute to w_m . This property is an immediate consequence of the conservation laws, and is therefore not restricted to multibaker models.

For a thermally closed system the peculiar kinetic energy w is advected by the flow. The values on the strips after one time unit are then

$$\begin{aligned} w'_{m,l} &= w_{m+1}, \\ w'_{m,s} &= w_m, \\ w'_{m,r} &= w_{m-1}. \end{aligned} \quad (19)$$

From this and the update (11) of the velocities the updated peculiar kinetic energy is found to be

$$w'_m = w_m + g(w_{m-1} + w_{m+1} - 2w_m) + \frac{gM}{2} [(v_{m-1} - v_m)^2 + (v_{m+1} - v_m)^2] - \frac{M}{2} \left[a^2 g \frac{(v_{m-1} + v_{m+1} - 2v_m)^2}{a^2} \right]. \quad (20)$$

The first two terms account for a diffusive rearrangement of the peculiar kinetic energy w . Therefore, we attribute the terms proportional to M to the effect of viscous heating in this discrete setting.

In order to model the action of a thermostat, which leads to local changes of the peculiar kinetic energy due to a heat flux into the environment, an additional *thermostat heat source* q_m is incorporated into the update of w_m by multiplying the right-hand side of Eq. (20) by a factor $[1 + \tau q_m]$,

$$w'_m = \left\{ w_m + g(w_{m-1} + w_{m+1} - 2w_m) + \frac{gM}{2} [(v_{m-1} - v_m)^2 + (v_{m+1} - v_m)^2] - \frac{M}{2} g^2 [v_{m-1} + v_{m+1} - 2v_m]^2 \right\} [1 + \tau q_m]. \quad (21)$$

This equation can be rewritten as

$$\frac{w'_m - w_m}{\tau} = Q_m + \frac{a^2 g}{\tau} \frac{w_{m+1} - 2w_m + w_{m-1}}{a^2} \quad (22)$$

with the *full heat source*

$$Q_m = \frac{q_m}{1 + \tau q_m} w'_m + \frac{a^2 g}{\tau} \frac{M}{2} \left[\frac{(v_{m-1} - v_m)^2}{a^2} + \frac{(v_{m+1} - v_m)^2}{a^2} \right] - \frac{\tau}{2} M \left[\frac{a^2 g}{\tau} \frac{(v_{m-1} + v_{m+1} - 2v_m)^2}{a^2} \right]. \quad (23)$$

The equation for the update of w can be rearranged into a balance equation for the heat per unit volume,

$$\frac{\rho}{M} \frac{w'_m - w_m}{\tau} = \frac{\rho Q_m}{M} - \frac{j_{m+1}^{(w)} - j_m^{(w)}}{a}, \quad (24)$$

which comprises the divergence of the discrete ‘‘heat’’ current

$$j_m^{(w)} = - \frac{a^2 g}{\tau} \frac{\rho}{M} \frac{w_m - w_{m-1}}{a}. \quad (25)$$

The first contribution to Q_m in Eq. (23) reflects the action of the thermostat, and the latter two the effect of viscous heating of the fluid. A steady state with a uniform w profile can be found for $Q=0$, which thus mimics an ideal thermostat. In contrast, in a bulk system in the sense of conventional irreversible thermodynamics $q_m=0$, and Q_m vanishes only when the discrete velocity gradients $v_{m+1} - v_m$ and $v_m - v_{m-1}$ across the cell vanish.

Finally, we note that in this model the fields v_m and w_m are passive in the sense that they do not influence the multibaker dynamics. Previous experience with a multibaker map describing thermoelectric cross effects [25] suggests, however, that the present discussion is not affected by a v_m or w_m dependence of the parameter g .

IV. ENTROPIES AND THEIR TIME EVOLUTION

A. The coarse-grained and the Gibbs entropy

The Gibbs entropy for cell m of a multibaker system with a density field $\varrho(x,p)$ and peculiar kinetic-energy field $w(x,p)$ takes the form [27]

$$S_m^{(G)} = -k_B \int_{\text{cell } m} dx dp \varrho(x,p) \ln \left[\frac{\varrho(x,p)}{\varrho^*} w(x,p)^{-\gamma} \right] \quad (26)$$

where γ is a free exponent. Since an initially uniform phase-space density $\varrho(x,p)$ is left invariant by the time evolution one can identify the reference density ϱ^* with $\varrho(x,p)$ and obtain

$$S_m^{(G)} = k_B \gamma \frac{a\rho}{M} \int_{\text{cell } m} \frac{dx dp}{a} \ln w(x,p). \quad (27)$$

Here, we have already replaced the phase-space density by the mass density (10).

The coarse-grained entropy of cell m is based on the cell-averaged coarse-grained value w_m of the kinetic energy $w(x,p)$. For the form (27) of the Gibbs entropy, one obtains

$$S_m = k_B a \gamma \frac{\rho}{M} \ln w_m \quad (28)$$

as the coarse-grained entropy.

In order to discuss the thermodynamic time evolution of entropies, one conveniently starts with uniform densities in every cell [21,14]. In that case the coarse-grained and the Gibbs entropies initially coincide. After one time step, however, they typically differ. The Gibbs entropy has changed due to the fact that the w field takes different values on the strips (R, \hat{S}, L) , leading to the new value

$$\begin{aligned} S_m^{(G)} &= k_B \gamma \varrho a b \{ g \ln [w_{m-1} (1 + \tau q_m)] \\ &\quad + (1 - 2g) \ln [w_m (1 + \tau q_m)] + g \ln [w_{m-1} (1 + \tau q_m)] \} \\ &= k_B \gamma \varrho a b \left\{ \ln [w_m (1 + \tau q_m)] + g \ln \frac{w_{m-1}}{w_m} - g \ln \frac{w_m}{w_{m+1}} \right\}. \end{aligned} \quad (29)$$

On the other hand, the coarse-grained entropy after one time step is

$$S'_m = -k_B a b \gamma \varrho \ln w'_m. \quad (30)$$

B. Entropy balance

The coarse-grained entropy depends only on the average kinetic-energy density w_m , and is therefore considered as the multibaker analog of the thermodynamic entropy. Its temporal change can be decomposed as

$$\frac{\Delta S_m}{ab\tau} \equiv \frac{S'_m - S_m}{ab\tau} = \frac{(S'_m - S_m^{(G)'}) - (S_m - S_m^{(G)})}{ab\tau} + \frac{S_m^{(G)' } - S_m^{(G)}}{ab\tau}, \quad (31)$$

where information-theoretic arguments [20,21,25,14] lead one to identify

$$\frac{\Delta_i S_m}{ab\tau} \equiv \frac{(S'_m - S_m^{(G)'}) - (S_m - S_m^{(G)})}{ab\tau} \quad (32a)$$

with the rate of entropy production, and

$$\frac{\Delta_e S_m}{ab\tau} \equiv \frac{S_m^{(G)' } - S_m^{(G)}}{ab\tau} \quad (32b)$$

with the entropy flux. Note that the second term of the numerator of $\Delta_i S_m$ vanishes due to the initial condition of uniform fields in the cells.

Inserting the values for S'_m and $S_m^{(G)'}$ into the definition (32a) yields

$$\frac{\Delta_i S_m}{a\tau} = \frac{k_B \gamma \rho}{M \tau} \left[\ln \left(\frac{w'_m}{w_m} (1 + \tau q_m)^{-1} \right) - g \ln \frac{w_{m-1}}{w_m} - g \ln \frac{w_{m+1}}{w_m} \right]. \quad (33)$$

Remarkably, this expression for the entropy production does not depend on the source term Q_m , but only on the values of the coarse-grained field w in cell m and its neighbors. The shear flow enters only indirectly through the update w'_m of w_m .

Similarly to the other balance equations, the entropy flux can be written as

$$\frac{\Delta_e S_m}{a\tau} = - \frac{j_{m+1}^{(s)} - j_m^{(s)}}{a} + \Phi_m^{(th)}, \quad (34)$$

where the discrete entropy current $j_m^{(s)}$ takes the form

$$j_m^{(s)} = -k_B \frac{a g}{\tau} \frac{\rho}{\gamma M} \ln \frac{w_{m+1}}{w_m}, \quad (35a)$$

and

$$\Phi_m^{(th)} = k_B \gamma \frac{\rho}{M} q_m \quad (35b)$$

describes the direct flux into the thermostat. Such a flux is encountered whenever there is a nonvanishing source term

q_m . In view of Eq. (23) this finding further supports the interpretation of q_m and Q_m given at the end of Sec. III D.

V. THE MACROSCOPIC LIMIT

In this section we evaluate the expressions of the different quantities considered in Secs. III and IV, and identify conditions for consistency with the thermodynamic results described in Sec. II.

A. Definition of the limit

For macroscopic systems $L \gg a$ (i.e., $N \gg 1$), so that the spatial coordinate

$$x \equiv am \quad (36)$$

is quasicontinuous. Moreover, the microscopic time scale τ is negligible as compared to the viscous relaxation time L^2/ν . Consequently, there is also a clear separation of typical microscopic and macroscopic time scales such that the time can also be considered as a quasicontinuous variable. We denote the scaling limit, where all contributions to the time evolution that explicitly depend on a or τ are neglected, as the *macroscopic limit*. Formally, it can be evaluated as

$$a, \tau \rightarrow 0, \quad (37)$$

such that the kinematic viscosity ν and the spatial coordinate $x \equiv am$ are finite. As mentioned earlier, the field w is assumed to go over into the local temperature $T(x)$ in the macroscopic limit, i.e.,

$$w_m \rightarrow C k_B T(x), \quad (38)$$

where C is a dimensionless constant.

B. The transport equations

The macroscopic form of the velocity current (16) becomes

$$j_m^{(v)} = - \frac{a^2 g}{\tau} \partial_x v. \quad (39)$$

In order to achieve a meaningful thermodynamic result the ratio $a^2 g/\tau$ has to be finite in the limit. Indeed, comparison with Eq. (8a) shows that

$$\nu \equiv \frac{a^2 g}{\tau} \quad (40)$$

is the kinematic viscosity.

Equations (39) and (40) imply that Eq. (14) is the discrete form of the Navier-Stokes equation (8a) for the laminar flow. Moreover, with this choice for g one obtains for the heat current (25)

$$j^{(w)} = - \frac{\rho}{M} \nu C k_B \partial_x T. \quad (41)$$

Hence, Fick's law of heat conduction is recovered with the heat conduction coefficient

$$\lambda = \frac{\rho}{M} \nu C k_B. \quad (42)$$

Due to Eq. (42), the macroscopic limit of Eq. (21) reduces to Eq. (8b) for the temperature evolution:

$$\partial_t T = \frac{\lambda}{C k_B \rho / M} \partial_x^2 T + \frac{\nu M}{C k_B} (\partial_x v)^2 + q T. \quad (43)$$

Comparing the coefficients in this equation with the ones in Eq. (8b), one obtains

$$C k_B = c_V M. \quad (44)$$

The proportionality constant C introduced in Eq. (38) thus corresponds to the specific heat at constant volume (measured in units of k_B).

C. The entropy balance

In the macroscopic limit the rate of irreversible entropy production (33) becomes

$$\frac{\Delta_i S_m}{a \tau} \rightarrow \sigma^{(irr)} = k_B \gamma \nu \frac{\rho}{M} \left(\frac{\partial_x T}{T} \right)^2 + \frac{\nu \rho}{T} (\partial_x v)^2. \quad (45)$$

It fully agrees with the thermodynamic form of the entropy production (9a) when the coefficient $k_B \gamma \nu \rho / M$ in front of the first term is the heat conductivity. In view of Eq. (42) we thus conclude that in our model $\gamma = C$, i.e., the exponent γ appearing in the definition (26) of the entropy is proportional to the specific heat. Hence, the final form of the heat conductivity λ can be settled to

$$\lambda = \frac{\rho \gamma k_B \nu}{M} = \rho c_V \nu. \quad (46)$$

Working out the expression (35a) for the entropy current $j_m^{(s)}$, one finds in the macroscopic limit

$$j_m^{(s)}(x) = -k_B \gamma \nu \frac{\rho}{M} \frac{\partial_x T}{T} = -\lambda \frac{\partial_x T}{T}. \quad (47)$$

In view of Eq. (46) this relation also fully agrees with its thermodynamic counterpart (9b).

VI. BOUNDARY CONDITIONS

In this section we demonstrate how boundary conditions for the shear flow can be implemented in the multibaker dynamics.

A. Boundary conditions for the velocity field

The multibaker dynamics for cell 0 is shown in Fig. 4. (An analogous prescription holds in cell $N+1$.) The action of the strip mapped from cell 0 to 1 fully agrees with that of the corresponding strips in the bulk such that the dynamics of cell 1 agrees with the bulk dynamics of Fig. 3(b). The

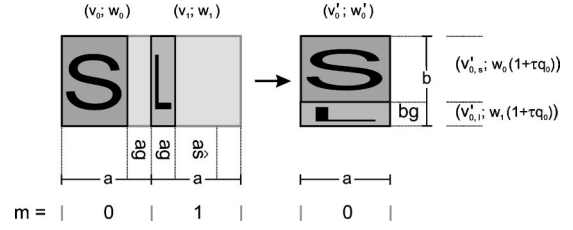


FIG. 4. Implementation of the boundary condition in cell 0. The indication of the width of strips, values of the fields on the strips, and action of the map follows the rules spelled out in Fig. 3.

important differences about the dynamics at the boundary are that (i) there is no column leaving cell 0 to the left, and (ii) the momentum of the particles entering cell 0 is not preserved. Condition (i) reflects that no particles can penetrate the walls of the system, and (ii) reflects that there is a force exerted by the boundary on the fluid. In strip L entering cell 0 (and analogously strip R entering cell $N+1$) the update of the velocity consequently contains the contribution of the external force f_0 (f_{N+1}), leading to

$$v'_{0,l} = v_1 + \frac{f_0 \tau}{g \rho}, \quad (48a)$$

$$v'_{N+1,r} = v_N + \frac{f_{N+1} \tau}{g \rho}. \quad (48b)$$

The update of the coarse-grained velocity of the leftmost cell is

$$v'_0 = v_0 + g(v_1 - v_0) + \frac{f_0 \tau}{\rho}, \quad (49)$$

and an analogous relation holds for cell $N+1$. A shear flow with a prescribed shear rate is enforced by adjusting the forces in such a way that v_0 and v_{N+1} take the respective values v_L and v_R of the velocities at the walls at any time.

In view of the time evolution of v_m , in a steady state [Eq. (14) with $v'_m = v_m$] the asymptotic velocity profile becomes linear,

$$v_m = v_L + \frac{m}{N+1} (v_R - v_L) \equiv v_L + \frac{m}{N+1} \Delta v, \quad (50)$$

irrespective of the temperature distribution in the system.

As in the situation for heat transport described in [14, Sec. 8.1] one has to keep in mind that the implementation (49) of the boundary conditions wrecks the time reversibility of the dynamics. After all, the boundary conditions do not allow reconstruction of the past velocity distribution of volume elements that entered the outermost cells. A thorough discussion of time reversibility in this model and its consequences on the probability distribution of fluctuations lie beyond the scope of the present exposition, however.

B. Boundary conditions for the kinetic-energy density

The modification of the dynamics of the velocities at the boundary also implies changes of the thermostat source

terms. Since the velocity in cell 0 is uniform by definition, the update of w_0 can be found from Eq. (18) where the terms containing $w_{m,l}$ and $v_{m,l}$ are not present since no particles enter cell 0 from the left. Consequently,

$$w'_0 = [w_0 + g(w_1 - w_0)](1 + \tau q_0).$$

This leads to the discrete temporal change

$$\frac{w'_0 - w_0}{\tau} = \frac{q_0}{1 + \tau q_0} w'_0 + \frac{1}{a} \frac{a^2 g}{\tau} \frac{w_1 - w_0}{a} \quad (51)$$

instead of Eq. (22). For a steady state $w'_0 - w_0$ vanishes, and the equation implies [cf. Eq. (25)]

$$a q_0 = - \frac{a^2 g}{\tau} \frac{(w_1 - w_0)/a}{w_0 + g(w_1 - w_0)} = - \frac{j_1^{(w)}}{\varrho [w_0 + g(w_1 - w_0)]}. \quad (52)$$

The right-hand side of this expression is finite in the macroscopic limit, where

$$a q_0 \rightarrow - \nu \frac{\partial_x T}{T} \Big|_{x=0} = - \frac{\nu j^{(T)}(0)}{\lambda T(0)}. \quad (53)$$

Since, however, $a \rightarrow 0$ in the macroscopic limit, the thermostat heat source q_0 cannot be interpreted as a density when there is a finite heat current $j^{(w)}(0)$. Its integral over the cell, $a q_0$, however, stays finite. As a consequence, the heat current has to vanish in a steady state when $q_0 = q_{N+1} = 0$.

VII. DIFFERENT MACROSCOPIC FLOWS

We have seen that in the macroscopic limit the local momentum, energy, and entropy balances for the multibaker map coincide with their thermodynamic forms. This result was achieved by inspecting the local time evolution of the densities without referring to particular boundary conditions, and it is not restricted to steady states. In order to underline these features, we discuss the global transport pictures for three different settings of transport. We emphasize that the considerations immediately generalize to arbitrary time-dependent states although the particular calculations are carried out for stationary coarse-grained velocity fields.

A. Isolated systems

In thermodynamics sheared systems are often considered to be thermally isolated. In that case q_m identically vanishes for all cells $m=0, \dots, N+1$. Equation (51) implies for the current (25)

$$j_1^{(w)} \equiv - \frac{a^2 g}{\tau} \frac{\rho}{M} \frac{w_1 - w_0}{a} = - \frac{a \rho}{M} \frac{w'_0 - w_0}{\tau}. \quad (54)$$

Assuming that the time derivative of w_0 is finite in the macroscopic limit, the current $j_1^{(w)} \rightarrow -a(\rho/M) C k_B \partial_t T(0)$ approaches zero as $a \rightarrow 0$. An analogous argument applies also to $j_{N+1}^{(w)}$.

Thus, for the asymptotic state, the boundary conditions imply that w_0 and w_{N+1} essentially coincide with w_1 and w_N , respectively. Moreover, the viscous heating term Q_m in the bulk depends only on the square of $v_{m+1} - v_m$. The heating is therefore spatially uniform in the long time limit. With this input, one immediately verifies that w_m approaches a spatially uniform value w^* . However, in view of the heat source Q_m in Eq. (23), it constantly grows in time,

$$\frac{w^{*'} - w^*}{\tau} = \nu M \left(\frac{\Delta v}{a(N+1)} \right)^2. \quad (55)$$

This *temporal* evolution of w reflects the rise of temperature due to the entropy production in the system. After all,

$$\frac{\Delta_i S_m}{a \tau} \equiv \frac{k_B \gamma \rho}{\tau M} \ln \frac{w^{*'}}{w^*} = \frac{k_B \gamma \rho}{w^*} \nu \left(\frac{\Delta v}{a(N+1)} \right)^2 + O(\tau)$$

which in the macroscopic limit reduces to the thermodynamically expected value

$$\sigma^{(irr)}(t) = \frac{\rho \nu}{T^*(t)} \left(\frac{\Delta v}{L} \right)^2$$

where $T^*(t) = \text{const} + (\nu/c_V)(\Delta v/L)^2 t$ is the spatially uniform but temporally increasing asymptotic temperature distribution. Note that the flux $\Phi^{(th)}$ and the entropy current vanish in this setting, implying an ever increasing entropy.

B. Systems subjected to an ideal (bulk) thermostat

In a system subjected to an ideal thermostat the viscous heating is instantaneously released into a heat bath. Accordingly, Q_m vanishes for all cells $m=1, \dots, N$ such that q_m can be determined from Eq. (23).

Moreover, according to the results obtained in Sec. VI B we are again dealing with a system with vanishing heat currents through its boundaries, i.e., for the asymptotic state the boundary conditions imply $w_0 = w_1$ and $w_N = w_{N+1}$, and there is no source term Q for the heat. Consequently, w_m approaches a spatially uniform state w^* that is *stationary* in this case. Entropy production arises due to the nontrivial form of q_m [cf. Eq. (23) with $Q_m = 0$]

$$q_m \equiv q^* = - \frac{\nu M [\Delta v/a(N+1)]^2}{w^* + \nu M \tau [\Delta v/a(N+1)]^2}$$

in the bulk [cf. the steady-state velocity profile (50)]. Hence, the irreversible entropy change is

$$\frac{\Delta_i S_m}{a \tau} \equiv - \frac{k_B \gamma b \varrho}{\tau} \ln(1 + \tau q^*) = \frac{k_B \gamma \rho}{M w^*} \nu \frac{\Delta v^2}{a^2(N+1)^2} + O(\tau), \quad (56)$$

and in the macroscopic limit it reduces to the thermodynamically expected value

$$\sigma_m^{(irr)} = \frac{\rho\nu}{T^*} \left(\frac{\Delta v}{L} \right)^2,$$

where T^* is the steady-state temperature. Also in this case there is no entropy current in the steady state. However, at every location in the system there is a nonvanishing entropy flux into the thermostat, which can be formally identified with $\Phi^{(th)}$ defined in Eq. (5):

$$\Phi^{(th)} = k_B \gamma b \varrho q_m \rightarrow - \frac{\rho\nu}{T^*} \left(\frac{\Delta v}{L} \right)^2. \quad (57)$$

It exactly compensates $\sigma^{(irr)}$ such that the entropy indeed is stationary.

C. Thermostating at the walls

Finally, we discuss a steady state in a hydrodynamic bulk system that generates heat flux into the walls due to the prescribed temperatures at the boundaries. There are no thermostat heat sources in the bulk, i.e., $q_m = 0$ for $m = 1, \dots, N$. On the other hand, there are source terms q_0 and $q_{N+1} = q_0$ acting in the two outermost cells that fix the values of w_0 and w_{N+1} (i.e., the temperature) to the same constant value w_0 . To this end the sources counterbalance a macroscopic heat current releasing the viscous heat into the bath at the boundaries [cf. Eq. (52)]. In contrast to the previous cases, the discrete heat current does not vanish at the boundaries. In view of Eqs. (25) and (51) the heat current through the left boundary of the steady-state system is

$$\frac{j_1^{(w)}}{\rho} \equiv -\nu \frac{w_1 - w_0}{a} = \frac{a q_0}{1 + \tau q_0} w_0. \quad (58)$$

Since the dynamics is symmetrical and $w_{N+1} = w_0$, the current at the right boundary takes the same value up to a change of the sign,

$$j_{N+1}^{(w)} = -j_1^{(w)}.$$

In a steady state the cells in the bulk consequently satisfy

$$0 = \rho \frac{w'_m - w_m}{\tau} = \rho \nu \frac{\Delta v^2}{a^2 (N+1)^2} - \frac{j_{m+1}^{(w)} - j_m^{(w)}}{a},$$

leading to a linear profile of the heat current,

$$j_m^{(w)} = a \left(m - 1 - \frac{N}{2} \right) \rho \nu \left(\frac{\Delta v}{a(N+1)} \right)^2. \quad (59)$$

In view of the definition Eq. (25) of $j_m^{(w)}$, this implies a parabolic profile of w in the steady state,

$$w_m^* = w_0 - \frac{am}{2} a [m - (N+1)] M \left(\frac{\Delta v}{a(N+1)} \right)^2, \quad (60)$$

as expected for the temperature profile in a shear flow subjected to identical temperatures at the two ends.

The entropy production in the bulk is related to the spatial variation of the steady-state distribution w_m^* [cf. Eq. (33)],

$$\begin{aligned} \sigma_m^{(irr)} &\equiv - \frac{k_B \gamma \rho}{\tau M} \left[g \ln \frac{w_{m-1}^*}{w_m^*} + g \ln \frac{w_{m+1}^*}{w_m^*} \right] \\ &= \frac{k_B \gamma}{M} \left[\frac{1}{w_m^*} \frac{j_{m+1}^{(w)} - j_m^{(w)}}{a} + \frac{j_{m+1}^{(w)2} + j_m^{(w)2}}{2\rho\nu w_m^{*2}} \right], \quad (61) \end{aligned}$$

where the second equation was obtained by expanding the logarithms to second order in the differences $w_{m+1}^* - w_m^*$, and rearranging terms. Using Eqs. (24), (23), and (59), the first term can be related to the applied shear rate, while the second one represents the contribution to the entropy production arising from the heat flow. Indeed, in the macroscopic limit one recovers in this case both contributions to Eq. (45). (For small shear rates the contribution from the temperature change is, however, negligible.) Correspondingly, there is a finite entropy current $j^{(s)}$ at every point in the system, but only at the boundaries there is a flux into the thermostat. According to Eq. (53) the macroscopic limit of the full entropy flux through the boundaries becomes

$$a\Phi^{(th)} = k_B \gamma b \varrho a q_0 \rightarrow k_B \gamma \nu \frac{\rho}{M} \frac{\partial_x T}{T} \Big|_{x=0}. \quad (62)$$

Since the stationary temperature profile (the macroscopic limit of w_m^*/Ck_B is obtained from Eq. (60) in the form of $T(x) = T(0) - [x(x-L)(M/2Ck_B)](\Delta v/L)^2$, the derivative at the origin is $\partial_x T|_{x=0} = ML(\Delta v/L)^2/(2Ck_B)$. The contribution at the right boundary is the same. Therefore we find for the integrated entropy flux

$$\Phi^{(th,tot)} = - \frac{\rho\nu}{T_0} L \left(\frac{\Delta v}{L} \right)^2, \quad (63)$$

where we used $\gamma = C$. For weak shear this is essentially the same as the integral of the constant flux (57) over the chain. Thus, we conclude that for sufficiently small heat currents thermostating in the bulk and at the boundaries can lead to the *same* global behavior.

The work per unit time done by the external force densities f_0 and f_{N+1} can be evaluated using their form Eq. (48) and the value of the constant velocity gradient

$$a(f_0 v_L + f_{N+1} v_R) = \nu \rho \frac{(\Delta v)^2}{L}. \quad (64)$$

This expression is exactly $-T_0 \Phi^{(th,tot)}$, such that in a steady state the work done by the external forces equals the total heat flux into the thermostat.

VIII. DISCUSSION

We have enlarged the family of multibaker maps by a model for momentum, energy, and entropy transport in viscous hydrodynamic flows. Although the macroscopic problem is of strongly dissipative nature, the proposed multibaker dynamics is area preserving (Hamiltonian). This is to be con-

trasted with previous multibaker models of electric transport [20,21] and thermoelectric cross effects [25,26] where the inclusion of a reversible dissipation mechanism was necessary in order to simulate the effect of thermostating on the particle dynamics. The form in which thermostating appears in the present model is via a heat-source term in the microscopic energy dynamics (which was already present in the model of cross effects [25]). This term, however, does not give rise to phase-space contraction.

The model has the following basic features.

(a) The time evolution of the system can be interpreted as that of weakly interacting particles. The resulting “multibaker” gas obeys the classical ideal-gas equation of state. The particle and heat diffusion coefficients and the kinematic viscosity are proportional to each other, as in the kinetic theory for classical ideal gases [28].

(b) The distribution of a macroscopic velocity does not enter the entropy explicitly. Rather, the shear rate appears in the entropy balance via its influence on the temperature dynamics only.

(c) The connection to a thermodynamic description of transport is achieved by considering fields that are coarse grained in regions of small spatial extension. Their properties are to be contrasted with those of the fields characterizing the microscopic evolution.

(d) Comparing these two levels of description allows us to identify all contributions to the *local* entropy balance, in full consistency with thermodynamics. They apply to both stationary and transient states.

(e) A source term is implemented in the evolution equation of the microscopic kinetic energy. It provides the possibility of implementing local irreversible cooling of the system, i.e., extraction of heat such that states which are permanently warmed up by viscous heating can become stationary. In traditional thermodynamics these terms are present only at the boundaries, and they vanish in the bulk.

(f) It is indicated how the velocity and the kinetic-energy

dynamics can be implemented at the walls in order to achieve correspondence with different macroscopic boundary conditions.

(g) When source terms are present in the bulk, the local entropy balance of nonequilibrium thermodynamics is generalized by introducing at every location an instantaneous flux of entropy (i.e., of heat) into a thermostat (the entropy flux is then no longer the divergence of the entropy current). The dynamics is in that case reminiscent of numerical algorithms based on Gaussian thermostats.

(h) The global entropy balance was worked out, in order to demonstrate that the total heat flux into a thermostat is independent to a large extent of whether thermostating is applied in the bulk or at the walls.

The major interest of the present model lies in the light it sheds on the origin of viscous heating in deterministic models of transport. It was pointed out how fractal structures emerge in multibaker models for a variety of physical settings of shear flow. In all cases the structures arise from the mixing of regions with different local temperatures and flow velocities whose differences are exponentially proliferating to smaller and smaller scales for a nonequilibrium system. One can explicitly follow this redistribution of the kinetic energy, until it reaches the scale of the domains used to define local thermodynamic averages. Motion at that scale has to be considered as contributing to the nondirectional motion, and hence leading to viscous heating. It is *only* due to this coarse-graining mechanism that the macroscopic shear rate appears in the expression of the irreversible entropy production.

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