Multifractality of drop breakup in the air-blast nozzle atomization process

Wei-Xing Zhou* and Zun-Hong Yu

East China University of Science and Technology, P.O. Box 272, Shanghai 200237, People's Republic of China (Received 1 June 2000; published 18 December 2000)

The multifractal nature of drop breakup in the air-blast nozzle atomization process has been studied. We apply the multiplier method to extract the negative and the positive parts of the $f(\alpha)$ curve with the data of drop-size distribution measured using dual particle dynamic analyzer. A random multifractal model with the multiplier triangularly distributed is proposed to characterize the breakup of drops. The agreement of the left part of the multifractal spectra between the experimental result and the model is remarkable. The cause of the distinction of the right part of the $f(\alpha)$ curve is argued. The fact that negative dimensions arise in the current system means that the spatial distribution of the drops yielded by the high-speed jet fluctuates from sample to sample. In other words, the spatial concentration distribution of the disperse phase in the spray zone fluctuates momentarily, showing intrinsic randomness.

DOI: 10.1103/PhysRevE.63.016302

PACS number(s): 47.27.Wg, 47.53.+n, 47.55.Kf, 02.50.Ey

I. INTRODUCTION

The transformation of bulk liquid into sprays and other physical dispersions of small droplets in a gaseous atmosphere is of importance in many agricultural and industrial processes, which includes applying agricultural chemicals to crops, paint spraying, spray drying, food processing, cooling of nuclear cores, combustion, gasification, and some other fields. Due to the complexity of the atomization process, it is too difficult to disclose clearly the mechanism and also impossible to combine in one model all the influence factors, which include equipment dimensions, size and geometry of nozzle, physical properties of the dispersed phase and the continuous phase, and operating mode. Hence, a lot of empirical and semiempirical models have been established so far to describe atomization processes [1]. To elaborate on the distortion and breakup mechanisms of a single liquid droplet injected into a transverse high-velocity air jet, diverse regimes were presented [2-6] that ignore the interaction of multiple droplets.

According to Mandelbrot [7], there exists a scaling principle of drop-size distribution in many physical systems. In Ref. [8], the fractal facet of drop-size distribution was studied with two characteristic parameters, namely the textural and structural fractal dimensions [9]. However, it is not sufficient that only two fractal dimensions are investigated to characterize the singularities of size distribution. The distribution of singularities on the geometry support, which is described by the multifractal spectrum $f(\alpha)$, should be considered [10,11]. Moreover, since intrinsic or practically induced randomness exists in many real systems, the application of the theory of random multifractals, such as turbulence [12] and diffusion-limited aggregation [13], is indispensable. Negative dimensions appear in these cases [14,15], which is a brand of randomness in many cases. (In fact, negative dimensions may be absent in random multifractal measures.)

As always, the measure considered in the theory of random multifractals is constructed through a randomly multiplicative cascade process. Let a cascade begin with mass equal to 1, uniformly spread over [0,1], and let the *n*th cascade stage share at random the mass in a cell of length b^{-n} among *b* subcells of length b^{-n-1} with multipliers M_i ($1 \le i \le b$). Since mass is conserved while it is spread around within a cell, strong conservation rules constrain the multipliers. Here the multipliers M_i are identically distributed with probability density function Pr(M) and independent. From Cramer's theorem of large deviations [16,17], the mass exponent, which is defined by an annealed averaging of moments of the multipliers, namely

$$\tau(q) = -D_0 - \frac{\ln\langle M^q \rangle}{\ln b},\tag{1}$$

is linked with the multifractal spectrum $f(\alpha)$ by the Legendre and inverse Legendre transform [18]. Here, the fractal dimension D_0 is equal to 1. Therefore, we have

$$\alpha(1) = \tau'(q) = -\frac{\langle M^q \ln M \rangle}{\langle M^q \rangle \ln b}$$
(2)

and

$$f(\alpha(q)) = q \alpha(q) - \tau(q) = \frac{\langle M^q \rangle \ln \langle M^q \rangle - \langle M^q \ln M^q \rangle}{\langle M^q \rangle \ln b} + D_0.$$
(3)

In this paper, we will investigate the multifractal nature of the drop breakup in the process of air-blast nozzle atomization, which is a follow-up to the work of Ref. [8].

II. MULTIFRACTAL NATURE OF DROP BREAKUP

A. Experiment

The measurement of the drop-size distribution is carried out using the 58N81 dual particle dynamic analyzer (dual PDA), which is based on the Doppler effect. The focus of the lens used in the experiment is 500 mm. The power of the argon-ion laser generator is 5 W, which generates three pairs of laser beams of green, blue, and purple. The minimal in-

^{*}Corresponding author. Email address: wxzhou@ecust.edu.cn



FIG. 1. Schematic chart of the dual PDA system.

crement of the movement of the measurement point is 0.02 mm. The angle included between the two arms is 63° . The schematic chart of the measurement system is illustrated in Fig. 1.

The diameter of the central passage of the selected nozzle is 3 mm, while the width of the annular space is 11.5 mm. The rake angle of the nozzle is 10° . The liquid phase water passes through the central passage with a flow rate of 0.21 m³/h, while the continuous-phase air speeds through the annular space with a flow rate of 115 m³/h. The measurement is carried out at different spatial positions throughout the spray zone, which covers 324 points with distances of 10–440 mm. The number of validated samples is up to 2000.

A record with 525 287 data points was obtained using the dual PDA sketched in Fig. 1. A portion of the diameter signals of the droplets in the spray zone is illustrated in Fig. 2. The Hurst exponent of the total record is about H=0.81, which show a relatively strong persistence. Therefore, the mass change of the adjacent drops is not large and one can expect Pr(M) to have a relatively great proportion near M = 0.5.



FIG. 2. Portion of the diameter signals of the droplets in the spray zone. Note that the signals are unilateral and the Hurst exponent is about 0.81. Hence, the mass change of the adjacent drops is not large and one can expect that Pr(M) have a relatively great proportion near M = 0.5.



FIG. 3. Comparison between the mass exponents obtained from the multiplier method (dotted lines) and from the randomly multiplicative cascade model (solid lines) for drop breakup in the atomization process.

B. Multifractal nature obtained by using the multiplier method

In order to extract the spectrum of the singularities $f(\alpha)$ from the experimental data, one can use the procedure from the scaling of histograms of multifractal measures, which is essentially a box-counting method [19]. This method works well when the scaling range is wide, and useful statistical information, such as lacunarity, on the iso- α set can be obtained. However, if the scaling range is small, corrections of high order become necessary, which leads to exponentially more work. In order to improve the accuracy and reduce the work when computing the $f(\alpha)$ function, the multiplier method should be utilized [20-23]. This approach is based on the viewpoint that the scaling properties reflecting the self-similar structure of the measure can be described in terms of a repeated composition of a level-independent distribution of multipliers that defines the rearrangement of the measure into small pieces [12,18]. By suitably manipulating these distributions, one can compute the complete $f(\alpha)$ function from Eq. (3). Hence, to compute the D_q , $\tau(q)$, or $f(\alpha)$ function is to obtain the multiplier density $\Pr(M)$.

The random multifractal measure measured in the experiment is composed of 525 287 pieces with equal scale on the interval (0,1). The mass distributed on the *i*th piece is equal to the mass of the corresponding drop m_i . The simplest way of computing Pr(M) is to cover the measure at the *n*th generation with boxes of size $l = 2^{(1-n)}$ and evaluate the mass in each box, then subdivide each of these boxes into pieces and compute the ratios of the masses *M* in the original box to any one of the two subdivided pieces. A relatively accurate way is to evaluate the averaging in Eqs. (1)–(3) in a discrete form. Thus we have

$$\langle g(M) \rangle = 2^{1-n} \sum_{i=1}^{2^{n-1}} [g(M_i) + g(1-M_i)].$$
 (4)

The dotted lines shown in Figs. 3-6 are the mass expo-



FIG. 4. Comparison between the generalized dimensions obtained from the multiplier method (dotted lines) and from the randomly multiplicative cascade model (solid lines) for drop breakup in the atomization process.

nents $\tau(q)$, generalized dimensions D_q , singularity strength $\alpha(q)$, and multifractal spectrum $f(\alpha)$, respectively.

C. Randomly multiplicative cascade model for drop breakup in the atomization process

Let N(dM) denotes the number of multipliers lying in the interval $[M - \frac{1}{2}dM, M + \frac{1}{2}dM]$. The probability density of the multipliers can be calculated by

$$\Pr(M) = \frac{N(dM)}{\Sigma N(dM)} \middle/ dM.$$
(5)

Note that $\Sigma N(dM) = 2^n$. In Fig. 7, we plot all Pr(M) at different spatial positions in the spray zone with dM = 0.001. One can find that these p.d.f.s of multipliers at different positions agree with each other and are hence stable in the spray zone, which implies that drop breakup is homogeneous throughout the spray zone from the viewpoint of the



FIG. 5. Comparison between the strengths of singularities obtained from the multiplier method (dotted lines) and from the randomly multiplicative cascade model (solid lines) for drop breakup in the atomization process.



FIG. 6. Comparison between the multifractal spectra obtained from the multiplier method (dotted lines) and from the randomly multiplicative cascade model (solid lines) for drop breakup in the atomization process. The two results agree remarkably with each other for $q \ge 0$. However, when q approaches -1, the discrepancy between the two methods becomes more and more notable. The dashed line is from the random model with Pr(M) = 1.

probability distribution of multipliers. Since the multipliers from the same mother box are M and 1-M, the resulting multiplier distribution must be symmetrical, that is,

$$\Pr(M) = \Pr(1 - M). \tag{6}$$

We find that the empirical probability density Pr(M) is roughly consistent with the triangular form

$$\Pr(M) = \begin{cases} -3.6719M + 1.1875, & 0 < M \le 0.16 \\ 2.6471M + 0.1765, & 0.16 < M \le 0.5 \\ -2.6471M + 2.8235, & 0.5 < M \le 0.84 \\ 3.6719M - 2.4844, & 0.84 < M < 1 \end{cases}$$
(7)



FIG. 7. The probability density Pr(M) of the multiplier measured from the experiment of atomization. The multiplier distribution is symmetrical to the line M = 0.5. The unit interval (0,1) is divided uniformly in 1000 subintervals. One can fit Pr(M) roughly with a piecewise triangular function, which leads to the analytic results of scaling properties.

Hence, the averaged q-order moments are in the form

$$\langle M^{q} \rangle = \frac{1}{q+2} [-6.3189 \times 0.16^{q+2} + 5.2941 \times 0.5^{q+2} \\ -6.3189 \times 0.84^{q+2} + 3.6719] \\ + \frac{1}{q+1} [1.0110 \times 0.16^{q+1} - 2.6471 \times 0.5^{q+1} \\ + 5.3079 \times 0.84^{q+1} - 2.4844].$$

$$(8)$$

It is obvious that $q_{\text{bottom}} = -1$. The reason is presented in Sec. III. Similarly, we obtain the functions characterizing scaling properties that are shown in Figs. 3–6 as solid lines. The two results agree remarkably with each other for $q \ge 0$. However, when q approaches -1^+ , the discrepancy between the two methods becomes more and more notable. The dashed line in Fig. 6 is from the random multifractal model with Pr(M) = 1.

III. DISCUSSION

A. The lower limit of *q* in the model

In the randomly multiplicative cascade model presented in Sec. II C, we find that there exists a lower limit $q_{\text{bottom}} =$ -1 of parameter q. As a matter of fact, for most of the random multifractal process, q_{bottom} exists and is a finite value that may be either negative or zero, which depends upon the probability distribution of multipliers. For instance, consider a multiplicatively generated random measure whose probability density of multipliers satisfies a power law, namely $\Pr(M) = (x+1)M^x$, where x > -1. The lower limit is a negative number -1-x, and when x tends to -1^+ , q_{bottom} approaches 0^- . Recall that q_{bottom} is also zero in leftsided multifractals [24,25]. However, these two cases are essentially different.

Assuming that Pr(M) can be expanded into the Taylor series at M=0, we have

$$Pr(M) = Pr(0) + Pr'(0)M + \frac{1}{2!}Pr''(0)M^{2} + \frac{1}{3!}Pr'''(0)M^{3} + \cdots$$
(9)

Suppose that $Pr^{(i)}(0) = 0$ for i < n and $Pr^{(n)}(0) \neq 0$. Then, the averaged moment can be expressed in the form

$$\langle M^{q} \rangle = \sum_{i=n}^{\infty} \frac{\Pr^{(i)}(0)}{i!} \int_{0}^{1} M^{q+i} dM.$$
 (10)

Since $\int_0^1 M^{q+1} dM$ has a spot at M = 0 for $q \le -(i+1)$, one can evaluate the spot integral as the limit of the corresponding normal integral, namely

$$\int_{0}^{1} M^{q+i} dM = \lim_{\delta \to 0^{+}} \int_{\delta}^{1} M^{q+i} dM$$
$$= \begin{cases} \lim_{\delta \to 0^{+}} \frac{1 - \delta^{q+i+1}}{q+i+1}, & q < -(x+1), \\ \lim_{\delta \to 0^{+}} \ln \delta, & q = -(x+1) \end{cases}.$$
(11)

We find that $\langle M^q \rangle$ is undefined for $q \leq -(i+1)$, since the limit in Eq. (11) tends to ∞ . By a transformation of $M = e^x$, it is easy to show that $\langle M^q \ln M \rangle$ is only defined for q > -(i+1) as well.

Now consider the case represented in Eq. (7). The integral concerning $\langle M^q \rangle$ has a spot at M=0 and it is obvious that i=0. Hence q_{bottom} is identical to -1.

B. The case of $q \ge 0$ and comparison with uniform distribution

We can find that, in Figs. 3–6, the agreement between the experiment and the model is perfectly good for $q \ge 0$. We also presented an alternative model with Pr(M) = 1 as shown in Fig. 6. The cause is from the breakup mechanism of drops. We have estimated the Weber numbers of drops throughout the spray region according to the experiments. A majority of drops in the spray have Weber numbers lower than the critical value of 12, indicating that these drops lie in the vibrational breakup regime [2]. Meanwhile, the rest drops have Weber numbers between 12 and 21.5, falling in the bag breakup regime. In the vibrational breakup regime, one drop splits into two droplets with the mass ratio of droplet to its mother drop at around 0.5, while in the bag breakup regime, one drop splits into several relatively bigger droplets and many smaller droplets. Therefore, vibrational breakup dominates and bag breakup also arises. In the case of bag breakup, we can regard the mother drop as several dummy drops. These breakup regimes conform to the probability distribution of multipliers. Since a triangular distribution is more precise than the uniform distribution, the multifractal spectrum of the former coincides with that of the experimental result better than the latter.

Consider the case of q=1. Since the first-order moment $\langle M \rangle = 0.5$, we fine that $\tau(1)=0$, and consequently $f(\alpha(1)) = \alpha(1)$. Therefore, the $f(\alpha)$ curve is tangent to the diagonal $f(\alpha) = \alpha$ of the first quadrant. This is a universal nature of the $f(\alpha)$ curve extracted via the multiplier method. The probability density of the multiplier satisfies Eq. (6) for the base 2. Hence, we have $\langle M \rangle = \langle 1-M \rangle$. Thus $\langle M \rangle = (\langle M \rangle + \langle 1-M \rangle)/2 = 0.5$ and $\tau(1) = 0$. More generally, $\langle M \rangle = 1/b$ for any fixed base *b*, which results in the property mentioned above.

For q=0, we have $\tau(0) = -1$ and $f(\alpha(0)) = D_0 = 1$. This is an inevitable ending of the construction that distributes measure everywhere in the geometric support (0,1).

C. The asymptotic behavior near q_{bottom} and ∞

In the tail of the right part of the multifractal spectrum, the decay of the experimental curve is much faster than that from the model. This is also universal when comparing multifractal spectra arising from continuous and discrete multiplier probability distribution. When one deals with the experimental data using the multiplier method, the rules of construction that one can choose is finite. Hence, $\alpha_{\min} = -\ln(\max\{M_i\})/\ln b = 1.48 \times 10^{-4}$ and $\alpha_{\max} = -\ln(\min\{M_i\})/\ln b = 13.25$. However, this is far from being the case when $\Pr(M)$ exists and is continuous. We find that $\alpha \in (0, +\infty)$.

From Eq. (8), $\langle M^q \rangle \sim 1.1875/(q+1)$ when $q \to -1^+$ or $q \to +\infty$. Thus we obtain the asymptotic behaviors of the scaling properties near q_{bottom} and of $q \to +\infty$ as follows:

$$\tau(q) \sim \log_2(q+1),\tag{12}$$

$$D_q \sim -\log_2(q+1)/2,$$
 (13)

$$\alpha(q) \sim \frac{1}{(q+1)\ln_2},\tag{14}$$

$$f(\alpha) \sim \log_2 \alpha - \alpha. \tag{15}$$

Obviously, $\alpha(q)$ behaves like a hyperbolic function when $q \rightarrow +\infty$ or $q \rightarrow -1$. Meanwhile, the $f(\alpha)$ curve behaves like a logarithmic function near q_{bottom} and like a straight line with slope -1 when $q \rightarrow +\infty$. On the other hand, $f(\alpha)$ has a maximum and a minimum when utilizing the discrete multiplier method, which relates to the refinement l of the construction and $\max\{M_i\}$ or $\min\{M_i\}$.

As proved by Mandelbrot and Evertsz [26], a consequence of $\alpha_{\text{max}} = \infty$ is that $q_{\text{bottom}} = 0$, meaning that for q < 0 the summation of q-order moments fails to scale like $\varepsilon^{\tau(q)}$ and the function $\tau(q)$ fails to be defined. Moreover, a consequence of $\alpha_{\min} = 0$ is that $q_{\text{top}} = 1$. It seems that the resultant definition domain of q in our random multifractal model is in contradiction to the consequences mentioned just now. In fact, a latent condition is used in the proof given in Ref. [26]. The presupposition is that $\alpha(0) = \infty$ for the first consequence and $\alpha(1) = 0$ for the second consequence. The proofs can be extended to more general cases. If there exist q_{bottom} and q_{top} that satisfy $\alpha(q_{\text{bottom}}) = \infty$ and $\alpha(q_{\text{top}}) = 0$, one can show that $q_{\text{bottom}} < q < q_{\text{top}}$, which leads directly to the result in the present case.

D. Comparison with log-normal distribution

Deviation of the triangular distribution model from the uniform distribution model is argued in the preceding subsection. It is also necessary to say some words about the log-normal distribution, since it is natural for readers to assume that the multipliers M_i fluctuate according to lognormal distribution as in the turbulence model [27,28]. The log-normality hypothesis comes from the application of the central-limit theorem to argue that $\ln M_i$ should have Gaussian distributions. However, the central-limit theorem cannot be applied to rare events, which are the ones that contribute most to high-order moments [12]. From the log-normality hypothesis, one may find that the multifractal function $f(\alpha)$ is parabolic in the central "bell" near the maximum and symmetric to $\alpha = \alpha(0)$ [15,29]. We may find that the multifractal function with log-normal distribution fits those in Fig. 6 near q=0 remarkably, but the central-limit theorem does not say anything about their form away from the maximum. Moreover, it is easy to see these points in Fig. 7.

IV. CONCLUSIONS

In this paper, the multifractal nature of drop breakup in the air-blast nozzle atomization process has been studied. We applied the multiplier method to extract the negative and the positive parts of the $f(\alpha)$ curve with the data of drop-size distribution measured using the dual PDA, which is based on Taylor's frozen-flow hypothesis. On the other hand, we proposed a random multifractal model with the multiplier triangularly distributed to characterize the breakup of drops. The agreement of the left part of the multifractal spectra between the experimental result and the model is remarkable. The cause of the distinction of the right part of the $f(\alpha)$ curve, which is due to the essence of the multiplier method, was discussed. Comparisons with uniform and log-normal distribution were performed, respectively.

The fact that negative dimensions arise in the current system, namely that of $f(\alpha) < 0$, means that the spatial distribution of the drops yielded by the high-speed jet fluctuates from sample to sample. In other words, the spatial concentration distribution of the disperse phase in the spray zone fluctuates randomly momentarily and shows intrinsic randomness. The randomness comes also from the experimental procedure, since the measurement of drop-size distribution may be considered as randomly oriented one-dimensional cuts through a three-dimensional spray zone, even if the latter comes from a strictly deterministic process.

ACKNOWLEDGMENTS

This research was supported by the National Development Programming of Key and Fundamental Researches of China (No. G1999022103).

- [1] A. H. Lefebvre, *Atomization and Sprays* (Hemisphere, New York, 1989).
- [2] M. Pilch and C. A. Erdman, Int. J. Multiphase Flow 13, 741 (1987).
- [3] L. P. Hsiang and G. M. Faech, Int. J. Multiphase Flow 8, 635 (1992).
- [4] P. K. Wu and G. M. Faech, Atomization Sprays 3, 265 (1993).
- [5] S. S. Hwang, Z. Liu, and R. D. Reitz, Atomization Sprays 6, 353 (1996).
- [6] Z. Liu and R. D. Reitz, Int. J. Multiphase Flow 23, 631 (1997).
- [7] B. B. Mandelbrot, *The Fractal Geometry of Nature* (Freeman, New York, 1982).

- [8] W. X. Zhou, T. J. Zhao, T. Wu, and Z. H. Yu, Chem. Eng. J. 78, 193 (2000).
- [9] B. H. Kaye, A Random Walk Through Fractal Dimensions (VCH, New York, 1989).
- [10] U. Frisch and G. Parisi, in *Turbulence and Predictability in Geophysical Fluid Dynamics*, edited by M. Gil, R. Benzi, and G. Parisi (North-Holland, New York, 1985), p. 84.
- [11] T. C. Halsey, M. H. Jensen, L. P. Kadanoff, I. Procaccia, and B. I. Shraiman, Phys. Rev. A 33, 1141 (1986).
- [12] C. Meneveau and K. R. Sreenivasan, J. Fluid Mech. 224, 429 (1991).
- [13] C. Amitrano, A. Coniglio, and F. D. Liberto, Phys. Rev. Lett. 57, 1016 (1986).
- [14] B. B. Mandelbrot, Physica A 163, 306 (1990).
- [15] B. B. Mandelbrot, Proc. R. Soc. London, Ser. A 434, 79 (1991).
- [16] H. E. Daniels, Ann. Math. Stat. 25, 631 (1954).
- [17] A. Dembo and O. Zeitouni, *Large Deviations: Techniques and Applications* (Springer, New York, 1998).
- [18] B. B. Mandelbrot, in Proceedings of the 1988 Erice Workshop

on Fractals, edited by L. Pietronero (Plenum, London, 1990).

- [19] C. Meneveau and K. R. Sreenivasan, Phys. Lett. A 137, 103 (1989).
- [20] A. B. Chhabra and K. R. Sreenivasan, Phys. Rev. A **43**, 1114 (1991).
- [21] A. B. Chhabra and K. R. Sreenivasan, Phys. Rev. Lett. 68, 2762 (1992).
- [22] B. Jouault, P. Lipa, and M. Greiner, Phys. Rev. E **59**, 2451 (1999).
- [23] B. Jouault, M. Greiner, and P. Lipa, Physica D 136, 125 (2000).
- [24] R. H. Riedi, J. Math. Anal. Appl. 189, 462 (1995).
- [25] R. H. Riedi and B. B. Mandelbrot, Adv. Appl. Math. 16, 132 (1995).
- [26] B. B. Mandelbrot and C. J. G. Evertsz, *Fractals and Disordered Systems*, edited by A. Bunde and S. Halvin (Springer, Berlin, 1996), p. 366.
- [27] A. N. Kolmogorov, J. Fluid Mech. 13, 82 (1962).
- [28] A. M. Obukhov, J. Fluid Mech. 13, 77 (1962).
- [29] B. B. Mandelbrot, Pure Appl. Geophys. 131, 5 (1989).