# Drag force regime in dry and immersed granular media

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The drag force acting on an intruder colliding with granular media is typically influenced by the impact velocity and the penetrating depth. In this paper, the investigation was extended to the dry and immersed scenarios through coupled simulations at different penetrating velocities. The drag force regime was clarified to exhibit velocity dependence in the initial contact stage, followed by the inertial transit stage with a  $F \sim z^2$  (force-depth) relationship. Subsequently, it transitioned into the depth-dependent regime in both dry and immersed cases. The underlying rheological mechanism was explored, revealing that, in both dry and immersed scenarios, the granular bulk underwent a state relaxation process, as indicated by the granular inertial number. Additionally, the presence of the ambient fluid restricted the flow dynamics of the perturbed granular material, exhibiting a similar rheology as observed in the dry case.

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# I. INTRODUCTION

Granular materials exhibit a range of phenomena that resemble macroscopic behavior observed in solids, fluids, and gases, highlighting their unique and universal condensed properties. Despite their significance in engineering and fundamental scientific research [1], a comprehensive and quantitative theory with a solid physical foundation that encompasses all the rich features of granular materials is still lacking. A specific area of investigation focuses on intruder penetration into bulk granular media, a widespread phenomenon encountered in various fields, such as structure-soil interaction in engineering [2], robotics locomotion [3,4], and the astrophysical realm [5]. In addition, intruder penetration in immersed granular media is ubiquitous in multiple realms, such as soil bed erosion by saturated debris flows [6], penetration tests in marine beds [7], and underwater crater formation in geological fields [8]. This process offers valuable insights into granular behavior, as it occurs in different stages where the substrate media exhibit characteristics of both solids and fluids. This suggests that granular media undergo phase transitions, determined by their mechanical behavior, as they shift between different flow regimes [9].

Considerable research efforts have been dedicated to understanding the mechanism of penetration in granular materials. In the quasistatic regime, the resistance encountered during penetration is like that of a regular fluid [10,11], and the modified Archimedean law has been used for predictions [12,13]. However, beyond the quasistatic regime, the proportionality of the force  $F_z$  to the depth z alone is insufficient. An additional term  $F_v$  proportional to the square of the velocity v, representing the inertial effect, is introduced [14-19]. In these cases, the resulting resistance can be estimated by  $F(z, v) = F_z(z) + F_v(v^2)$  when  $v > v_c = \sqrt{2gd_g}$ , with  $v_c$  being the speed of a particle falling under gravity [17]. While the separate contributions of depth and velocity to the drag force are widely discussed in the context of impact processes [14,20,21], the underlying physical justification remains unclear due to the complex interplay between depth and velocity during the dynamic events. This complexity is further amplified in the immersed case, where the response of the fluid-solid mixture substrate becomes intricate. Consequently, previous investigations on this problem are via either a continuum or discrete approach [9,16,22-28]. However, the isolated mechanisms governing the  $F_z(z)$  and  $F_v(v^2)$  terms are yet to be fully elucidated. Recent studies [29,30] have shed light on the distinct nature of the  $F_{\nu}(v^2)$  term, which deviates from theoretical expectations. Nevertheless, a comprehensive understanding of the settlement behavior of granular materials, including momentum transfer and local or nonlocal rheology evidence, remains incomplete, particularly in the context of the immersed conditions. This paper aims to elucidate the underlying mechanism of drag force in both dry and immersed cases, meanwhile uncovering the analogies and correlations between the two scenarios.

## **II. MODEL DESCRIPTION AND NUMERICAL SETUP**

To investigate the coupling mechanisms between velocity (v) and depth (z) and to examine the influence of the ambient fluid, in this paper, we aimed to establish a general numerical approach for understanding the intrusion phenomena. A coupled computational fluid dynamics and discrete element method (CFD-DEM) implemented in the software PFC3D and OpenFOAM model was employed to simulate the impact pen-

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FIG. 1. (a) Particle size distribution (PSD) of polydispersed grains and the numerical model configuration of the dry modeling scenario and (b) numerical model configuration of the immersed modeling scenario.

etration process at a constant velocity ( $v_0$ ). Unlike previous approaches using homogenized particles and fluid, the current model explicitly solved the individual motion of particles and fluid [28]. In this paper, polydispersed grains were utilized to mimic natural granular packing state and prevent crystallization. The rolling resistance contact model, accounting for angular particle shapes, was incorporated to capture the shape effect [31]. In the immersed case, the fluid and particle motion were derived from the numerical solution of the Navier-Stokes equations and Newton's second law of motion, respectively, using a coarse-grid coupled scheme [32].

The simulation setup is depicted in Figs. 1(a) and 1(b). A frictional spherical intruder with a diameter (D) of 2.2 cm  $(6.1d_g, d_g = \text{mean grain diameter})$  and a density of  $7.8 \text{ g/cm}^3$ was initially placed at the bed surface and then forced to penetrate a granular bed at a constant speed  $(v_0)$  ranging from 25 to 500 cm/s. The bed container dimensions were sufficiently large (W/D > 10) to minimize boundary effects, following the size recommendations adopted in the experimental and numerical investigations [29,33]. This configuration also enables the simultaneous capture of both quasistatic and inertial regimes. The granular bed consisted of grains with a diameter  $(d_g)$  in the range of  $3.6 \pm 1.8$  mm, as shown in Fig. 1(a), with a density ( $\rho_g$ ) of 2.6 g/cm<sup>3</sup>. The particle interactions were governed by a contact model developed based on physical principles where the contact behavior among the normal, shear, rolling, and twisting directions has been related by the integration algorithms in the finite contact area, incorporating parameters such as the effective contact modulus  $(E = 7 \times 10^7 \text{ Pa})$ , shape parameter ( $\beta = 0.25$ ), local crushing coefficient ( $\xi_c = 4.0$ ), and friction coefficient ( $\mu = 0.5$ ); further detail can be found in the Supplemental Material [34]. The granular sample was prepared using the undercompaction multilayer method (UCM) [35] and consolidated under the influence of gravity ( $g = 9.8 \text{ m/s}^2$ ). The resulting granular volume packing fraction ( $\phi$ ) was 0.61, indicating a dilatation required for flow and the emergence of the breakage of jamming states during the penetration [18,36]. The time step is autocalibrated by the software during the simulation as  $10^{-6}$  s according to the contact stiffness and particle

mass; meanwhile, kinematic constraints are applied. In the immersed case, the mesh size is selected as the same as the intruder. Water properties were set for the fluid, with a density  $(\rho_f)$  of 1000 kg/m<sup>3</sup> and a kinetic viscosity  $(\nu)$  of  $10^{-6}$  m<sup>2</sup>/s. The time step of fluid is set as  $1e^{-4}$  s fitting the Courant-Friedrichs-Lewy (CFL) condition in CFD, which leads to the data exchange frequency equal to 100. Additional detailed information regarding the numerical method and model setup can be found in the Supplemental Material [34].

# **III. RESULTS AND DISCUSSION**

#### A. Drag force evolution

Figure 2(a) displays the evolution of drag force  $F(z, v_0)$ with the dimensionless penetration depth  $\tilde{z} = z/D$  (normalized by the intruder size) in both dry and immersed modeling scenarios, recalling the complete phenomenon observed in previous studies [29,37]. Through a comprehensive analysis of the drag force F, important insights are gained. Contrary to the expected  $F(z, v) = F_z(z) + F_v(v^2)$  relationship depicted in the inset plot of Fig. 2(b), both dry and immersed cases exhibit distinct trends to reach the depth-dependence stage. As indicated in Figs. 2(a) and 2(b), the beginning of the penetration process (referred to as the initial contact stage) exhibits velocity dependence. A sharp peak, denoted as the peak force  $(F_{\text{peak}})$ , occurs at  $\tilde{z} \sim 0.25$ , like what has been reported in the impact process ( $\tilde{z} \sim 0.125$ ). Subsequently, during the transition stage, fluctuations of varying magnitudes are observed in distinct scenarios (dry and immersed), suggesting the reorganization of the granular medium following intense perturbations [29,30]. Eventually, all  $F(z, v_0)$  curves, with different  $v_0$  values, converge into the same increasing slope  $dF/d\tilde{z}$  in the dry case (referred to as the depth-dependence stage). In contrast, in the immersed case, though in the depth-dependence stage,  $dF/d\tilde{z}$  is still positively correlated with the penetration velocity. The depth at which the stage transition occurs is defined as the characteristic depth  $(z^*)$ , and the corresponding F value is referred to as the characteristic force  $(F^*)$ . The ambient fluid affected the penetration process by attenuating the fluctuations and increasing the magnitude level of the drag force F. This effect is evident in the larger characteristic force  $F^*$  and the subsequent higher  $dF/d\tilde{z}$ values in the depth-dependence stage of the immersed case.

#### **B.** Regime identification

The distinct intrusion characteristics, including the peak force  $F_{\text{peak}}$ , characteristic force  $F^*$ , and characteristic depth  $z^*$ , have been examined in detail to provide a comprehensive description of the different stages. Figure 3(a) presents the scaling law between the peak force  $F_{\text{peak}}$  and penetration velocity  $v_0$ . Interestingly, the linear correlation observed in both dry and immersed cases contradicts previous findings [29] of a quadratic dependence. However, this linear relationship between  $F_{\text{peak}}$  and  $v_0$  aligns with experimental results related to drag force in plow or upward drag problems [36,38]. This deviation from the previously observed quadratic dependence can be attributed to the breakup of the jamming state, during which the granular bulk transitions from a static state to a flow regime [39,40]. The dilatancy characteristic of granu-



FIG. 2. The drag force offered by granular bulk on a spherical intruder vs z in different speeds in (a) dry and (b) immersed modeling scenarios, respectively. The vertical dashed lines delimit the stages, and the inclined dashed lines are the linear fitting. The inset plot in (b): Expected results from the theoretical model,  $\Delta v$ : the incremental penetration velocity of the intruder. The drag force is normalized by the weight of the intruder  $G_{in} = m_{in}g$ , and the penetration velocity is normalized by  $v_c = \sqrt{2gd_g}$ .

lar material, which was accounted for in this paper through rolling and twisting resistances, may contribute to more intense shear-dilatancy behavior in the dense state. The inset plot in Fig. 3(a) demonstrates the gradual convergence of  $F/v_0$  vs  $\tilde{z}$  evolution trend, indicating the velocity-dependence characteristic with distinct viscous behavior in this stage. As shown in Fig. 2(b), the quadratic scaling law between  $F^*$  and  $v_0$  is observed in both immersed and dry modeling scenarios and imply the inertial effect, albeit with different fitting coefficients. Meanwhile, a similar convergence trend of  $F/v_0^2$  in different ranges of penetration depth can be observed in the inset plot, which indicates the collisional momentum transfer



FIG. 3. (a) Correlation between the peak force  $F_{\text{peak}}$  and penetration velocity  $v_0$ . The inset plot is the drag force scaled by the velocity as the function of the penetration depth  $\tilde{z}$ . (b) Correlation between the characteristic force  $F^*$  and penetration velocity  $v_0$ . The inset plot is the drag force scaled by the quadratic velocity as the function of the depth  $\tilde{z}$ , and the separation time is marked as solid blue squares. (c) Correlation between the characteristic depth  $z^*$  and the penetration velocity  $v_0$ . The inset plot is the log-log relationship between the drag force F and penetration depth  $\tilde{z}$ . In (b) and (c), the data points corresponding to intruder velocity <1 m/s were not plotted due to their weak inertial effect.



FIG. 4. (a) The relationship between  $F \sim \tilde{z}$  derived from the numerical results. The delimitation line is marked as a dashed line. The inset plot summarizes the published numerical and experimental results [30,42]. (b) The extracted model adapted to the immersed case. The drag force is normalized by the weight of the intruder  $G_{in} = m_{in}g$ , and the penetration velocity is normalized by  $v_c = \sqrt{2gd_g}$ .

[30]. The observed difference in  $F^*$  caused by the ambient fluid in the transition stage indeed deviates from the initial stage which includes a slight difference in  $F_{\text{peak}}$  caused by the interstitial fluid. This evidence suggests different action mechanisms of fluid in these two different stages (i.e., initial contact, transition). The relationship between  $z^*$  and  $v_0$ , depicted in Fig. 3(c), illustrates the characteristics of dynamic relaxation for the granular bulk during intrusion. The negligible difference between the two cases indicates that the ambient fluid does not affect the intrusion depth required for particle contact network reorganization [41]. Recall the inset plot of Fig. 3(b), the consistency between the depth at which  $F/v_0^2$  deviates from the overlapping collapse trend and the corresponding  $z^*$  is obtained. This observation indicates the progression toward the depth-dependence stage (quasistatic regime) is accompanied by a gradual reduction in the inertial effect, as evidenced by the quadratic velocity dependency relationship.

Filtering the fluctuations provided by the discrete characteristic of granular media, Fig. 4 presents a schematic extracted trend of the penetration process to reflect the main feature of the drag force evolution, which captures the essential characteristics of the initial contact, transition, and depth-dependence stage. The state curves for the linear  $F \sim \tilde{z}$  and quadratic  $F \sim \tilde{z}^2$  functions define the boundaries of different stages. Furthermore, the underlying quasistatic and inertial regimes of these stages are also highlighted. In the inset plot of Fig. 4(a), the experimental and numerical data from previous studies [30,42] are summarized, demonstrating the same power law with different coefficients that confirm the generality of the observed behavior. Despite quantitative deviations, the immersed case follows a similar regime hierarchy to the dry case. A comparison with the ideal pattern of the evolution of the drag force shown in the inset plot of Fig. 2(b) suggests a shared underlying physical nature, while highlighting the different approaches to the depth-dependence regime. The theoretical model neglects the state transformation from the jamming state [39,43] in the initial contact stage, and the progressive evolution of compound components

 $[F_z(z), F_v(v), \text{ and } F_v(v^2)]$  in the transition stage presents a more idealized inheritance mechanism of the inertial effect.

## C. Local measurements

For the mechanical analysis, the local rheology measurement [44] is employed to provide a comprehensive understanding of the effect of the ambient fluid and the underlying mechanisms governing dry and immersed granular materials. The variable protocol begins with the decomposition of the strain rate and stress tensor, denoted as  $\dot{e}$  and  $\sigma$ , into isotropic and deviatoric parts:  $\dot{e} = \dot{\varepsilon} \mathbf{I} + \dot{e}_{d}$  and  $\sigma = -p\mathbf{I}$  $+ \sigma_d$ . Here, **I** represents the unit tensor,  $\dot{\varepsilon} = \frac{1}{3} \text{tr}(\dot{e}) = \frac{1}{3} \text{div } \mathbf{v}$ is the dilation rate,  $\dot{e}_{d}$  is the shear rate tensor, p is the pressure, and  $\sigma_d$  is the shear stress tensor. Scalar quantities corresponding to the invariants of the strain rate and stress tensors are presented, including the dilation rate, pressure, shear rate  $(\dot{\gamma})$ , and shear stress  $(\tau)$ . Further detailed calculation approaches of the physical field can be found in the Supplemental Material [34]. The analysis focuses on an intermediate penetration velocity  $(v_0)$  of 3.0 m/s, chosen to reveal detailed mechanisms. Two measurement circles of the same size as and moving together with the intruder (characteristic length) are selected: the central area directly beneath the intruder and the direct edge next to the intruder at the same vertical position. The spatially averaged approach has been adapted to the lateral monitoring point. As a result, these monitored areas provide insights into the local flow characteristics surrounding the intruder.

The evolutions of the shear rate  $(\dot{\gamma})$  and dilation rate  $(\dot{\varepsilon})$  are presented in Figs. 5(a) and 5(b), respectively, while the timeaveraged quantities are summarized in Table I. Throughout the penetration process,  $\dot{\gamma}$  remains almost constant, with larger values observed in the central area. On the other hand,  $\dot{\varepsilon}$  reaches a stable state once the intruder is fully submerged, with higher values observed in the central area, consistent with  $\dot{\gamma}$ . The spatial distribution of the relevant physical value is illustrated in the inset plots. From the plot of averaged velocity  $\bar{U}$ , the symmetric pattern with the stagnant



FIG. 5. (a) and (b) The evolution of the shear rate  $\dot{\gamma}$  and dilation rate  $\dot{\varepsilon}$  vs penetration depth  $\tilde{z}$  in different regions. The boundary between the dilation and contraction is marked as the horizontal black dashed line in (b). The inset plot is the field distribution of the corresponding properties extracted from the position marked by the vertical red dashed line.

area underneath the intruder was observed, like the findings presented in the experiment [45]. The shear-rate contour shows the coincident results as the curves of the main plot that the highest shear rate emerges underneath the intruder. The similar shear-rate evolution pattern between the different depths discussed here is reflected by the stable state mentioned previously. As for the volumetric strain rate in the inset plot, the intense fluctuation and the spatial distribution feature could be verified qualitatively. Based on the time-averaged results in Table I, the effect of the ambient fluid on the strain rate  $(\dot{e})$  is identified. The interstitial fluid enhances the sheardilation behavior in both edge and central areas, while it has no effect on  $\dot{\gamma}$ . It can be speculated that this effect of the ambient fluid on the strain rate has a synergistic mechanism with the increased pressure observed in the immersed bulk granular media. This suggests a potential rheological explanation for the influence of the fluid based on the higher pressure in the immersed case.

The evolution of stress (including pressure and shear stress) in the central and edge areas is shown in Figs. 6(a) and 6(b), respectively. The significant differences between these two locations indicate the localization of stress beneath the intruder and the emergence of higher stress in the immersed case, providing a mesoscale explanation for the influence of the ambient fluid on the macroscopic drag force. Furthermore, the consistent evolution patterns between shear stress ( $\tau$ ), pressure (p), and drag force (F in Fig. 2) suggest that the resistance is determined by the integration of stress applied to the interface. From the contour, the concentrated stress appears in the bottom area of the intruder; meanwhile,

TABLE I. Time-averaged results of strain rate.

	Immersed		Dry	
	Edge	Center	Edge	Center
Shear rate, $\dot{\gamma}(s^{-1})$ Dilation rate, $\dot{\varepsilon}(s^{-1})$	19.075 1.358	93.064 5.621	21.121 3.86	92.38 7.531

the larger stress level in the immersed case could also be distinguished from the pattern feature.

As one of the key granular properties, the granular temperature T has been considered to essentially affect the origin of the nonlocal behavior [46]. It could be defined as the mean square of the fluctuations of the particle velocity as T = $\langle (v-\langle v \rangle)^2 \rangle$  [47], where  $\langle \ldots \rangle$  computes the spatial averaged value. It can be further normalized as  $T^* = T \rho / p$ , where p is the pressure. Figure 7 illustrates the variation of  $T^*$  and T in regions beneath and surrounding the intruder during the penetration process. The dimensionless temperature exhibits a rapid increasing trend in the transition stage which indicates the inertial granular flow. In addition, combined with the same evolution pattern of the inertial number, it could be derived that the  $T^*$  monitored is correlated with the inertial number, as pointed out in the literature [47]. Regarding the spatial distribution feature, the granular material in the lateral position indicates a high inertial state with intense velocity fluctuations. As shown in the inset plot, after the initial contact stage, the nondimensional granular temperature exhibits a nearly steady state, which is like the time evolution of the shear rate, and subsequently, this consistency states the strong correlation between the two variables. As a result, a stronger kinetic behavior has been observed in the lateral regions near the intruder in both dry and immersed modeling scenarios. In the underneath region, the low-temperature  $T^*$  is observed. The comparison indicates that the ambient fluid has a certain weakening impact on the dimensionless temperature, which originates from the constrained effect provided by the fluid viscous interaction.

It needs to be noted that the granular temperature is related to the nonlocal behavior through the diffuse process and induces creep motion and destruction at some positions with relatively lower energy. The cooling effect provided by the ambient fluid originates from the constraints of the kinetic behavior of the particles, which has potentially changed the nonlocal behavior by decreasing the temperature gradient. However, this topic is beyond the scope of this paper and could be investigated in future work.



FIG. 6. (a) and (b) The evolution of the shear stress ( $\tau$ ) and pressure (*p*) vs penetration depth  $\tilde{Z}$  in different regions. The inset plot in (b) is the corresponding field distribution extracted from the position marked by the vertical red dashed line in (a) and the symbol is on the plot Im: immersed.

#### D. Rheological mechanism

The rheological characteristics of granular media under the influence of intruder are depicted in Fig. 8, for the effective friction coefficient  $\mu = \tau/p$ , viscosity  $\eta = \tau/\dot{\gamma}$ , and the inertial number  $I = |\dot{\gamma}| d/(P/\rho_s)^{0.5}$ . The inertial number Iprovides comprehensive insights and aids in determining the granular flow regime, which is closely related to other granular properties mentioned in previous sections. In Fig. 8(a), the inertial number I increases sharply at the intruder impact and peaks quickly in the transition stage. The value of I in the region surrounding the intruder surpasses the inertial effect limit and eventually returns to the quasistatic state. During this process, the ambient fluid could significantly influence the flow regime of the granular bulk, where the momentum transfer between the fluid and particles slows down the granular flow dynamics through the viscous effect. As shown in the inset plot of Fig. 8(a), the contour of the effective friction coefficient is demonstrated in the transition stage to reflect the correlation between  $\mu$  and I in spatial distribution. It could be observed that the peak values emerge near the intruder,



FIG. 7. The dimensionless granular temperature  $(T^*)$  vs normalized depth  $(\tilde{z})$  in regions beneath and surrounding the intruder for the dry and immersed modeling scenarios. The inset plot shows the evolution of the granular temperature (T).

indicating the main agitated flowing region there. The comparative results of the contour between the immersed and dry cases are consistent with the evolution of inertial number. In the transition stage, the immersed granular materials present a lower value of  $\mu$ , which is expected by the low inertial values illustrated by the main plot. In Fig. 8(b), the time evolution of the viscosity is plotted, as contrary to the trend of inertial number I, the viscosity undergoes a descending and then recovering trend in the transition stage. The inset plot illustrates the spatial distribution of viscosity, in which the agitated region during the penetration process can be clearly identified. The observed peak value underneath the intruder of the immersed scenario indicates the low inertial region among the granular media. Furthermore, the ambient fluid strengthened viscosity during the penetration process, resulting in a higher resistant force, especially with nearly the same shear rate as shown in Table I.

As shown in Fig. 9(a), the parameters I and  $\mu$  are nonlinearly positively correlated, which aligns with the classical local rheology model  $\mu(I) = \mu_s + (\mu_2 - \mu_s)/(I_0/I + 1)$  [48] qualitatively in both immersed and dry cases. In Fig. 9(b), the viscosity  $\eta$  and inertial number I follows a  $\eta \sim I^{-2}$  scaling law. For the granular material, the transition of mechanical responses is always accompanied by the evolution of the granular structures, including the texture and the lifespan characteristic of the contact force. In line with the observed phenomenon, the corresponding structural evolution in the granular bulk during the penetration is revealed and interpreted by the coordination number  $C_n$  in Fig. 9(c). A clear  $C_n \sim I^{-1}$  scaling law between  $C_n$  and I is observed, indicating a decreasing contact in the intensely flowing materials, which is consistent with the results reported in the literature [49]. Combining the evolution of I in Fig. 8(a), after the initial contact stage with a relatively intact contact net, the region surrounding the intruder experiences intense fluidization, with some regions displaying extremely low coordination numbers. This indicates a complete suspension state wherein the collision becomes dominant. Finally,  $C_n$  recovers in the depthdependence stage, indicating the recurrence of the quasistatic



FIG. 8. The evolution of (a) the inertial number I and (b) the viscosity  $\eta$  during the penetration process in the central and edge regions. The inset plots are the contour of the effective friction  $\mu$  [in (a)] and  $\eta$  [in (b)] in the transition stage.

regime. This analysis unveils the microreflection of the inertial number *I* at the grain scale.

During penetration, the ambient fluid restrains the flow dynamics of the granular material, specifically in the low inertial regime. However, it seems that the same rheological characteristic is shared between the dry and immersed cases, as illustrated in Fig. 9(a). In essence, the combination of high  $\eta$  and low *I* led to the low dynamics of the penetration stage for a  $F \sim v_0$  relationship, while the combination of low  $\eta$  and high *I* facilitated the  $F \sim v_0^2$  relationship for high penetration dynamics. This observation also reflects the decisive role of Reynolds number  $\text{Re}_p$  in computing the drag force of Newtonian fluids for a gradually transition from laminar flow to turbulent flow as  $\text{Re}_p$  increases. These findings inspire a homology between *I* and  $\text{Re}_p$  in the granular intrusion process. It needs to be noted that the numerical simulations conducted in this paper manifest the fluid-inertial regime according to the



FIG. 9. (a) The relationship between *I* and  $\mu$ , where the fitting curve (blue line) is the function  $\mu(I) = \mu_s + (\mu_2 - \mu_s)/(I_0/I + 1)$ . (b) and (c) The relationship between the viscosity  $\eta$ , coordination number  $C_n$ , and inertial number *I*.

regime phase from the literature [50]. Therefore, the expected unified rheology of the  $\mu$ -*I* correlation between the dry and immersed cases was observed, which has further validated our work. The mechanism of penetration in the viscous regime will be the next stage in the path approach to the complete unified theory/description.

#### **IV. CONCLUSIONS**

The constant penetration in the granular media, in both dry and immersed modeling scenarios, has been studied using a coupled numerical simulation model. Through the local rheology measurement, the dynamics of the drag force and its underlying mechanisms were explored. Various regimes were observed in the system, including the initial contact stage with  $F_{\text{peak}} \sim v_0$  relationship, signifying viscous behavior, followed by the transition stage characterized by fluidization and viscosity reduction. The depth-dependence regime showed a viscosity and inertial state recovery, and the proposed  $F \sim \tilde{z}^2$  line aligned well with some existing published work. The evolution of local flow characteristics has been checked, and the influence of the ambient fluid was investigated, revealing its constraining effect on granular flow dynamics, resulting in a lower inertial number I and granular temperature  $T^*$ . Nonlinear correlations in  $\mu(I)$ ,  $\eta(I)$ , and  $C_n(I)$  were evaluated and validated in both dry and immersed cases, indicating that the same rheology properties were shared by both scenarios. By disentangling velocity and depth-dependent contributions to the drag force, a general drag force evolution pattern unifying dry and immersed cases was proposed, which captures the common features  $[F_{\text{peak}} = F(v), z^* = F(v), \text{ and } F^* = F(v^2)]$  and states the distinct mechanism from the multiscale perspective. Overall, in this paper, we provided insights into the rheological mechanism in the penetration process for both dry and immersed granular material and the unified characteristics of this phenomenon.

The datasets generated during and/or analyzed during this study are available [59].

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- [1] H. Askari and K. Kamrin, Nat. Mater. 15, 1274 (2016).
- [2] M. Omidvar, J. D. Malioche, Z. Chen, M. Iskander, and S. Bless, Geotech. Test. J. 38, 656 (2015).
- [3] J. Aguilar and D. I. Goldman, Nat. Phys. 12, 278 (2016).
- [4] J. Aguilar, T. Zhang, F. Qian, M. Kingsbury, B. McInroe, N. Mazouchova, C. Li, R. Maladen, C. Gong, M. Travers *et al.*, Rep. Prog. Phys. **79**, 110001 (2016).
- [5] K. R. Housen and K. A. Holsapple, Icarus 163, 102 (2003).
- [6] P. Song and C. E. Choi, J. Geophys. Res. Earth Surf. 126, e2020JF005930 (2021).
- [7] X.-S. Guo, T.-K. Nian, D. Wang, and Z.-D. Gu, Acta Geotech. 17, 1627 (2022).
- [8] L. F. Jansa and G. Pe-Piper, Nature (London) 327, 612 (1987).
- [9] S. Dunatunga and K. Kamrin, J. Fluid Mech. 779, 483 (2015).
- [10] A. Seguin, Y. Bertho, P. Gondret, and J. Crassous, Phys. Rev. Lett. 107, 048001 (2011).
- [11] A. Seguin, Y. Bertho, F. Martinez, J. Crassous, and P. Gondret, Phys. Rev. E 87, 012201 (2013).
- [12] W. T. Kang, Y. J. Feng, C. S. Liu, and R. Blumenfeld, Nat. Commun. 9, 1101 (2018).
- [13] Y. Feng, R. Blumenfeld, and C. Liu, Soft Matter 15, 3008 (2019).
- [14] D. Van Der Meer, Annu. Rev. Fluid Mech. 49, 463 (2017).
- [15] M. Tiwari, T. R. K. Mohan, and S. Sen, Phys. Rev. E 90, 062202 (2014).
- [16] H. Katsuragi and D. J. Durian, Nat. Phys. 3, 420 (2007).
- [17] D. I. Goldman and P. Umbanhowar, Phys. Rev. E 77, 021308 (2008).
- [18] P. Umbanhowar and D. I. Goldman, Phys. Rev. E 82, 010301(R) (2010).
- [19] Z. Peng, X. T. Xu, K. Q. Lu, and M. Y. Hou, Phys. Rev. E 80, 021301 (2009).
- [20] C. S. Bester and R. P. Behringer, Phys. Rev. E 95, 032906 (2017).
- [21] L. A. T. Cisneros, V. Marzulli, C. R. K. Windows-Yule, and T. Pöschel, Phys. Rev. E 102, 012903 (2020).
- [22] X. Zhang, D. Zhang, Y. Wang, S. Ji, and H. Zhao, Granular Matter 25, 18 (2023).
- [23] R. Jewel, A. Panaitescu, and A. Kudrolli, Phys. Rev. Fluids 3, 084303 (2018).
- [24] T. Hossain and P. Rognon, Phys. Rev. Fluids 5, 054306 (2020).
- [25] S. Dunatunga and K. Kamrin, J. Mech. Phys. Solids 100, 45 (2017).
- [26] T. A. Brzinski, III, J. Schug, K. Mao, and D. J. Durian, Phys. Rev. E 91, 022202 (2015).
- [27] S. Agarwal, A. Karsai, D. I. Goldman, and K. Kamrin, Sci. Adv. 7, eabe0631 (2021).
- [28] A. S. Baumgarten and K. Kamrin, J. Fluid Mech. 861, 721 (2019).
- [29] L. K. Roth, Granular Matter 23, 54 (2021).
- [30] L. K. Roth, E. D. Han, and H. M. Jaeger, Phys. Rev. Lett. 126, 218001 (2021).

ing and Physical Sciences Research Council (Grant No. EP/V028723/1), Hainan Province Science and Technology Special Fund (Grant No. ZDYF2021SHFZ264), and the State Key Laboratory of Disaster Reduction in Civil Engineering (Grant No. SLDRCE19-A-06).

- [31] M. Jiang, Z. Shen, and J. Wang, Comput. Geotech. 65, 147 (2015).
- [32] C. Kloss, C. Goniva, A. Hager, S. Amberger, and S. Pirker, Prog. Comput. Fluid Dyn. 12, 140 (2012).
- [33] A. Seguin, Y. Bertho, and P. Gondret, Phys. Rev. E 78, 010301(R) (2008).
- [34] See Supplemental Material at http://link.aps.org/supplemental/ 10.1103/PhysRevE.109.064908 for detailed information about the numerical method, which includes Refs. [44,51–58].
- [35] M. Jiang, J. Konrad, and S. Leroueil, Comput. Geotech. 30, 579 (2003).
- [36] N. Gravish, P. B. Umbanhowar, and D. I. Goldman, Phys. Rev. E 89, 042202 (2014).
- [37] F. Pacheco-Vázquez, G. A. Caballero-Robledo, J. M. Solano-Altamirano, E. Altshuler, A. J. Batista-Leyva, and J. C. Ruiz-Suárez, Phys. Rev. Lett. **106**, 218001 (2011).
- [38] N. Gravish, P. B. Umbanhowar, and D. I. Goldman, Phys. Rev. Lett. 105, 128301 (2010).
- [39] S. R. Waitukaitis and H. M. Jaeger, Nature (London) 487, 205 (2012).
- [40] A. J. Liu and S. R. Nagel, Nature (London) 396, 21 (1998).
- [41] D. D. Carvalho, N. C. Lima, and E. M. Franklin, Phys. Rev. E 105, 034903 (2022).
- [42] X. Ye and C. Zhang, Acta Mech. Sin. 39, 722198 (2023).
- [43] M. B. Stone, R. Barry, D. P. Bernstein, M. D. Pelc, Y. K. Tsui, and P. Schiffer, Phys. Rev. E 70, 041301 (2004).
- [44] A. Seguin, C. Coulais, F. Martinez, Y. Bertho, and P. Gondret, Phys. Rev. E 93, 012904 (2016).
- [45] M. Harrington, H. Xiao, and D. J. Durian, Granular Matter 22, 17 (2020).
- [46] J. Gaume, G. Chambon, and M. Naaim, Phys. Rev. Lett. 125, 188001 (2020).
- [47] W. Han, H. Zhao, and D. Wang, Phys. Fluids 35, 063304 (2023).
- [48] P. Jop, Y. Forterre, and O. Pouliquen, Nature (London) 441, 727 (2006).
- [49] E. Azéma and F. Radjai, Phys. Rev. Lett. 112, 078001 (2014).
- [50] K. F. E. Cui, G. G. D. Zhou, L. Jing, X. Chen, and D. Song, Phys. Fluids **32**, 113312 (2020).
- [51] P. A. Cundall and O. D. Strack, Geotechnique 29, 47 (1979).
- [52] R. Di Felice, Int. J. Multiphase Flow 20, 153 (1994).
- [53] J. Link, L. Cuypers, N. Deen, and J. Kuipers, Chem. Eng. Sci. 60, 3425 (2005).
- [54] J. Zhao and T. Shan, Powder Technol. 239, 248 (2013).
- [55] L. Jing, C. Kwok, Y. F. Leung, and Y. Sobral, Int. J. Numer. Anal. Methods Geomech. 40, 62 (2016).
- [56] C. K. Batchelor and G. K. Batchelor, *An Introduction to Fluid Dynamics* (Cambridge University Press, Cambridge, 1967).
- [57] G. Q. Zhao and D. M. Wang, Powder Technol. **374**, 1 (2020).
- [58] A. Seguin, Granular Matter 22, 48 (2020).
- [59] https://figshare.com/s/cf06f0726b7b2551108e.