

Interplay between activity, elasticity, and liquid transport in self-contractile biopolymer gelsAnne Bernheim-Groswasser^{*,†} and Gefen Livne[†]*Department of Chemical Engineering, Ben-Gurion University, Be'er Sheva 8774624, Israel*Paola Nardinocchi[‡] and Filippo Recrosi[§]*Department of Structural Engineering & Geotechnic, Sapienza Università di Roma, 00184 Roma, Italy*Luciano Teresi^{||}*Department of Mathematics & Physics, Università Roma Tre, 00146 Roma, Italy*

(Received 14 August 2023; accepted 29 November 2023; published 3 January 2024)

Active gels play an important role in biology and in inspiring biomimetic active materials, due to their ability to change shape, size, and create their own morphology. We study a particular class of active gels, generated by polymerizing actin in the presence of cross-linkers and clusters of myosin as molecular motors, which exhibit large contractions. The relevant mechanics for these highly swollen gels is the result of the interplay between activity and liquid flow: gel activity yields a structural reorganization of the gel network and produces a flow of liquid that eventually exits from the gel boundary. This dynamics inherits lengthscales that are typical of the liquid flow processes. The analyses we present provide insights into the contraction dynamics, and they focus on the effects of the geometry on both gel velocity and fluid flow.

DOI: [10.1103/PhysRevE.109.014601](https://doi.org/10.1103/PhysRevE.109.014601)**I. INTRODUCTION**

Self-contractile active gels are usually generated by polymerizing actin in the presence of cross-linkers and clusters of myosin as molecular motors [1–7]. The mechanics of active gels presents interesting characteristics: self-contractions generate internal stresses and stiffen the material, thus driving the network into a highly nonlinear, stiffened regime [2]; morphing from flat to curved geometries can be expected when thin disks of active elastic gels are considered [5]; boundaries affect morphing [3].

A distinctive feature of active gels is the fact that the source that drives the system out of equilibrium is local, rather than at the system's boundaries as in passive gels, where boundary tractions and/or fluxes and changes in the chemical equilibrium of the external ambient are the driving forces [8]. From that, we get the definition of active gels as *soft materials in which detailed balance is broken locally* [9].

The first models of active gels are based on a description of the contraction dynamics within the framework of active generalized hydrodynamics, which deal with gel mechanics, liquid transport, and gel activity [5,8–12]. The characteristics of these model are as follows: (i) the liquid flow is described through the mass conservation law and the Stokes equations; (ii) the overall stress in the gel is decomposed in an elastic

component, borrowed from the linear elasticity, and an active component, which mimics the active contractile stress generated by the embedded motors; (iii) the overall stress satisfies the balance of forces under a friction force resulting from the relative velocity of the gel and liquid components. The friction force and the active stress make gel mechanics, liquid transport, and gel activity fully coupled.

Hydrodynamic models are very accurate in describing the contraction dynamics at the network mesh scale, and less interested in coupling that dynamics with the nonlinear mechanics of active gels, which is strongly affected by the liquid flow and important when the description of shape transitions in active gels is of interest [5]. More recently, the mechanics of active gels has been at the center of a few theoretical studies, set within the framework of nonlinear mechanics. The interactions between elastic stresses and liquid flow have been investigated in the presence of gel activity, which affects the behavior of the material, and they have been included through different approaches [13–15]. The common point of view is that activity provides structural changes of the network, which induce liquid motion within the gel. Differently from generalized hydrodynamics, gel and liquid motion are modeled using the stress-diffusion theory, a refined version of nonlinear poroelasticity where liquid mass conservation governs liquid transport, and Fick's law takes the place of Darcy's law [16–18].

In [13], a dynamic cross-linking mechanism is introduced that drives an evolution of the mechanical stiffness of the polymeric network and brings the system out of thermodynamic equilibrium. The consequent gradient in the chemical potential of the liquid drives the liquid flow in the active gel. In the approach exploited in [14,15] by some of the authors,

*bernheim@bgu.ac.il

†livneg@post.bgu.ac.il

‡paola.nardinocchi@uniroma1.it

§filippo.recrosi@uniroma1.it

||teresi@uniroma3.it

gel activity acts as a local time-dependent source of strain, driven by generalized forces, whose action breaks locally the thermodynamic equilibrium of the system.

Here, we describe the active gel state in terms of the liquid density, the large displacement of the gel, and the active strain, as in [14, 15]. In addition, we introduce the relationships between active strains and changes in the natural mesh size of the polymer, defined as the distance between cross-links at zero free-energy; we solve the transient problem for gel disks of different aspect ratio; with reference to those disks, we discuss the regimes of fast and slow liquid transport; we identify the characteristic times of the contraction dynamics; and we study the changes in the overall stress state in gel disks of different aspect ratio.

The characteristics of this model are as follows: (i) the liquid flow is described through the mass conservation law, which prescribes the change in liquid concentration in the gel and delivers the liquid velocity relative to the gel; (ii) the total large deformation of the gel is the product of an active component, which mimics the contraction generated by the embedded motors, and an elastic component, following the *active strain* approach, which has already been successfully exploited to describe morphing and growth in active materials [19–21]; (iii) the overall stress depends on the elastic component through a nonlinear constitutive equation and satisfies the balance of forces under zero external force; (iv) the generalized forces driving gel activity satisfy a balance equation, equivalent to a flow rule for the local time-dependent active strain.

Finally, it is worth noting that, in the limit of small deformations, the active strain approach yields an overall stress that is the sum of a passive and an active component, as in generalized hydrodynamics [19].

The goal of the model is describing the interactions between activity, elasticity, and liquid transport through a boundary value problems with initial conditions. Changes in boundary and initial conditions allow us to model a variety of dynamical phenomena and, hopefully, to inspire further experiments to improve the design of the active characteristics of the gel and of its relevant mechanics.

Specifically, we aim to reproduce qualitatively the experimental findings presented in [5], where the contraction dynamics of an active gel disk has been followed and described in great detail. In doing so, the analysis of the competitive role of gel contractility and liquid flow in driving the mechanics of the active gel is exploited. It is shown that the shortest lengthscale is relevant for the contraction dynamics, whereas the aspect ratio of the disk (diameter to thickness ratio) affects the evolution of the disk size and the stress distribution.

In Sec. II, the basic characteristics of the active gel model are presented and contrasted with those of standard passive gels. In Sec. III, liquid flow, stresses, and gel contractions are introduced, and the equations driving the transient behavior of the disks are presented under the cylindrical symmetry hypotheses. In Sec. IV, the steady states of the active gel are presented. In Sec. V, the regimes of fast and slow liquid transport are identified, and the contraction dynamics of active gel disks of different aspect ratios is studied through a set of numerical experiments.

II. POLYMER FRACTION AND ACTIVE VOLUME

Differently from passive polymer gels, active gels have the ability to *reorganize* their mesh, that is, to reduce their natural mesh size by means of motor-induced filaments sliding. A few characteristics of the active and passive gel mechanics are contrasted here through a simple analysis to highlight the key elements that can be described by the macroscopic models of passive and active gels [15, 17, 18, 22–24].

The mechanics of passive polymer gels is commonly studied within the Flory-Rehner model [25, 26]. The model assumes the free energy to be the sum of an elastic energy of the network and a mixing energy for the interactions solvent/network. The elastic energy depends on the stretch of the polymer chains from the dry conditions through a nonlinear spring model. The mixing energy depends on the polymer fraction ϕ , that is, the ratio between the volume V_p occupied by the polymer and the current volume v of the gel:

$$\phi = \frac{V_p}{v} \quad \text{with} \quad v = V_p + v_l, \quad (1)$$

where v_l is the volume of solvent content. Formula (1) is based on the assumption that a given mass of polymer occupies a *constant* volume V_p , and any change of the current volume v must be entirely due to the solvent volume v_l . The zero-energy state, that is, the natural state of the gel, corresponds to the dry state ($\phi = 1$). Any change in the solvent content, driven by changes in the chemical potential, stretches the chains, mixes solvent and polymer, and increases the free energy. The balance between the mixing energy, which favors swelling, and the elastic energy, which hampers swelling, yields the thermodynamic equilibrium state.

Our active gel model uses the same assumptions for the free energy, but relieves the constraint of a constant polymer volume. The volume of the polymer can vary because of a change of the natural length of the mesh size due to the pulling of molecular motors, and this new volume v_a is named *active volume*. It is worth noting that V_p and v_a correspond to the same mass of dry polymer; thus, activity, by changing only the gel volume v , varies the ratio between the polymer mass and the overall gel volume, that is, the effective gel density. Moreover, as liquid is expelled during contraction, gel density increases, a phenomenon called *densification*. For the active gel model, the polymer fraction is given by

$$\phi = \frac{v_a}{v} \quad \text{with} \quad v = v_a + v_l. \quad (2)$$

Thus, we may have the same polymer fraction ϕ with different pairs v_a, v_l :

$$\phi = \frac{v_{a0}}{v_{a0} + v_{l0}} = \frac{v_{a1}}{v_{a1} + v_{l1}} \quad \Rightarrow \quad \frac{v_{a1}}{v_{a0}} = \frac{v_{l1}}{v_{l0}} \quad (3)$$

as $1/\phi = 1 + v_{l0}/v_{a0} = 1 + v_{l1}/v_{a1}$. From (3), it follows that a contraction of the polymer network yields a proportional reduction of its solvent content, that is, for $v_{a1} < v_{a0}$ it holds that $v_{l1} < v_{l0}$. For example, if we have $v_{a0} = 1 \text{ mm}^3$ and $v_{l0} = 1000 \text{ mm}^3$, we have $\phi = 1/1001$. We may have the same polymer fraction ϕ , with a contraction that halves the polymer volume, that is, $v_{a1} = 0.5 \text{ mm}^3$, and reduces the solvent content to $v_{l1} = 500 \text{ mm}^3$.

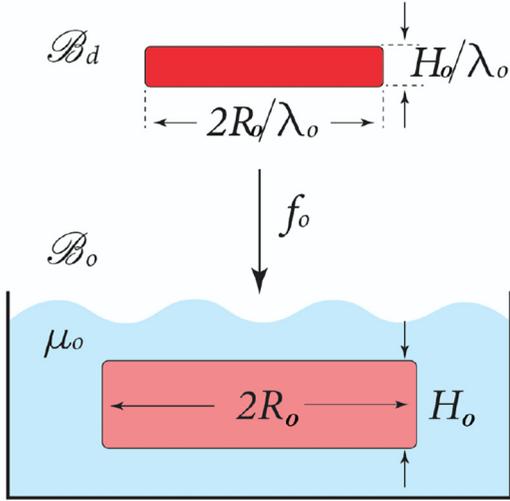


FIG. 1. The disk is dry at the reference configuration \mathcal{B}_d , and swollen at the initial one \mathcal{B}_o . The volume of \mathcal{B}_o is much larger than that of \mathcal{B}_d due to liquid content: H_o and $2R_o$ are the thickness and diameter of \mathcal{B}_o , which are λ_o times larger than the corresponding reference lengths. The initial configuration is given by $x_o = \lambda_o X$, where the stretch λ_o is determined by the bath's chemical potential.

The natural state of the active gel corresponds to $\phi = 1$, and changes in the solvent content can be driven also at constant chemical potential of the bath: liquid flow is generated by active contraction. We anticipate a key feature of the model: to maintain a steady gel volume, that is, a volume that remains constant in time, motor activity is required. This latter is a distinctive feature of active gels compared to passive ones. Indeed, passive gels under external loads stay in their equilibrium state until a change at the system's boundaries occurs. On the contrary, active gels are brought out of thermodynamic equilibrium by the action of local molecular motors [8].

This key point inspired us. The model presents a new evolution equation, which describes gel activity; it is driven by a source term representing the local magnitude of motor activity, which brings the system out of equilibrium [9]. This activity in turn generates a solvent flow in the gel: contraction of the polymer mesh, driven by the motors, yields solvent flow towards the boundary of the body, favoring its release.

We conclude this section by writing the relations between the average mesh sizes of the gel and its volumes. Continuing with the example above, the current mesh size ξ is related to the current gel volume v by $v \sim \xi^3$; likewise, the natural mesh size ξ_a is related to the active volume v_a by $v_a \sim \xi_a^3$. Thus, the ratio between the two active volumes v_{a0} and $v_{a1} = v_{a0}/2$ would scale as $\xi_{a1}/\xi_{a0} = (1/2)^{1/3} \simeq 0.8$. Both ξ_a and ξ may be very different from the reference mesh size ξ_d of the dry polymer (before contraction acts), i.e., the passive one, due to activity and liquid flow, as it has been shown in [5] by fluorescence micrographs of a polymerizing and actively contracting actomyosin network (see the cartoon in Fig. 2).

III. LIQUID FLOWS, STRESSES, AND GEL CONTRACTIONS

The active gel model is formulated in the framework of three-dimensional (3D) continuum mechanics (see [14,15]

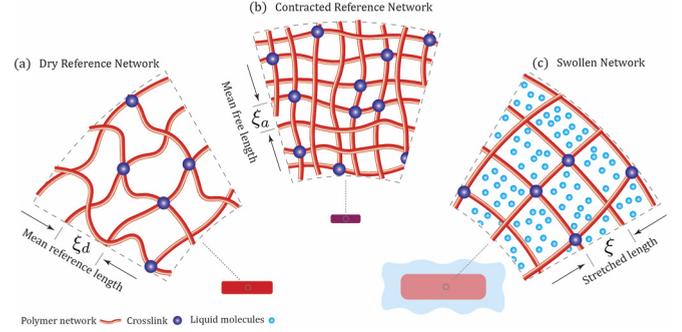


FIG. 2. Schematics of the gel: (a) Dry-reference mesh (red) of size ξ_d with cross-links (blue dots). (b) Dry-contracted mesh: mesh size ξ_c is reduced with respect to ξ_d , and cross-link density is higher. (c) Swollen mesh: liquid molecules (light blue dots) swell the dry-contracted mesh: the free energy is proportional to the stretch ξ/ξ_a between the contracted mesh and the swollen one.

for details), which allows us to set up initial-boundary value problems relevant to describe real experiments. Here, inspired by the experiments in [5], we consider a disklike continuum body. At the initial time, the swollen, flat gel disk \mathcal{B}_o has radius R_o and thickness H_o . Both R_o and H_o are λ_o times larger than the radius and thickness of the corresponding dry disk \mathcal{B}_d assumed as a reference configuration of the active gel disk (see Fig. 1). The model describes the state of the gel at any material point $X \in \mathcal{B}_d$ and time $\tau \in \mathcal{T}$, with \mathcal{T} the time interval, by using the following three state variables: the solvent concentration $c_d(X, \tau)$ per unit of dry volume ($[c_d] = \text{mol/m}^3$), the mechanical displacement $\mathbf{u}_d(X, \tau)$ ($[\mathbf{u}_d] = \text{m}$), and the active strain tensor $\mathbf{F}_a(X, \tau)$ ($[\mathbf{F}_a] = 1$). To these three state variables of the model, there correspond three balance equations, which control liquid flow, stress state, and active contractions.

The current position x of the point X of the gel is given by $x = X + \mathbf{u}_d(X, \tau)$ and the deformation gradient $\partial x/\partial X$ is $\mathbf{F}_d = \mathbf{I} + \nabla \mathbf{u}_d$. We denote with \mathcal{B}_τ the current configuration of the gel at time τ ; the initial configuration \mathcal{B}_o is thus given by $x_o = X + \mathbf{u}_d(X, 0) = \lambda_o X$, where the stretch λ_o is determined by the bath's chemical potential.

Solvent concentration c_d and displacement \mathbf{u}_d are the standard state variables of the Flory-Rehner model; the active strain \mathbf{F}_a is the new variable used to describe the gel contraction, that is, the local change of the natural shape of the mesh due to motor activity (see Fig. 2). The tensor \mathbf{F}_a is the 3D local equivalent of the volume v_a mentioned in the previous section: given the reference volume element dV_d , the corresponding contracted and current volume elements dv_a and dv are given by

$$dv_a = J_a dV_d \quad \text{and} \quad dv = J_d dV_d, \quad (4)$$

with $J_a = \det \mathbf{F}_a$ and $J_d = \det \mathbf{F}_d$. The deformation between the current and the contracted state is measured by the elastic deformation $\mathbf{F}_e = \mathbf{F}_d \mathbf{F}_a^{-1}$; see [19,27]. It is worth noting that no contraction corresponds to $\mathbf{F}_a = \mathbf{I}$, $J_a = 1$, and we recover the standard stress-diffusion model of passive gels. Moreover, the time-dependent symmetric tensor $\mathbf{C}_a = \mathbf{F}_a^T \mathbf{F}_a$ corresponds to the target or natural metric used in [20,21], and the symmetric tensor $\mathbf{C}_e = \mathbf{F}_e^T \mathbf{F}_e$ describes the so-called elastic metric, which affects stress distribution in the network [19].

At any point $X \in \mathcal{B}_d$ and time $\tau \in \mathcal{T}$, the solvent content of a volume element is $dv_l = \Omega c_d dV_d$, with Ω the molar volume of the liquid ($[\Omega] = \text{m}^3/\text{mol}$). The requirement that the current volume element dv is the sum of the active volume dv_a plus the liquid volume dv_l , that is, $dv = dv_a + dv_l$, yields an important relation that couples the three state variables of the problem,

$$J_d(X, \tau) = J_a(X, \tau) + \Omega c_d(X, \tau). \quad (5)$$

Looking at the mesh size, we have the same scaling as in the previous 1D example: $dv \sim \xi^3$, $dv_a \sim \xi_a^3$, $\xi_a/\xi_d \simeq J_a^{1/3}$, and $\xi/\xi_d \simeq J_d^{1/3}$.

The polymer fraction ϕ , that is, the ratio between dv_a and dv , is now a function of X and τ , and is given by

$$\phi(X, \tau) = \frac{J_a(X, \tau)}{J_d(X, \tau)} = \frac{1}{J_e(X, \tau)} \quad \text{with} \quad J_e = \det \mathbf{F}_e. \quad (6)$$

In the following, we shall study highly swollen active gels whose polymer fraction $\phi \simeq 10^{-3}$, while J_d ranges between 1000 and 50. Thus, most of the gel volume is due to liquid content, and given the assumption that the mass of the solid matrix remains constant, the gel densification can be measured by the ratio $dv_o/dv = J_{do}/J_d$, where $dv_o = J_{do} dV_d$ is the volume element of the initial configuration \mathcal{B}_o . During the contraction, this ratio becomes much larger than 1, as a large volume of liquid is expelled from the gel. This phenomenon has been observed in experiments [5] and is reproduced by our physical model.

A. Liquid flows

Any gel contraction deforms the gel and drives liquid flow through it; thus, liquid flows within a moving medium. In the spatial frame, the liquid content dv_l of a volume element is described by the current concentration c , defined by $dv_l = \Omega c_d dV_d = \Omega c dv$. From (4), it follows that $c_d = c J_d$. Analogously, the gel velocity \mathbf{u}_d is described by the spatial velocity \mathbf{v} . The local liquid mass conservation in the current configuration is

$$\dot{c} + \text{div}(\mathbf{h} + c\mathbf{v}) = 0 \quad \text{in} \quad \mathcal{B}_t, \quad (7)$$

and it shows that the solvent flux is the sum of a diffusive component \mathbf{h} and a convective component $c\mathbf{v}$, due to gel velocity \mathbf{v} , ($[\mathbf{h}] = [c\mathbf{v}] = \text{mol}/\text{m}^2 \text{ 1/s}$). Equation (7) can be rewritten as follows:

$$\dot{c} + \text{div}(c\mathbf{v}_l) = 0 \quad \text{with} \quad \mathbf{v}_l = \frac{\mathbf{h}}{c} + \mathbf{v}, \quad (8)$$

where \mathbf{v}_l represent the liquid velocity. Hence, the liquid flux \mathbf{h} depends on the relative liquid velocity to the gel as $\mathbf{h} = c(\mathbf{v}_l - \mathbf{v})$. The cartoon in Fig. 3 shows the consequences of Eq. (8) for some values of the relative liquid/gel velocity $\mathbf{v}_l - \mathbf{v}$. The liquid volume-rate $d\dot{v}_l$ through the boundary da of a volume element dv is given by

$$d\dot{v}_l = -\Omega \mathbf{h} \cdot \mathbf{n} da = -\Omega c(\mathbf{v}_l - \mathbf{v}) \cdot \mathbf{n} da. \quad (9)$$

It holds that $d\dot{v}_l > 0$ when liquid is uptaken and $d\dot{v}_l < 0$ when it is expelled. The same volume-rate $d\dot{v}_l$ can be written in the material frame by using a standard pull-back map; we have

$$d\dot{v}_l = -\Omega \mathbf{h} \cdot \mathbf{n} da = -\Omega \mathbf{h}_d \cdot \mathbf{m} dA_d, \quad (10)$$

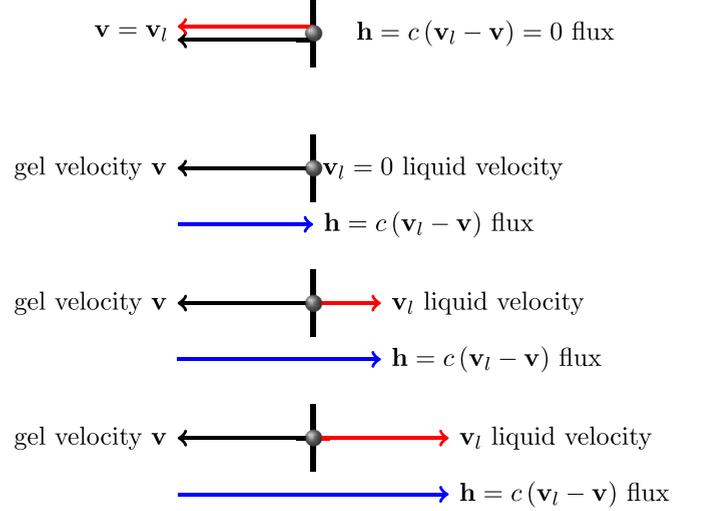


FIG. 3. Given a point (circle) on the boundary (vertical thick line), the current flux \mathbf{h} through the boundary (blue arrow) depends on the relative velocity $(\mathbf{v}_l - \mathbf{v})$. The cartoon shows four cases with different \mathbf{v}_l (red arrow), whose outcome ranges from zero flux (top) to a very large flux (bottom).

with \mathbf{n} and \mathbf{m} the unit normals to the area elements da and dA_d , respectively. Equation (10) yields the definition of the reference flux $\mathbf{h}_d = J \mathbf{F}^{-1} \mathbf{h}$.

Also, the local liquid mass conservation (7), written in the current configuration, can be pulled back from \mathcal{B}_t to \mathcal{B}_d : the corresponding liquid mass conservation written in the material frame \mathcal{B}_d is given by

$$\dot{c}_d + \text{div} \mathbf{h}_d = 0 \quad \text{in} \quad \mathcal{B}_d. \quad (11)$$

Equation (11) is the one we shall use and solve in our model. It is worth noting that by writing the liquid mass conservation in the material frame, it could not be noticed at a glance that the liquid flux \mathbf{h}_d is the sum of a diffusive term plus a convective one.

B. Stresses and active contractions

The overall stress in the current configuration is measured by the Cauchy stress tensor \mathbf{T} , which gives the force $\mathbf{T}\mathbf{n}$ per unit current area da . To \mathbf{T} there corresponds a nominal stress $\mathbf{S}_d = \mathbf{T}\mathbf{F}_d^*/J$, which gives the force $\mathbf{S}_d\mathbf{m}$ per unit reference area dA [therein, $\mathbf{F}_d^* = (\mathbf{F}_d^T)^{-1}$]. The balance equation of forces in the reference configuration \mathcal{B}_d is written in terms of \mathbf{S}_d as

$$\text{div} \mathbf{S}_d = \mathbf{0} \quad \text{in} \quad \mathcal{B}_d \quad \text{and} \quad \mathbf{S}_d \mathbf{m} = \mathbf{0} \quad \text{on} \quad \partial \mathcal{B}_d. \quad (12)$$

The right side of (12) is zero because we are neglecting inertial forces (as timescales associated with diffusion and activity are considerably longer than those associated with inertia). The right side of (12) is zero because we are assuming that the boundary pressure exerted by the liquid in the bath on the gel is negligible, and we do not have any other external boundary tractions.

Balance of forces holds at any time t and, when the liquid flux $\mathbf{h} = \mathbf{0}$, characterizes the thermodynamic equilibrium in passive gels. In active gels we have one more balance equation describing the contraction dynamics. It produces a

dissipative dynamics in the form of a flow rule for the local time-dependent active strain \mathbf{F}_a as

$$\dot{\mathbf{F}}_a = \mathbf{M}^{-1} \{[\mathbf{B} - \mathbf{E}_{\text{sh}}(\mathbf{F}, c_d)]\} \mathbf{F}_a, \quad (13)$$

where the generalized force \mathbf{B} mimics the action of the molecular motors, and the Eshelby tensor \mathbf{E}_{sh} brings in the model the effect of the chemomechanical state of the body. Finally, the power density dissipated in the system due to active contraction is $\mathbf{M}\dot{\mathbf{F}}_a \cdot \dot{\mathbf{F}}_a$, and the *dissipation tensor* \mathbf{M} is assumed to be positive-definite (to get a positive dissipation power density) and diagonal.

C. Model equations under cylindrical symmetry

We exploit the cylindrical symmetry that greatly simplifies the evolution equations of the problem; thus, the reference disk \mathcal{B}_d is represented by its vertical cross section \mathcal{S}_d spanned by the radial coordinate $r \in (0, R_d)$ and the vertical one $z \in (0, H_d)$. With this, the displacement \mathbf{u}_d has two nonzero components: the radial u and the vertical w component; within the class of tensors \mathbf{F}_a , which are cylindrically symmetric, we choose a diagonal one and write $\mathbf{F}_a = \text{diag}(\gamma_r, \gamma_\theta, \gamma_z)$. The consequence of this choice is that our active contraction provides a change in the natural mesh size that acts as a local time-dependent source of volumetric and linear strains, whereas shear strains are neglected.

The state variables of the problem are reduced to the following six scalar fields: the solvent concentration c_d , the two displacements (u, w) , and the three contractions $(\gamma_r, \gamma_\theta, \gamma_z)$; each field is a function of the coordinates (r, z) and the time τ . Moreover, we assume that the derivatives $u_{,z}$ and $w_{,r}$ are zero, that is, we neglect any possible small shearing between the vertical and radial directions. It follows that the deformation gradient \mathbf{F}_d reduces to $\mathbf{F}_d = \text{diag}(\lambda_r, \lambda_\theta, \lambda_z)$ with the radial, hoop, and vertical deformations defined as

$$\lambda_r = 1 + u_{,r}, \quad \lambda_\theta = 1 + u/r, \quad \lambda_z = 1 + w_{,z}, \quad (14)$$

respectively. Under the symmetry assumption, the volumetric constraint (5) takes the form

$$\lambda_r \lambda_\theta \lambda_z = 1 + \Omega c_d. \quad (15)$$

The state of the active gel is ruled by the set of balance equations introduced above. Under the cylindrical symmetry hypotheses, Eq. (11) reduces to

$$-\dot{c}_d = h_{r,r} + \frac{h_r}{r} + h_{z,z}, \quad [3mm] \quad (16)$$

where h_r and h_z are the radial and vertical components of the solvent flux. So, the liquid volume rate through the lateral surface of the disk is $2\pi R_d \Omega h_r(R_d, z) dz$, whereas the liquid volume rate through the top face of the disk is $2\pi r \Omega h_z(r, H_d) dr$. Equations (12) reduce to

$$s_{r,r} + \frac{s_r - s_\theta}{r} = 0 \quad \text{and} \quad s_{z,z} = 0, \quad (17)$$

where s_r , s_θ , and s_z are the radial, hoop, and vertical components of the nominal stress (also called symmetric Piola stress), that is, the stress components on an area element dA_d orthogonal to the radial direction, to the azimuthal direction, and to the vertical direction.

Fluxes h_r and h_z , chemical potential μ , and stresses s_r , s_θ , and s_z are related to the stretches λ_i and the contractions γ_i ($i = r, \theta, z$) by constitutive equations, whose derivation is fully described in several texts and papers (see [16,18,27]). Shortly, liquid transport in the gel is described by a kinetic law, based on the assumption that the liquid molecules move across the gel pores following Fick's law (linear dependence on the chemical potential gradient):

$$h_r = -\frac{D c_d}{RT \lambda_r^2} \mu_{,r} \quad \text{and} \quad h_z = -\frac{D c_d}{RT \lambda_z^2} \mu_{,z}, \quad (18)$$

where D is the diffusion coefficient, which has been assumed to be the same in the radial and vertical directions, R and T are the gas constant and the temperature, respectively, and $\mu = \mu(J_e, p)$ is the chemical potential of the solvent in the gel:

$$\mu = RT g(J_e) + \Omega p, \quad J_e = \det \mathbf{F}_e = \frac{J_d}{J_a}, \quad (19)$$

with

$$g(J_e) = \left[\log \left(\frac{J_e - 1}{J_e} \right) + \frac{1}{J_e} + \frac{\chi}{J_e^2} \right]. \quad (20)$$

Therein, the parameter χ is the nondimensional disaffinity parameter, which controls the attraction between liquid and network, and the pressure field p is the Lagrangian multiplier of the constraint $J_d = J_a + \Omega c_d$ [Eq. (5)] [22]. The characteristic time $l^2/D = \tau_d$ of the liquid transport, with l a characteristic length of the problem, will be compared with the characteristic times brought in the model by contraction dynamics to identify different regimes.

Finally, the overall stresses are given by constitutive equations of the form

$$\begin{aligned} s_r &= G \lambda_r \frac{\gamma_\theta \gamma_z}{\gamma_r} - p \lambda_\theta \lambda_z, \\ s_\theta &= G \lambda_\theta \frac{\gamma_r \gamma_z}{\gamma_\theta} - p \lambda_r \lambda_z, \\ s_z &= G \lambda_z \frac{\gamma_r \gamma_\theta}{\gamma_z} - p \lambda_r \lambda_\theta, \end{aligned} \quad (21)$$

where G is the shear modulus of the dry polymer network ($[G] = \text{J/m}^3$). The corresponding Cauchy stresses are $\sigma_r = s_r/\lambda_\theta \lambda_z$, $\sigma_\theta = s_\theta/\lambda_r \lambda_z$, and $\sigma_z = s_z/\lambda_r \lambda_r$.

Finally, Eq. (13) specializes to three scalar equations, which deliver the flow rules for the active contractions γ_i ($i = r, \theta, z$) [28]:

$$\begin{aligned} \dot{\gamma}_r &= \frac{1}{\eta_r} (\beta_r - E_r) \gamma_r, \\ \dot{\gamma}_\theta &= \frac{1}{\eta_\theta} (\beta_\theta - E_\theta) \gamma_\theta, \\ \dot{\gamma}_z &= \frac{1}{\eta_z} (\beta_z - E_z) \gamma_z. \end{aligned} \quad (22)$$

These equations show that flow rules are driven by $(\beta_i - E_i)$ ($i = r, \theta, z$), that is, by the difference between the generalized forces β_i and the components E_i of the Eshelby tensor, which depends constitutively on the chemomechanical state of the gel. We assume $\beta_i(X, \tau) = \beta(\tau)$, corresponding to assuming an isotropic and homogeneous distribution of motors in the gel, and we view it as the control parameter of the contraction

process. On the contrary, we cannot control the components E_i , which are in general neither homogeneous nor constant and, within the Flory-Rehner thermodynamics, depend on the state of the gel as

$$E_i = e_y - J_d \sigma_i \quad (i = r, \theta, z) \quad (23)$$

with

$$e_y = \frac{RT}{\Omega} J_a F(\mathbf{C}_e) - c_d \mu(J_e, p). \quad (24)$$

The function $F(\mathbf{C}_e)$ is the dimensionless free-energy density per unit natural volume, and it reads $F(\mathbf{C}_e) = f_c(J_e) + m f_e(\mathbf{C}_e)$, with f_c and f_e the dimensionless mixing and elastic free-energy, where $m = G\Omega/RT$ is the ratio between the elastic energy and the mixing energy:

$$f_c(J_e) = (J_e - 1) \log\left(1 - \frac{1}{J_e}\right) + \chi \left(1 - \frac{1}{J_e}\right),$$

$$f_e(\mathbf{C}_e) = \frac{1}{2} (\text{tr} \mathbf{C}_e - 3). \quad (25)$$

Equations (22)–(25) show that the interplay between activity, elasticity, and liquid transport depends on the effective controls $(\beta - E_i)$; in general, the dissipation constants η_i can be different in the three directions and can bring in the model more than one characteristic time $\tau_{\eta_i} = \eta_i/RT/\Omega$; large dissipation constants yield small contraction time rates $(\dot{\gamma}_r, \dot{\gamma}_\theta, \dot{\gamma}_z)$, under the same effective input.

We assume that the disk is not constrained, nor loaded, the entire disk boundary is permeable, and chemical equilibrium holds at the boundary, that is,

$$\mu = \mu_e \quad \text{on} \quad \partial \mathcal{S}_d, \quad (26)$$

where μ_e is the difference between the chemical potential of the bath and that of pure water ($\mu_e = 0$ corresponds to a pure water bath). Finally, the initial conditions for the displacements u, w , the concentration c_d , and the contractions γ_i ($i = r, \theta, z$) are the following:

$$u = (\lambda_o - 1)r, \quad w = (\lambda_o - 1)z, \quad c_d = c_{d0}, \quad \gamma_i = 1, \quad (27)$$

corresponding to the deformation $f_o(X) = \lambda_o X$ for any $X \in \mathcal{B}_d$ from \mathcal{B}_d to \mathcal{B}_0 (see Fig. 1).

IV. INITIAL AND FINAL EQUILIBRIUM STATES

The controls μ_e and β trigger contraction-liquid transport dynamics between the initial and the final state (see Fig. 4). We assume that both μ_e and β have a characteristic evolution dynamics from their initial values (μ_0, β_0) to their final values (μ_1, β_1) , described by the following time laws:

$$\mu_e = \mu_e(\tau) = \mu_0 + (\mu_1 - \mu_0) s(\tau/\tau_\mu),$$

$$\beta = \beta(\tau) = \beta_0 + (\beta_1 - \beta_0) s(\tau/\tau_\beta), \quad (28)$$

where $s(\cdot)$ is a smoothed step function [29] running from 0 to 1 in the interval (0,1), and τ_μ and τ_β are characteristic times [30], which have been tuned to match the results presented in [5]; see Table I. For the motors, the characteristic time depends on the binding/unbinding kinetics of the motors to the actin filaments, whereas for the chemical potential, the

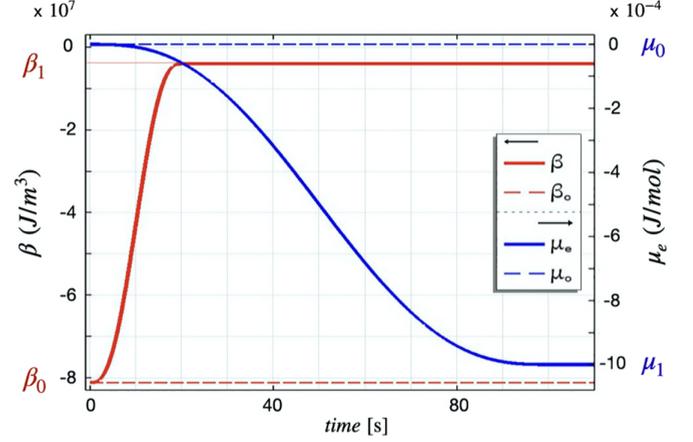


FIG. 4. β goes from β_0 to β_1 in $\tau_\beta = 20$ s (dashed and solid red lines); μ stays constant in scenario (a) and goes from $\mu_0 = 0$ to μ_1 in $\tau_\mu = 100$ s (solid blue). β axis at left, μ axis at right.

characteristic time reflects the mixing kinetic of possibly free biopolymer chains and the liquid in the bath.

The initial state and the final one are *equilibrium states*, that is, $\mathbf{h}_d = \mathbf{0}$, which implies $\dot{c}_d = 0$ and $\dot{\gamma}_i = 0$ ($i = r, \theta, z$).

We assume that at the initial and final equilibrium states, \mathbf{F}_d and \mathbf{F}_a are uniform and spherical, that is, $\mathbf{F}_d = \lambda \mathbf{I}$, $\mathbf{F}_a = \gamma \mathbf{I}$, and that the overall stress is null. With this, and with Eqs. (21), (19), and (23), we can represent the chemical potential and the Eshelby components at those equilibrium states as functions of $J_a = \gamma^3$ and $J_d = \lambda^3$:

$$\mu = \mu(J_d/J_a) = \mu(J_e) \quad \text{and} \quad E_i = e_y(J_a, J_e). \quad (29)$$

Moreover, the equilibrium states are guaranteed by constant and homogeneous chemical potential μ_e and bulk source β such that

$$\mu_e = \mu \quad \text{and} \quad \beta = E_i. \quad (30)$$

Equations (29) and (30) deliver the relation between the pair (J_a, J_d) and the pair (μ_e, β) which must hold at the equilibrium states:

$$\mu_e = \mu(J_e) \quad \text{and} \quad \beta = e_y(J_a, J_e). \quad (31)$$

TABLE I. Material and geometrical parameters.

Shear modulus	$G = 135$ Pa
Flory parameter	$\chi = 0.4$
Water molar volume	$\Omega = 1.8 \times 10^{-5}$ m ³ /mol
Temperature	$T = 293$ K
Energy ratio	$m = G\Omega/RT = 1 \times 10^{-6}$
Diffusivity	$D = 1 \times 10^{-3}$ m ² /s
Dissipation	$\eta = 1 \times 10^5$ Pa s
Initial radius	$R_o = 1500$ μ m
Initial swollen volume and stretch ratio	$J_o = 1000$, $\lambda_o = 10$
Initial aspect ratio	$AR = 2R_o/H_o = 20$ – 40
Initial thickness	$H_o = 150$ – 75 μ m
Final volume/initial volume	$J_{a1} = 0.05$
Control time for β	$\tau_\beta = 20$ s
Control time for μ	$\tau_\mu = 100$ s

We label (J_{d0}, J_{a0}) the pair corresponding to the initial equilibrium state and (J_{d1}, J_{a1}) the pair corresponding to the final state; the same labels hold for all the other quantities.

1. Material parameters

The values assigned to the initial thickness and aspect ratio (AR) have been prompted by [5], and the successive parametric analyses always consider values of AR and H_o not too far from the initial ones. The discrepancy between our value for the shear modulus G and the value reported in [5] is due to the fact that the former is the shear modulus at dry conditions, while the latter is the effective shear modulus G_{eff} measured at the swollen state, with $G_{\text{eff}} \simeq G/J_{d0}^{1/3}$. We set the diffusivity constant D and the dissipation $\eta_r = \eta_\theta = \eta_z = \eta$ in order to get a time evolution from \mathcal{B}_o to \mathcal{B}_1 similar to that taken by the real disk to reach a mechanically stable state (steady state), that is, ~ 200 s. With this, we set the characteristic time τ_η , leaving τ_d free to get different values, depending on H_o , which are in any case always higher than τ_η (see Table I for the complete list of material parameters).

2. Initial state

We assume a fully swollen state as the initial state of the gel, characterized by a not contracted mesh size ξ_a equal to the reference mesh size ξ_d . From an experimental point of view, it means that self-contraction and liquid release are going to be initiated; from the modeling point of view, it means that the active gel is still not contracted and is in its thermodynamic equilibrium, that is,

$$\mu_e(0) = \mu_0 = 0 \text{ J/mol} \quad \text{and} \quad J_{a0} = 1. \quad (32)$$

By putting these values in Eqs. (31), we find the initial change in volume $J_{d0} = J_{e0} = \lambda_0^3$ of the gel and the initial value β_0 of the generalized force which maintains that initial state. Specifically, Eqs. (31) take the form

$$0 = \mu(J_{d0}/J_{a0}) \quad \text{and} \quad \beta_0 = e_y(J_{a0}, J_{e0}). \quad (33)$$

The zero stress condition at the initial time delivers $p_0 = G/\lambda_o$. With this, the constitutive Eqs. (19) and (20) for the chemical potential and Eq. (33) deliver

$$0 = \left[\log \left(1 - \frac{1}{\lambda_0^3} \right) + \frac{1}{\lambda_0^3} + \frac{\chi}{\lambda_0^6} \right] + \frac{m}{\lambda_0}. \quad (34)$$

Equation (34) can be solved for λ_0 , and Eq. (33) determines the initial value β_0 which the control has to get to guarantee null contraction ($\xi_a = \xi_d$) and the free swelling stretch λ_0 :

$$\frac{\Omega}{RT} \beta_0 = (\lambda_0^3 - 1) \left(\frac{\lambda_0^3 - 1}{\lambda_0^6} \chi - \frac{1}{\lambda_0^3} \right) + m \left(\frac{1}{\lambda_0} + \frac{\lambda_0^2}{2} - \frac{3}{2} \right). \quad (35)$$

It is worth noting that Eq. (34) is standard in stress-diffusion theories based on Flory-Rehner thermodynamics [25,26]; it is easy to verify that, given μ_0 , the free-swelling stretch λ_0 increases as m decreases. On the contrary, Eq. (35) does not belong to standard stress-diffusion theory, and it is peculiar to the present augmented model.

The initial values of J_d , J_e , c_d , p , and β , corresponding to the material parameter in Table I, can be easily evaluated. In particular, we get $J_{d0} = 1000$.

3. Final states

We consider two different scenarios: (a) where only a change in the generalized force drives the active contractions and liquid transport, that is, $\beta_1 \neq \beta_0$ and $\mu_1 = \mu_0$; (b) where also a change in the chemical potential of the bath drives the active contractions and liquid transport, that is, $\beta_1 \neq \beta_0$ and $\mu_1 \neq \mu_0$.

The differences between the two scenarios are noteworthy. Indeed, in passive gels the input that drives the system out of equilibrium is at the system's boundaries, that is, a change of the chemical potential in the bath starts liquid transport. On the contrary, a distinctive feature of active gels is the fact that the input that drives the system out of equilibrium is local. Through the analysis of the two scenarios, we compare dynamics due to only local input, that is, a change in the generalized force, and to both local and boundary input, that is, a change in both the generalized force and the chemical potential of the bath.

In both the scenarios, however, and in accordance with the experiments in [5], we assume that at the final state the mesh is contracted by $\xi_a/\xi_d = J_{a1}^{1/3} \simeq 0.38$ with respect to the dry mesh size, that is, $J_{a1} = (\xi_a/\xi_d)^3 = 0.05$. The estimation of the final value J_{a1} allows us, within the model, to estimate the final value β_1 of the generalized force, as is shown below by describing step-by-step the procedure to infer those data from the equations of the model.

Scenario a (fluid flow induced by active contractility). We assume

$$\mu_1 = \mu_0 = 0 \text{ J/mol}, \quad J_{a1} = 0.05, \quad (36)$$

and we put these values in Eqs. (31) to obtain the final swelling ratio J_{d1} and the generalized force β_1 . Specifically, the two equations take the form

$$0 = \mu(J_{d1}/J_{a1}) \quad \text{and} \quad \beta_1 = e_y(J_{a1}, J_{e1}). \quad (37)$$

With our data, we find $J_{d1} = 50$. Comparing this value with the change in volume delivered under the same chemical conditions, that is, $J_{d0} = 1000$, we can conclude that, due to self-contraction, an effective bulk stiffening is predicted by the model, as has already been recognized as crucial in other works [10].

Scenario b (fluid flow generated by the active contractility and changes in the chemical potential of the liquid bath). Typically, in the experiments, the chemical potential of the bath is not controlled. While previously assumed constant [see (a)], it is possible that chains, small fragments, and even monomers can be broken from the gel and released into the solution upon contraction of the gel, by changing the chemical potential of the bath [31]. This motivated our choice to study the impact of a change in μ_e on the contraction dynamics.

We assume that at the final equilibrium state, J_{d1} is half the value of case (a), while J_{a1} is the same as before, that is,

$$J_{d1} = 25, \quad J_{a1} = 0.05. \quad (38)$$

TABLE II. Data about the aspect ratios; values of R_o and H_o are in mm.

Constant R_o $H_o(R_o = 1.5)$	Constant H_o $R_o(H_o = 0.1)$	AR
0.15	1.0	20
0.12	1.25	25
0.1	1.50	30
0.086	1.75	35
0.075	2.0	40
0.066	2.25	45

By putting these values in Eqs. (31), we obtain the pair (μ_1, β_1) . Specifically, the two equations take the form

$$\mu_1 = \mu(J_{d1}/J_{a1}) \quad \text{and} \quad \beta_1 = e_y(J_{a1}, J_{e1}). \quad (39)$$

Of course, other choices would be possible; for example, apart from setting different values for J_{d1} , we could first set μ_1 and then determine J_{d1} from Eqs. (31). What we aimed to remark is that the same value of β_1 can deliver a quite different value of the final change in volume J_{d1} of the disk (25 versus 50) when liquid transport and release is driven by both the mesh contraction and the change in the chemical conditions of the bath.

V. CONTRACTION DYNAMICS

Gel activity does not have any characteristic lengths, since motor activity is assumed to be homogeneous across the system. However, contraction dynamics inherits the characteristic length of the dynamic of liquid transport. The disks built and tested in [5] represent a good basis for a pilot study aimed to discuss the relations between the two dynamics in terms of the key geometrical parameter, which is the aspect ratio of the disks.

We carried on the analysis by either changing the disk initial thickness H_o , for a fixed initial disk radius $R_o = 1.5$ mm, or by varying the disk initial radius at a fixed thickness $H_o = 0.10$ mm. The investigated range of parameter AR is described in Table II: it goes from disks of initial aspect ratio 20 (thick disks) to disks of initial aspect ratio 45 (thin disks).

We show the results obtained for gel disks that contract due to motor only [so-called scenario (a)]. All the experiments start with $J_{d0} = 1000$, i.e., at a highly swollen initial state, and $J_{a0} = 1$, and they evolve towards their final steady values $J_{d1} = 50$ and $J_{a1} = 0.05$. As stated above, these values correspond to a reduction in mesh size $= \xi_{a1}/\xi_{a0} = 0.05^{1/3} = 0.38$, where ξ_{a1} represents the final mesh size, and, as stated above, we consider the final state to be stress-free.

In the regime under study, the system reaches its final steady state after $\tau_1 \simeq 200$ s, that is, we have $\tau_\beta \ll \tau_1$ and the dynamics is ruled by the redistribution of water across the gel mesh until its eventual expulsion through the disk boundary.

A. Diffusion-limited regime

Given the equations of the model, there are different characteristic times whose values have an influence on the

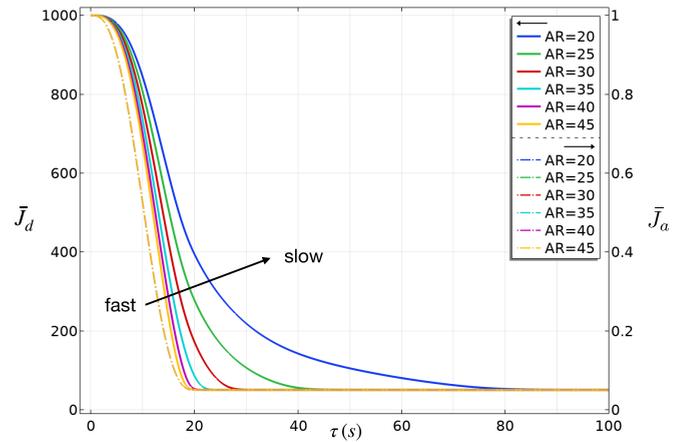


FIG. 5. Plot of \bar{J}_d (solid) and \bar{J}_a (dashed) vs time for different values of AR; disk geometry is given in the first column of Table II. Being $\tau_\eta \ll \tau_\beta$, all the \bar{J}_a curves (dashed) are superimposed, as \bar{J}_a evolves at the same pace of β , and this evolution is not affected by AR. The \bar{J}_d curves (solid) depends strongly on AR, and the thicker the disk, the slower the volume change. This is a consequence of the fact that the liquid must exit through the boundary, and the thickness is the important geometric parameter within our range of AR.

different solution regimes. In particular, the characteristic time τ_η which governs mesh contraction is not size-dependent, being $\tau_\eta \propto \eta \Omega / RT$, while the characteristic time τ_d which governs liquid transport has a length scale, which for our geometries is the current height H , that is, $\tau_d \propto H^2 / D$. Given our choice of η , we have $\tau_\eta \simeq 10^{-3}$ s; the estimation of a value for τ_d is much more difficult because of the large size-change experienced by the disks during contraction.

Our experiments shows that, for our choice of parameters and geometry, the contraction dynamics is *diffusion-limited*, as is affected by the lengthscale. The opposite regime, the so-called *motor-limited* regime, can be realized when $\tau_d \ll \tau_\eta$. The simplest way to discuss the different regimes is through the analysis of the flow rule for J_a , which can be easily derived from Eqs. (22)–(24). Cylindrical symmetry implies

$$J_a = \gamma_r \gamma_\theta \gamma_z \quad \text{and} \quad J_a = J_a \left(\frac{\dot{\gamma}_r}{\gamma_r} + \frac{\dot{\gamma}_\theta}{\gamma_\theta} + \frac{\dot{\gamma}_z}{\gamma_z} \right). \quad (40)$$

With this, the flow rule for J_a can be derived from those for γ_i by Eqs. (22), and it takes the form

$$j_a = \frac{1}{\eta} [3(\beta - e_y) + J_d \text{tr} \mathbf{T}] J_a. \quad (41)$$

Equation (41) and the equation governing the dynamics of diffusion allow us to discuss some of the evidences of our numerical experiments.

To discuss contraction dynamics, we define the averages $\bar{J}_d(\tau)$ and $\bar{J}_a(\tau)$ of $J_d(r, z, \tau)$ and $J_a(r, z, \tau)$, respectively, which well represent the main features of the phenomenon under study, and give a global glance at the contraction dynamics. Due to the cylindrical symmetry of the system, both averages are evaluated on the two-dimensional domain \mathcal{S}_d of area $R_d \cdot H_d$.

In Fig. 5, we plot \bar{J}_a (dashed) and \bar{J}_d (solid) versus time for different values of AR; the figure shows two major findings.

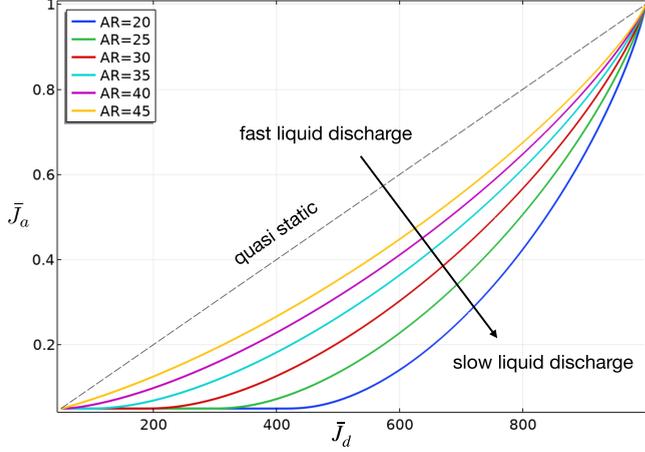


FIG. 6. Plane (\bar{J}_d, \bar{J}_a) : evolution path at constant radius $R_o = 1.5$ mm for different values of AR; disk geometry is given in the first column of Table II. Lower AR correspond to the evolution path far from equilibrium; higher AR corresponds to paths that tend to the quasistatic stress (dashed line).

First, all the curves for \bar{J}_a are superimposed, as $\tau_\eta \ll \tau_\beta$, that is, the evolution of β is slow with respect to the characteristic time τ_η , and $\bar{J}_a(\tau)$ has the same dynamics of $\beta(\tau)$; in particular, the evolution of \bar{J}_a can be approximated as a sequence of equilibrium problems, which depend on β . Moreover, as contraction is a local mechanism, this dynamics is much faster than diffusion, and it is not affected by AR.

Secondly, the curves for \bar{J}_d , representing the volume change, strongly depend on AR, and the thicker the disk, the slower the volume change. This is a consequence of the fact that the liquid must exit through the boundary, and for the range of AR under investigation, the thickness is the important geometric parameter.

B. Dynamics in the plane (\bar{J}_d, \bar{J}_a)

We now focus on the evolution paths in the plane (\bar{J}_d, \bar{J}_a) for scenario (a), that is, $\mu_e = \mu_o = \text{const}$. In this plane, a quasistatic stress-free path is represented by a straight line at constant $\bar{J}_e = \bar{J}_d/\bar{J}_a$, and the dashed line in Figs. 6 and 7. This path corresponds to a sequence of equilibrium states where the current swollen volume \bar{J}_d corresponds to a free swelling for a dry mesh whose current natural volume is \bar{J}_a .

Due to the choices made in Table I, which yields a diffusion-limited regime, liquid transport is affected by the lengthscale. Thus, thinner disks (higher AR) show an evolution in the plane that is closer to the stress-free path, that is, under the same contraction dynamics, liquid transport is faster for these disks, which can quickly recover the original stress-free state. On the contrary, for thicker disks (lower AR), the evolution path is very far from the quasistatic regime: namely, motor-induced contraction is faster than the water transport across the gel mesh, which makes the thick gels highly stressed during their evolution.

We investigated the evolution paths for different AR for varying H_o at constant R_o (Fig. 6) and varying R_o at constant H_o (Fig. 7). In the first case, Fig. 6 shows that by increasing the thickness H_o , that is, the characteristic lengthscale across

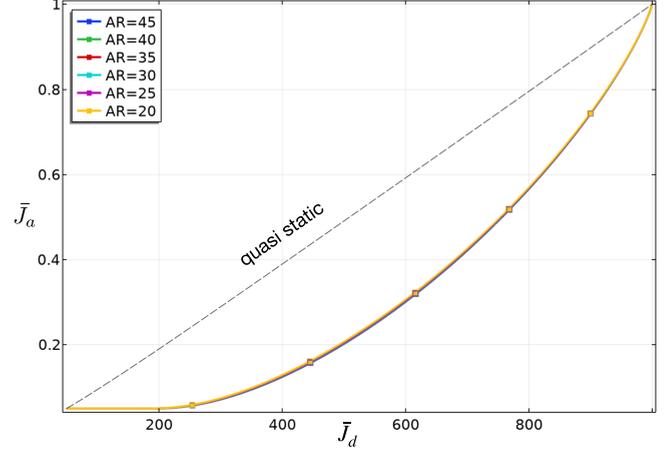


FIG. 7. Plane (\bar{J}_d, \bar{J}_a) : evolution path at constant thickness $H_o = 0.1$ mm for different values of AR; disk geometry is given in the second column of Table II. All the paths are superimposed and the master curve is the one corresponding to AR = 30 in Fig. 6.

which water flows, it increases the characteristic timescale of water transport (from yellow to blue solid lines). As $\tau_\eta \gg \tau_d$ for any values of H_o , the quasistatic path is never realized; however, the thinner the disk is, the closer is the evolution path to the quasistatic one.

To confirm our expectations that the important lengthscale for water exit is H_o , we also studied disk geometries having constant thickness and varying radius. Figure 7 shows the results for the same range of AR: it might be noticed that all the curves are now superimposed as, being that the shortest lengthscale H_o is constant, AR has no effect on the dynamics.

C. Gel contraction velocity

We studied the contraction velocity of the lateral boundary of the disk, i.e., the radial velocity and the effects of AR on it. To do so, we evaluate the average radial stretch Λ_r as follows:

$$\Lambda_r(\tau) = 1 + \frac{1}{H_d} \int_0^{H_d} \frac{u(R_d, z, \tau)}{R_d} dz; \quad (42)$$

it is easy to verify that the average stretch Λ_r also corresponds to the average $\bar{\lambda}_r(\tau)$ of the radial deformation $\lambda_r(r, z, \tau)$ on the cross section \mathcal{S}_d of area $R_d \cdot H_d$.

We also defined an average current radius $R(\tau)$ and a radial contraction velocity $\dot{R}(\tau)$ with the formulas

$$R(\tau) = \Lambda_r(\tau)R_d \quad \text{and} \quad \dot{R}(\tau) = \dot{\Lambda}_r(\tau)R_d. \quad (43)$$

It follows from (43) and the definition of AR that the radial velocity can also be rewritten as $\dot{R}(\tau) = \dot{\Lambda}_r(\tau) \frac{H_d}{2} \text{AR}$. The radial velocity $\dot{R}(\tau)$ is always negative, as the gel disk is contracting and negative is also the generalized force β that produces a contraction. So, in both Figs. 8 and 9 we represented $-\dot{R}(\tau)$ and $-\beta/\beta_0$.

Figure 8 shows that, for a constant radius, the radial velocity $\dot{R}(\tau)$ is characterized by two timescales, one for the time interval during which the velocity increases, and the second for the following interval where the velocity decreases. In the first time interval, the curves fit to a linear law, that is, $\dot{R}(\tau) \propto \tau/\tau_r$, with τ_r the characteristic time of rising.

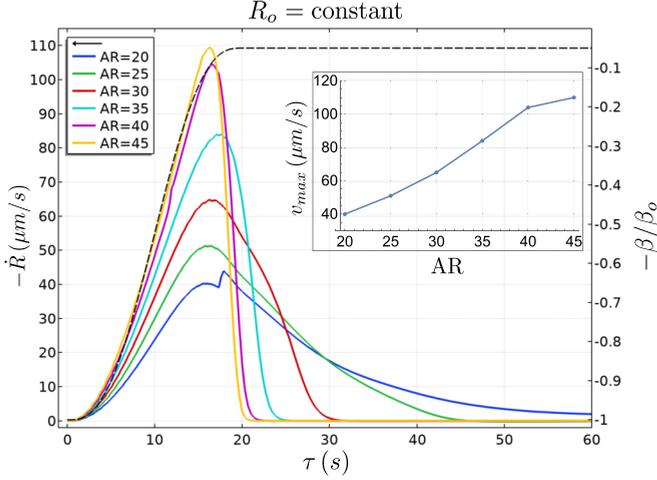


FIG. 8. The time evolution of β (dashed) and corresponding radial contraction velocity \dot{R} of the lateral boundary of the disk at constant radius $R_o = 1.5$ mm for different values of AR; disk geometry is given in the first column of Table II. The color code is the same as in Figs. 6 and 7. The small wiggle in the blue line at $\tau \simeq 17$ s is due to a mechanical buckling: the disk departs from the flat shape; see Fig. 12, panel (c). Velocity ranges over the left vertical axis and β/β_o over the right vertical axis.

During the decreasing time interval, curves fit to an exponential law $\dot{R}(\tau) \propto v_{\max} \exp(-\tau/\tau_{\text{decay}})$, with τ_{decay} the characteristic time of decay. The characteristic times of rising and decay have been estimated for any aspect ratio and are listed in Table III.

The inset in Fig. 8 shows that the maximum radial velocity v_{\max} , attained at peak time τ_p , depends on the geometric parameter AR [32].

Actually, the analysis of Eqs. (42) and (43) shows that when AR changes with H_d (or, equivalently, with H_o as the

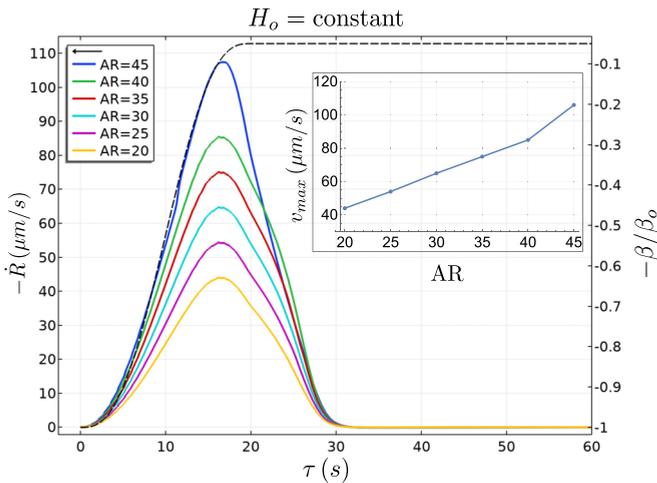


FIG. 9. The time evolution of β (dashed) and corresponding radial contraction velocity \dot{R} of the lateral boundary of the disk at constant thickness $H_o = 0.1$ mm for different values of AR; disk geometry is given in the second column of Table II. Color code is the same as in Figs. 6 and 7. Velocity ranges over the left vertical axis and β/β_o over the right vertical axis.

TABLE III. Max velocity v_{\max} , peak time τ_p , rising time τ_r , and decay time τ_{decay} for different values of aspect ratio AR.

AR	v_{\max} ($\mu\text{m/s}$)	τ_p (s)	τ_r (s)	τ_{decay} (s)
20	44	$\simeq 16$	0.22	13
25	52	$\simeq 16$	0.22	13
30	74	$\simeq 17$	0.18	8
35	84	$\simeq 17$	0.14	3
40	104	$\simeq 17$	0.12	2
45	111	$\simeq 17$	0.11	1.5

initial free-swelling is homogeneous), with R_o constant, the dependence of \dot{R} on AR is also affected by H_d and cannot be linear. The same equations show that, for H_d constant, the dependence of \dot{R} on AR is simply linear. This is what the inset in Fig. 9 shows for the maximum velocity v_{\max} relative to the study at varying radius.

We can split the average stretch Λ_r into an elastic component Λ_e and an active component Λ_a , related to the analogous decomposition of the deformation gradient $\mathbf{F} = \mathbf{F}_e \mathbf{F}_a$ and of the radial deformation λ_r . Thus, the stretching velocity $\dot{\Lambda}_r$ can be written as the sum of two terms, and the radial velocity \dot{R} is represented by

$$\dot{R} = (\dot{\Lambda}_a \Lambda_e + \Lambda_a \dot{\Lambda}_e) R_d, \quad (44)$$

where Λ_a is the average of the active radial deformation γ_r , and it depends on self-contraction, while Λ_e is the average of the elastic radial deformation λ_r/γ_r , and it depends on liquid transport.

Equation (44) highlights the existence of two timescales for \dot{R} : for $\tau < \tau_\beta$ the stretching velocity is dominated by the time evolution of $\beta(\tau)$, while for $\tau > \tau_\beta$ it is dominated by liquid transport, that is,

$$\dot{R} \simeq \dot{\Lambda}_a \Lambda_e R_d \quad \tau < \tau_\beta, \quad (45a)$$

$$\dot{R} \simeq \Lambda_a \dot{\Lambda}_e R_d \quad \tau > \tau_\beta. \quad (45b)$$

Equation (45a) shows that for $t < \tau_\beta = 20$ s, the radial velocity \dot{R} changes with the same rate of Λ_a , which in turns depends on β , as Figs. 8 and 9 show (compare the colored lines with the dashed black line in both figures).

On the other side, Eq. (45b) shows that for $t > \tau_\beta = 20$ s, the radial velocity \dot{R} changes with the rate of Λ_e , which depends on liquid transport and on the smallest lengthscale of the disk, which in our case is H_o , as a comparison between Figs. 8 and 9 shows. The same pair of figures also show clearly that the maximal velocity is reached when τ approaches τ_β , that is, when contraction is near to its maximum value—as was suggested in [5] [see Fig. 4(f) in [5]].

Finally, it is worth noting that the active control β , needed to change the target mesh size, does not change further once it has taken its maximal value. Beyond that, the system evolves towards its steady state by releasing liquid until a new free swollen configuration is reached; at this final state, the effects of the network elasticity balance the active control.

We conclude this section by showing a comparison with experimental results obtained for a very thin disk with $\text{AR} = 50$. By properly tuning the diffusivity D and the dissipation η , our theoretical model is able to reproduce quite

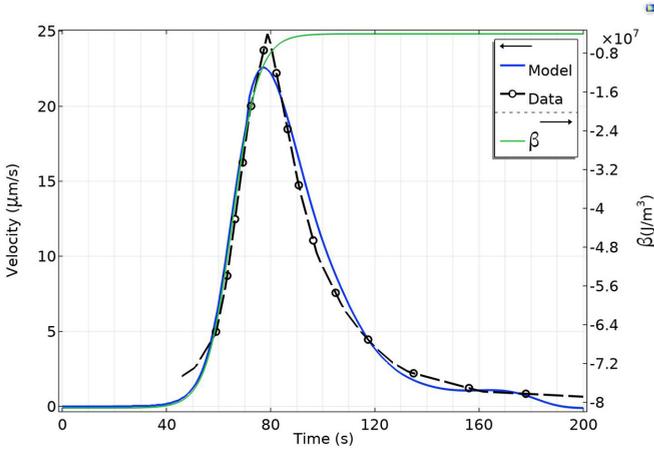


FIG. 10. Radial contraction velocities vs time. Radial \dot{R} (solid blue) contraction velocity of the disk compared with experimental data (dashed with markers). Disk geometry: $R_o = 1.5$ mm, $AR = 50$; material parameters: $D = 0.951 \times 10^{-4}$ m²/s, $\eta = 1.51 \times 10^5$ Pa s.

well the time course of the radial contraction velocity \dot{R} . Figure 10 compares the predicted results (solid-blue) with the experimental ones (dashed-black, circle markers).

D. Densification and stress distribution

As observed in [5], the network starts contracting from the boundary, and the actual mesh size starts decreasing from the boundary to the center of the gel disk. This contraction mode yields boundary effects, which are detected on the gel density, defined as the ratio between the polymer mass and the overall gel volume, and on the overall stress state in the disk.

In [5], a gel densification was observed, that is, an increase of the gel density starting at the periphery and propagating into the gel interior.

Within the model, we use the ratio J_{d0}/J_d to measure the densification from the initial state. Figure 11 shows the den-

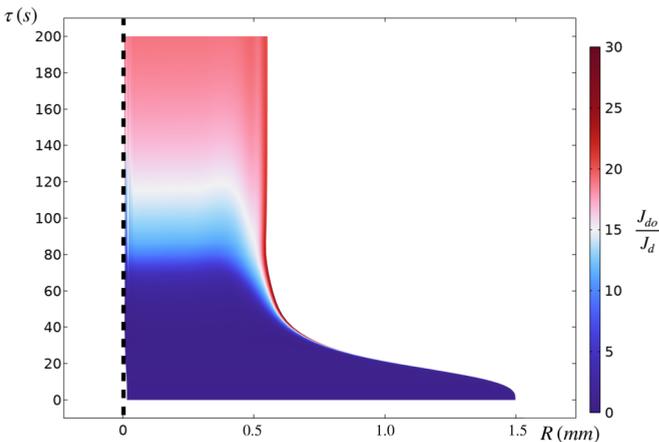


FIG. 11. Densification at the middle cross section of the disk. Ratio J_{d0}/J_d in the plane (R, τ) ; color map: blue is more wet, red is more dry. Densification (red color) starts at the boundary and then propagates inward; disk radius contracts from $R_o = 1.5$ mm to $R_1 \simeq 0.55$ mm.

sification at the middle cross section of the disk by plotting the ratio J_{d0}/J_d in the plane (R, τ) , with $R = r + u$ the current radial position. It is noted that, when $\tau \equiv \tau_\beta = 20$ s and contraction is fully developed, a narrow red strip of densification appears at the periphery; then, it propagates towards the interior until the whole cross section is more dense. The representation in the current domain determines the peculiar “boot” shape of the profile: as time goes on, the disk contracts and its radius contracts from $R_o = 1.5$ mm to $R_1 \simeq 0.55$ mm. On the other hand, stress analysis in the active disk can be relevant, as overall stress distribution might drive mechanical instability, which leads to a variety of different shapes at the end of the contraction [5,20,33,34]. The analysis of instabilities is beyond the scope of the present work, and it will mark our future efforts. However, through the aforementioned studies, we might have interesting clues about shape transitions by investigating the effects of AR on the evolution of radial stress σ_r and the hoop one σ_θ in the disk, which may drive further experiments.

We only report results for the case of constant radius. We compare the stress state in a thick ($AR \simeq 20$) and a thin ($AR \simeq 45$) disk. Panels (a) and (b) of Fig. 12 show the existence of two stress patterns: in a core region (beige), the stress is constant along the radius and spherical, that is, $\sigma_r = \sigma_\theta$; in the periphery (cyan), the stress varies with the radius and $\sigma_r \neq \sigma_\theta$. As the bulk contraction β is homogeneous and isotropic in the whole disk, these two regions are determined by the dynamics of liquid transport. In particular, the width of the peripheral region is of the order of the thickness because the solvent in this region can escape from both the lateral boundary and the top and bottom surfaces. In contrast, for the solvent in the core, the shortest path to exit the gel disk is through the top and bottom surfaces. Corresponding to our values of AR, we have $H_{\text{thin}} \simeq 0.04R_d$ and $H_{\text{thick}} = 0.1R_d$.

In particular, in Fig. 12, for $AR = 20$ we have essentially $\sigma_r < 0$ along all the radius, and σ_θ varying from negative to positive [see panel (a)]; for $AR = 45$ we have $\sigma_r > 0$ along all the radius, and σ_θ varying from positive to negative [see panel (b)]. The stress distribution for these two cases is typical of that found in frustrated domelike or saddelike disks [see Fig. (12), panels (c) and (d)] [20,33,34].

That is a preliminary requirement for observing instability patterns that can deliver domes or saddles, depending on other key factors, which are not investigated in the present paper.

E. Evolution of the aspect ratio during contraction

Finally, the geometry of the gel body suggests that we investigate the possibility of having dissipations η_r and η_θ in the plane, different from the vertical dissipation η_z . Dissipations are related to the resistances of the mesh to reorganize, which can be expected to be different. Our conjecture needs to be validated, and the analysis may stimulate further experiments in this direction.

As noted at the end of Sec. II, the system is controlled by the pair (μ_e, β) , and here we also analyze the combined effects of varying the chemical potential μ_e and active force β (scenario b).

We always consider a homogeneous and isotropic generalized force β . Nevertheless, during gel contraction, the radial

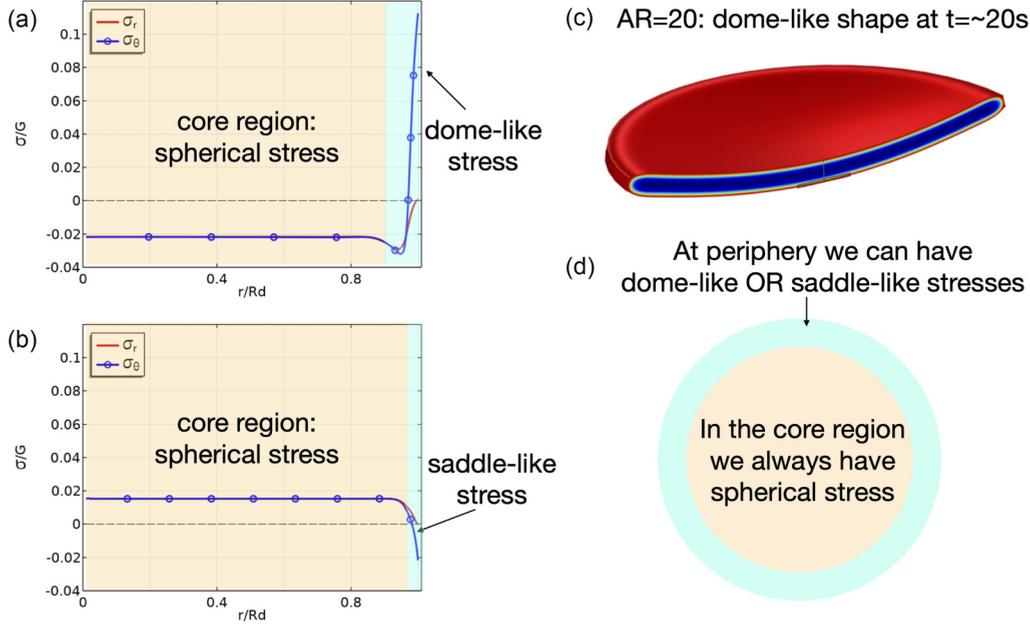


FIG. 12. Effect of AR on stress distribution for disks with constant radius. Panels (a) and (b) show the radial σ_r (red) and hoop σ_θ (blue) overall stresses vs the nondimensional radius r/R_d at $\tau = 20$ s, for AR = 20 and 45. (a) AR = 20: the hoop stress is negative in the core (beige) and positive at the periphery (cyan), a typical pattern of frustrated domelike shape.

and vertical stretches might differ locally, and each one of them can vary in time and space. We use the average values $R(\tau)$ and $H(\tau)$ of radius and thickness to describe the change in the aspect ratio of the disk, with $R(\tau)$ defined by Eq. (43) and $H(\tau)$ defined as $H(\tau) = \Lambda_z(\tau) H_d$ with

$$\Lambda_z(\tau) = 1 + \frac{1}{R_d} \int_0^{R_d} \frac{w(r, H_d, \tau)}{H_d} dr. \quad (46)$$

At any time τ , the ratio $H(\tau)/H_o$ can be plotted against the ratio $R(\tau)/R_o$ to illustrate the evolution path of the radial and vertical stretches, that is, the curve $\tau \mapsto (R(\tau)/R_o, H(\tau)/H_o)$, plotted in the plane $(R/R_o, H/H_o)$. In Fig. 13, the curve has been represented for a disk with AR = 22 and $R_o = 1.5$ mm. In that plot, the dashed line represents an isotropic evolution, during which the aspect ratio remains constant during network contraction.

For each of the two analyzed cases, corresponding to scenario (a) (red) and (b) (blue), we show two curves, one corresponding to equal dissipations (diamond markers), $\eta_r = \eta_\theta = \eta_z$, and the other with different horizontal and vertical dissipations (asterisk markers), $\eta_r = \eta_\theta = 2 \eta_z$. We note that the evolution is very sensitive to dissipation, while the differences between scenarios (a) and (b) are less noticeable. For all simulations, the system evolves via a characteristic path. It departs from the isotropic contraction path, but in the case with equal dissipations the steady-state configuration ends on the dashed line (i.e., on the isotropic path), while the case with different dissipations ends far from it. In particular, when $\eta_r = \eta_z$, the contraction is almost isotropic until $H/H_o = R/R_o \sim 0.8$; then, the radial contraction is faster, and eventually the vertical one becomes faster. When $\eta_r = 2 \eta_z$, the vertical contraction is much faster than the radial one, and the final state is not isotropic.

These first clues deserve to be investigated further both experimentally and numerically to stress the morphing chances of active gel.

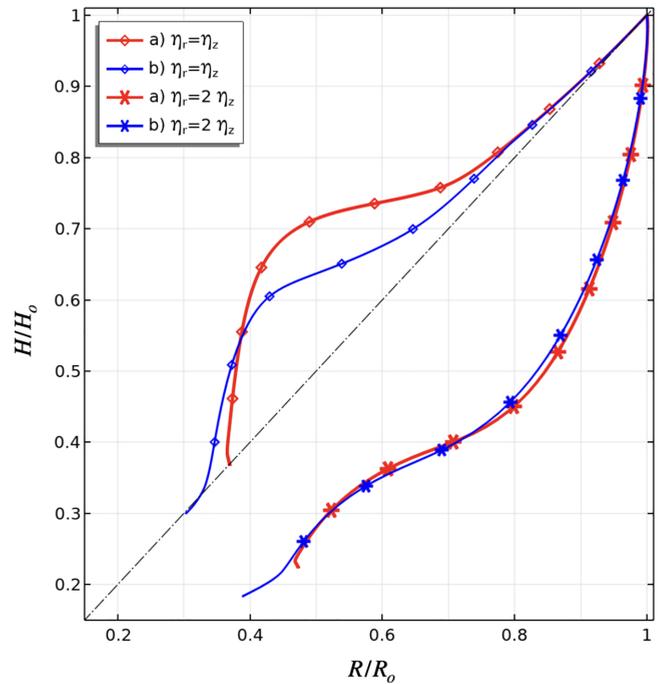


FIG. 13. Thickness ratio H/H_o vs radius ratio R/R_o during contraction for cases (a) (red) and (b) (blue) with equal friction $\eta_r = \eta_z$ (diamond) and differential friction $\eta_r = 2 \eta_z$ (star); $\eta_r = 10^5$ Pa s. The dashed line represents isotropic contractions; with different frictions, the radial and vertical contractions are not isotropic. Disk geometry: $R_o = 1.5$ mm, AR = 22.

VI. CONCLUSIONS AND FUTURE DIRECTIONS

We discussed the interplay between elasticity, liquid transport, and self-contractions in active gel disks from the perspective of continuum mechanics. The transient problem for gel disks of different aspect ratios has been solved, and different aspects of the problem have been discussed: the regimes of fast and slow liquid transport, the characteristic times of the contraction and liquid transport dynamics, and the changes in the stress state in gel disks of different thickness. In doing so, the analysis of the competitive role of gel contractility and liquid flow in driving the mechanics of the active gel has been exploited.

To keep the model easy, the numerical model has been developed under the hypothesis of cylindrical symmetry, which excludes the challenge to observe disk morphings, which are not compatible with the cylindrical symmetry. Actually, we are planning to give up the symmetry hypothesis above and investigate the blossom of stresses in the disk, which may drive instability patterns and, consequently, a variety of steady shapes of the gel. This was beyond the scope of the present work, and it will mark our future efforts.

Giving up the symmetry hypothesis also makes more interesting the identification of the determinants of possible changes in shape, whose control would make it possible to get actuators based on self-contractile gels, a promising field that can be set within the framework here presented.

ACKNOWLEDGMENTS

This work has been supported by MAECI (Ministry of Foreign Affairs and International Cooperation) and MOST

(Ministry of Science and Technology–State of Israel) through the project PAMM. A.B.-G. is also grateful to the Israel Science Foundation (Grant No. 2101/20). G.L. is grateful to the MOST for the Jabotinsky PhD Scholarship. F.R. also thanks INDAM-GNFM for support with Progetti Giovani GNFM 2020. L.T. acknowledges the Italian grant PRIN 2017KL4EF3, “Mathematics of active materials: From mechanobiology to smart devices.”

APPENDIX

1. Details of finite-element analysis

Equations (15), (16), and (22), together with the boundary (26) and initial (27) conditions, are rewritten in a weak form and implemented in the software COMSOL MULTIPHYSICS by using the Weak-Form physics interface. The calculus domain is the rectangular domain S_d , which is meshed with triangular elements whose maximum mesh size is $H_d/10$, yielding about 200 K DOFs. Lagrangian polynomials are used as shape functions: polynomials of order 4 for the displacement and the solvent concentration, of order 3 for the volumetric constraint, of order 2 for the boundary conditions (also implemented in weak form), and of order 1 for the remodeling variables. The whole set of coupled equations are solved by using the Newton method with variable damping as the nonlinear solver; the linear solver is the direct solver Pardiso, while the time-dependent solver uses the BDF method with order 1–2. The time-dependent analysis starts at the initial state \mathcal{B}_0 and stops at a final equilibrium state \mathcal{B}_1 , which is preselected.

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